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Fluid Systems Configuration Databook

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ABBREVIATIONS AND ACRONYMS

AFD	Aft Flight Deck
ACS	Attitude Control System
ACS	Atmosphere Control and Supply
AR	Atmosphere Revitalization
B-CRS	Bosch Caron Reactor Subsystem
CFE	Continuous Flow Electrophoresis
ECLSS	Environmental Control and Life Support System
EEU	Extra-vehicular Excursion Unit
ELM	Experimental Logistics Module
ESA	European Space Agency
EVA	Extra-vehicular Activity
F	Fahrenheit
FDS	Fire Detection and Suppression
FMS	Fluid Management System
GPF	Gas Processing Facility
HFM	Hollow Fiber Membrane
HPTA	High Pressure Tank Assembly
HR&T	Heat Rejection and Transport
IFMS	Integrated Fluid Management System
IOC	Integrated Operational Capability
IOC	Integrated Operations Configuration
INS	Integrated Nitrogen System
IWFS	Integrated Waste Fluid System
IWS	Integrated Water System
JEM	Japanese Experiment Module
кон	Potassium Hydroxide
kW	Kilowatt
1b	Pound
1bm	Pounds Mass
LHe	Liquid Helium
MEOP	Maximum Expected Operating Pressure
MLI	Milti-Layer Insulation
MMU	Manned Maneuvering Unit
MORL	Manned Orbiting Research Laboratory
MSFC	(George C.) Marshall Space Flight Center
NASA	National Aeronautics and Space Administration
NASDA	National Space Development Agency (Japanese)
NHB	NASA Handbook
NSTS	National Space Transportation System
OMV	Orbital Maneuvering Vehicle
ORU	Orbit Replaceable Unit
OSCRS	Orbital Spacecraft Consumable Resupply System
OTV	Orbital Transfer Vehicle
PLC	Pressurized Logistics Carrier
PM	Payload Module
PMMS	Process Material Management System
PPV	Portable Pressure Vessels
psia	Pounds Per Square Inch Absolute
PWHS	Process Waste Handling System
RF	Radio Frequency
RMS	Remote Manipulator System

ABBREVIATIONS AND ACRONYMS (continued)

SFHe	Superfluid Helium
SFHT	Superfluid Helium Tanker
SIRTF	Space Infrared Telescope Facility
SMR.	Sabatier Methanation Reactor
SS	Space Station
SSP	Space Station Program
SSPE	Space Station Program Element
TBD	To Be Determined
TBS	To Be Determined by Supplier
TCS	Thermal Control System
TED	Thermoelectric Device
THC	Temperature and Humidity Control
ULC	Unpressurized Logistics Carrier
USL	United States Laboratory
U.S.	United States
WHS	Waste Handling System
WM	Waste Management

FOREWORD

This report was prepared by Martin Marietta Space Systems Company, under Contract NAS8-36438 in compliance with data submittal requirement J-1-3 in the Statement-of-Work. The contract is being administered by Marshall Space Flight Center, Huntsville, Alabama. Mr. John Cramer is the NASA Project Manager.

INTRODUCTION

This databook contains fluid system requirements and system descriptions for Space Station Program Elements. Program elements include the United States and International modules, integrated fluid systems, attached payloads, fluid servicers and vehicle accommodation facilities. Fluid system requirements and system configurations were derived from the DR-02, "Databooks from Work Package 1" and October 19896 Fluids Integrated Panel Data. Data contained in this document was used to generate EP 2.2, "Space Station Program Fluid Inventory Databook."

The fluid system requirements and system descriptions of each Space Station Program Elements are defined in the following sections.

```
Section 1.0
              United States Laboratory
Section 2.0
              Habitation Module and Airlocks
Section 3.0
              Logistics Elements
Section 4.0
              Japanese Experimental Module
Section 5.0
              Columbus
Section 6.0
              Integrated Waste Fluid System
Section 7.0
              Integrated Water System
Section 8.0
              Integrated Nitrogen System
Section 9.0
              Environmental Control and Life Support System
Section 10.0
              Thermal Control System
Section 11.0
              Attached Payloads
              Fluid Services/Vehicle Accommodations
Section 12.0
```

Each section includes a discussion of the overall system requirements, specific fluid systems requirements and system descriptions. The system descriptions contain configurations, fluid inventory data and component lists. In addition, a list of information sources are referenced at the end of each section.

1.0 UNITED STATES LABORATORY MODULE

1.1 UNITED STATES LABORATORY OVERALL REQUIREMENTS

The USL will be a multidiscipline facility for payload accommodation within a pressurized habitable volume. It will accommodate materials research and development most sensitive to acceleration, research in basic science requiring long duration of extremely low acceleration levels, life sciences research relating to benefits of and adaption to long duration exposure to extremely low acceleration levels and control and monitoring of user-attached pressurized modules and selected external attached payloads.

The microgravity requirement of 10^{-5} for payload operations will enhance materials processes and allow for the advancement of knowledge and the development of process controls. The USL will also accommodate the scale-up to pilot plant operations and the operation of pre-production and commercial facilities in space.

The overall requirements for the United States Lab (USL) Module are presented in Table 1.1-1.

Table 1.1-1 Overall Requirements for the United States Laboratory

- 1) Accommodate the performance of selected complements of experiments.
- 2) Provide cooling of 6 kW with selected double-rack cooling of 15 kW to accommodate experiment compliments.
- 3) Provide a process fluids system.
- 4) Provide a vacuum vent system.
- 5) Provide a waste management system.

1.2 UNITED STATES LABORATORY FLUID SYSTEMS REQUIREMENTS

Fluid requirements for the Environmental Control and Life Science System, Thermal Control System, Process Materials Management System, and Vacuum Vent System are provided in Table 1.2-1.

1.3 UNITED STATES LABORATORY FLUID SYSTEMS DESCRIPTIONS AND CONFIGURATIONS

The USL fluid systems may be categorized into four working groups; the Environmental Control and Life Support System (ECLSS), the Thermal Control System (TCS), the Process Materials Management System (PMMS) and the Vacuum Vent System.

1.3.1 Environmental Control and Life Support Systems (ECLSS)

The USL Environmental Control and Life Support System's primary function will be to maintain a habitable environment in which the crew members can perform laboratory experiments. A system description, fluid quantities and component lists of the ECLSS have been included in Section 9 of this report.

The primary ECLSS user interfaces will be in the areas of avionics air cooling and air contamination control. Thermal control interfaces will include cabin heat exchangers, avionics heat exchangers and air revitalization equipment. Manned systems interfaces will include the commode, shower and hand washing systems.

Table 1.2-1 Fluid Systems Requirements for The United States Laboratory

USL Element	USL	Fluid System Requirement
Environmental Control and Life Support	1)	Provide atmospheric pressure and composition control.
System*	2)	Provide temperature control and humidity maintenance.
	3)	Provide atmospheric revitalization.
		Provide water to meet crew and experimental needs.
	5)	Provide waste management.
Thermal Control System	1)	Provide an integrated system which maintains structures, ancillary compartments, components, subsystems and customer payloads within their specified temperature limits.
	2)	
Process Material Management System	1)	Provide storage and distribution of USL process fluids.
	2)	Provide safe handling, removal, storage and disposition of USL payload waste by-products.
	3)	Provide a .25 torr vacuum pressure for waste gas removal from all USL payloads.
	4)	_ · ·
	5)	Comply with Space Station external contamination constraints.
	6)	• •
	7)	Interface with Integrated Fluid Management System (IFMS).
·	8)	Provide storage in the gaseous waste handling system of all gases that are not
		compatible with the IWFS for a minimum of 14 days.
Vacuum Vent	1)	Maintain a high quality vacuum resource for USL
System		user community.
	2)	Provide a minimum of .001 torr vacuum pressure to experiments.

^{*} Primary control is monitored and maintained by the Space Station core module

1.3.2 Thermal Control System

The thermal control system will consist of three basic cooling loops, a primary experiment loop, an attached payload pump and a refrigerator/freezer loop. The primary experiment loop will be a pumped single-phase water coolant loop which services the experiment racks, the avionics cooling heat exchanger and the cabin condensing heat exchanger. Waste heat from this primary loop will be transferred to the Space Station Heat Rejection and Transport System (HR&T) through central bus heat exchangers mounted on the exterior of the USL end cone structure.

The attached payload loop will be used to cool equipment in adjacent nodes. This loop will also use single-phase water as the working fluid.

Refrigeration/freezing services will be provided to the USL with an integrated air/freon cooling loop. Heat acquired in the freezer will be transferred to low temperature body mounted radiators to reject the heat necessary to meet a -30° C freezer requirement.

The TCS will be a closed loop system that does not require scheduled fluid resupply and as a result will be considered independent from the integrated fluid systems. Accommodations have been made in the TCS for fluid leakage and system purging to remedy system contamination. However, the fluid quantities specified may be considered insignificant in comparison to the overall water inventory of the Space Station elements.

1.3.3 Process Material Management System (PMMS)

The Process Material Management System will be responsible for two major USL services. The first Service is the storage and distribution of USL process fluids and the second is the safe handling, removal, storage and disposal of USL payload waste by-products. Figure 1.3-1 shows an overview of the entire PMMS responsibilities.

1.3.3.1 Process Fluids Storage and Distribution

Process Fluids Supply

The PMMS will be responsible for the storage and distribution of specific consumable gases and liquids used by the USL facilities and laboratory support equipment. Process fluids include water, helium gas, nitrogen gas, argon gas, oxygen gas, carbon dioxide gas and hydrogen gas. Fluid groups such as etchants, solvents, buffers, cleaning fluids, xenon, acetylene gas and fuels were identified as possible process fluid candidates but are required in small quantities or by single users and have been defined as being user supplied.

Several experiment payloads have requested to use liquid nitrogen and liquid helium. These fluids are requested for their thermal properties and not necessarily required to perform the experiment. The Critical Point Facility is the only exception which will utilize LN2 and LHe as part of the experiment other than for cooling. To minimize long term storage problems associated with cryogenics and system complexity, experiment cooling will be provided by a closed loop helium refrigeration cycle. This concept, discussed in greater detail under the cryogenics section will provide a 138.6 K temperature level when required, and in the process will eliminate cryogenic storage and transportation problems.

The closed loop cryogenic refrigeration cycle will not require helium resupply with the exception of leakage makeup. As a result, the only requirement for liquid helium is requested by the Critical Point Facility. Because of the large amount of power required for liquid helium production, liquid helium has been recommended to be user provided.

Liquid nitrogen will be produced by transferring gaseous nitrogen from the ECLSS system and cooling it with the helium refrigeration system in a portable dewar. The liquid nitrogen will then be transported in the dewar to the experiment.

The PMMS will be required to provide a 90 day supply of the process fluid quantities previously mentioned. These fluid quantities and storage interface requirements for the storage and distribution system are summarized in Tables 1.3-1 and 1.3-2. A list of components for the storage and distribution system is also provided in Table 1.3-3.

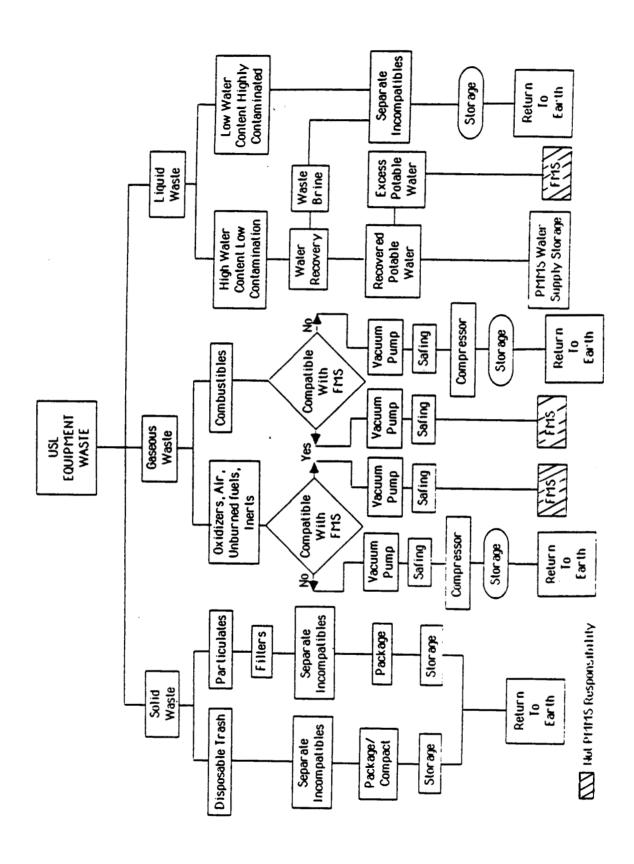


Figure 1.3-1 Process Material Management System Overview

Table 1.3-1 USL Process Material Management System Fluid Inventory Requirements

8 8	FLUID	SUBSYSTEM	FLUID	STORED	USAGE	RESUPPLY QUANTITY (LB/90 DAYS)	ITY (LB/90 DAYS)	RESUPPLY	FLUID COMPOSITION	REMARKS
į	i i				(LB/HR)	MEAN	MAX			
33	Isn	CRYOGENIC	989	OET.	4.2 CEM MAX/.26 MINIO	0	LEAKAGE MAKEUP	SUPPLY LINE	780	CLOSED LOOP REFRIGERATION SYSTEM.
~	lust	PFS	HZ0	992.3	130	1130	15072	FLUID TRANSFER	99.5 \$ PURE	ASSUMES 858 WASTE MATER RECOVERY WITH PHMS.
· ·	lost	. _	GN2	255.3		161.0	170.2	ECLSS	OET -	
.	lust	Sal	200	42.6	1380	22.9	128.4	ECLSS	SE -	
· · ·	Inst	- LE	9 70	3.5	Outi	6.1		FLUID TRANSFER/PPV		
	Tsn i	- LPFS	- E	17.7 SCF	OET -	10.7	9.0_	FLUID TRANSFER	oer i	
	l UST	- LES	<u>- ¥</u> _	55.5	TBO	 32.6 	137.0	FLUID TRANSFER/PPV	08	
•	Inst	PFS		9.		126.0	36.4	l Pev	GE 1.	
, <u>, , , , , , , , , , , , , , , , , , </u>	Inst	Sää	FREON	-1		-0	6.0	FLUID TRANSFER	OE:	
_ = 	1901 	PFS	AIR	0.0	OH T	189.3	7.76	FLUID TRANSFER FROM ECLSS	 SEE REMARKS 	PPO2-2.83 TO 3.35 PSIA PPN2-11.87 TO 11.35 PSIA
	Inst	SJ4 I		128.1	TBO	10.9	118.7	PPV	081	
 	Inst	SJa	ACETYLENE	8		0.0	0.0	Ada	OHT .	
 	lost	S.a.d.	CLEANING SOL'N	248.4	TBO	117.1	- 165.6 	l PPV	1390	
	Inst	PFS -	CUTTING POLISH	DEL .	-11BO		-11 08 1	Add.	08.1	OF OE
11	Inst	PES	ETCHANTS	1780	OET.	TBO	Jan Ogri	PPV	DET	rigi Po
	Inst	PES	SOLVENTS	OBT	1180 		1380	PPV	OET	INA DOH
	Tsn!	PES	BUFFER SOLUTION IBD		- TBO	iriso		PPV	OST	TT :
	Inst	S.d.	FUELS	08.	TBD	OET	1.130 1.	PPV	TBO	PAC UA
	LOST	FPS	BUTANE	OET	1730	TBO	OHT.	l PPV	1380	īĒ. LIT
	lost	PFS	METHANE	081	1780	TBO	1780 	l PPV	1780 08.1	IS Y
	I nor	PFS	 PROPANE		TIBO	TBD I		PPV		
	Inst I	PFS	ALCOHOL	OET.	LTBO		1730	PPV	- I TBO	
	lust	- IPFS	TOLUENE	1780	TBD	irBO		PPV	TBO	
	insr 	PFS	XYLENE	1780 1	TBD	Ogt .	TBO	PPV		

Table 1.3-1 (Continued) USL Process Material Management System Fluid Inventory Requirements

REMARKS							HATER IS TRANSFERED FROM ORBITER FUEL CELLS AND ECISS TO NODE STORAGE SYSTEM.
FIUID		TBD	OBT .	TBD	TBD	SEE TABLE 1.3-6	POTABLE NATER WATER IS IT
RESUPPLY		PPV	Ada	PPV	PPV	HA	TRANSFER FROM ORBITER
TY (LB/90 DAYS)	HAX	981	OE -	0E	- 136 - 136		OET -
RESUPPLY QUANTITY (LB/90 DAYS)	MEAN	OHL	Off	Offi	TBO		1130
USAGE	(1.B/HR)	730	OET	-E-	OB	3.178 cfm max NA	.176 GFH
STORED		OET.		- T-	<u></u>	1	992.3
TYPE		STERILIZERS	STAINS	CULTURE MEDIA	NUTRIENTS	MIXTURE	
SUBSYSTEM		PFS	PFS	PFS	PFS	PMB	WATER RECOVERY SYS. H20
SYSTEM		Tsn Tsn		Inst	In TSD	TSO TSO	Tsn.
38		- 2	28 UST	58	===-	<u>×</u>	я я

PWH - Process Waste Handling Mixture - Fluids and Gases Listed in Table 1.3-5

Table 1.3-2 USL Frocess Material Management System Fluid Interface Requirements

REMARKS		DELIVERY IS NOT FAILURE TOLERANT	FALISAFE	FALSAFE	FALLSAFE	FAILSAFE	FALLSAFE	FALLSAFE	FAILSAFE	FALISAFE	FALISAFE	FAILSAFE	FALLSAFE
FAITURE	TOLERANCE	NONE DE	ZERO FA	ZERO F.A.	ZERO FA	ZERO (FA)	ZERO IFAI	ZERO FAI	ZERO FAI	ZERO FAI	ZERO FAI	ZERO FAI:	ZERO FAL
HETHOD OF	MANAGEMENT	RECYCLED	S#4	SH4S	Proc	PHPS	Phets	PMS	Press	Press	PHPES	Press	PM4G
	LINE SIZES	27. 27.	375	375 11	.375	.25 .25	375 I	2	PPV IP	PPV IP	.25 -18	PPV PPV	PPV IPP
INLET AND CUTLET FLUID CONDITIONS	124e	113	130 07	22	0,0	28	88	28	0,0 11.4	8 8 - # #	70 14.7	70 81 81	77 7 8 1 1 1
JULIET FLUID	PRESSURE (PSIA)	300	001 001	200	1250	3000/2000	100	3000/2000	2000 TBD	12000	70.07	08T 08T	TBO OBT
INIET AND	PNO.	STORAGE	NODE FILTRATION	ECLSS EXPERIMENT	EXPERIMENT	LOG MODULE EXPERIMENT	HYDRIDE TANK EXPERIMENT	LOG MOD EXPERIMENTS	LOG NOD EXPERTMENT	LOG MOD EXPERIMENT	ECLSS EXPERIMENT	LOG MOD EXPERIMENT	LOG MOD
TYPE		GBo	Н20	GN2	2005	GHe	GH2	Αr	88	FREON	AIR	 .	ACETYLENE
SUBSYSTEM		CRYOGENIC	PFS	534	PFS	PFS	PFS	SJ4	PFS	PFS	PFS	PFS ()	PFS
SYSTEM		UST	nsr.	Tsn	TSO	lust	nsr				al Tsn	USI. IF	
ģ		32	- 	= m		s		7 IUSL	9	10 lust	= = 	12 10	13 USL

 $ilde{r}_{e}$ ble 1,3-2 (Continued) USL Process Material Management System Fluids Interface Requirements

I	DIULI	TYPE	INIET AND C	INIET AND COTLET FLUID CONDITIONS	CONDITIONS			FAILURE	REMARKS	
•			FROM	PRESSURE (PSIA)	TEMP. (F)	LINE SIZES	MANAGEMENT			
PFS		CLEANING SOL'N	LOG MOD EXPERIMENT	780 780	66	PPV PPV	PMS	ZERO	FAILSAFE	
PFS		CUTTING POLISH	LOG MOD EXPERIMENT	55	88	PPV	Press	ZERO	FALLSAFE	
PFS		ETCHANTS	LOG MOD EXPERIMENT	55	5 5	PPV	PMMS	ZERO	FAILSAFE	
PFS		SOLVENTS	LOG NOD EXPERIMENT	01.13 04.1	86	MA.	Profes	ZERO	FAILSAFE	
PFS	го.	BUFFER SOLUTION	LOG HOD EXPERTHENT	9 9	22	PPV	STATE	ZERO	FALLSAPE	
PFS	ø	FUELS	LOG MOD EXPERIMENT	22	22	PPV	Procs	ZERO	FAILSAFE	
PFS	ø	BUTANE	LOG NOD EXPERIMENT	01.11 01.11	22	Mad I	Proc	ZERO	FAILSAFE	
PFS	ø	METHANE	LOG NOD EXPERIMENT	087 087	88	PPV	SADAS	ZERO	FAILSAFE	
PFS	ys	PROPANE	LOG NOD EXPERIMENT	OST	88	MA .	Precs	ZERO	FALLSAFE	
PFS	ya	ALCOHOL	LOG NOD EXPERIMENT	08T 08T	55	PPV	Prots	ZERO	FAILSAFE	
PFS	'n	I TOLLUENE	LOG MOD EXPERIMENT	OET I	2 2	IPPV IPPV	Proces	ZERO	FALLSAFE	
_ 53.a_	Ş.	XYLENE	LOG MOD EXPERIMENT	OET OET	88	PPV	Sign	ZERO	FAILSAFE	
_==-	PFS	 Sterilizers 	LOG MOD EXPERIMENT	087	22	PPV	SI#18	ZERO	FAILSAFE	
_==	PFS	STAINS	LOG MOD EXPERIMENT	06T 04T	22	Mail Mail	PHAS	ZERO	FAILSAFE	
=	PFS	CULTURE MEDIA	LOG MOD EXPERIMENT	08T T	22	I P PV	Prevs	ZERO	FAILSAFE	
_=	PFS	NUTRIENTS	ILOG MOD EXPERIMENT	0.01	88	744 744	Procs	ZERO	Falisafe	
<u> </u>	PWH	MIXTURE	EXPERIMENT IMPS	1.005-500	06 70 06 70	- 5 5	SAFING COMPONENTS BEFORE IMPS		FAILURE TOLERANT	
=	MATER RECOVERY SY H20	I H20	USL STORAGE WATER PURIFICATION	100	0. 2.5	.375	CONTINUOUS RECYCLING	NONE	HUST BE DEIGNIED AND PYROGEN FREE, POTABLE AND DISTILLED. SUPPLY NOT FAILURE TOLERANT.	
١										

Mixture - Various combinations of constituents in Table 1.3-5.

Table 1.3-3 USL Process Material Management System Component List

10 10 10 10 10 10 10 10	ITEM	PROGRAM APPLICATON	COMPONENT	RECO	SIZE (in)	PRESSURE MEOP (psia)	USAGE	APPROK MASS (1b)	VENDOR NAME	VENDOR PART NUMBER
High states Control 1	•	USI., PFS	DISCONNECT,	12	.25	3000	GHE, AR	0.7	1780	TBD
COLUMNITATION COLUMNITATION 1373 1300 150 <td></td> <td>USL, PFS</td> <td>DI SCONNECT,</td> <td>\$</td> <td>.25</td> <td>100</td> <td>H20</td> <td>7.0</td> <td>130</td> <td>130</td>		USL, PFS	DI SCONNECT,	\$.25	100	H20	7.0	130	130
1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1,		USL, PFS	DI SCONNECT,	36	375.	100	H20	7.0	1 TBD	130
10.1. 10.1. 13.5 13.0 10.0 10.1 10.0 10.1. 10.1. 13.5 13.0 10.0 0.0 1.3 10.0 10.1. 10.2. 10.2 13.5 10.0 0.0 1.3 10.0 10.1. 10.2 10.2 10.0 10.0 10.2 10.0<		USI., PFS	FILTER, INLINE		.375	100	H20	5.5	TBD	Off
10.00 10.00 <th< td=""><td></td><td>USL, PFS</td><td>MISC, FLEX HOSE</td><td></td><td>.375</td><td>98</td><td>ξ<u>ξ</u></td><td>1.1</td><td>TBD</td><td>081</td></th<>		USL, PFS	MISC, FLEX HOSE		.375	98	ξ <u>ξ</u>	1.1	TBD	081
Light Fire loosed 44 775 789 180		USL, PFS	MISC, FLEX HOSE		.375	100	82	•.0	THE COLUMN	Off
10.1.7.7.1.2. Model 10.1.7.1.2. Model 1.0.1.2. Model <th< td=""><td></td><td>USL, PFS</td><td>MISC, FLEX HOSE</td><td>\$</td><td>.375</td><td>100</td><td>H20</td><td>2.5</td><td>TBD</td><td>130</td></th<>		USL, PFS	MISC, FLEX HOSE	\$.375	100	H20	2.5	TBD	130
ULI, 753 RGC, FOME LGC 1,73 100 RGC 114 TDD ULI, 753 FOLK, MARY DECEMBER 1 1,73 100 RGC 13,1 TD ULI, 753 FOLK, MARY DECEMBER 6 2,3 200 RGC 33,1 TD ULI, 753 FOLK, MARY DECEMBER 6 2,3 200 RGC 33,1 TD ULI, 753 FOLK DECEMBER 1 2,3 200 RGC 13,0 TD ULI, 753 FOLK DECEMBER 1 2,3 200 GGC, AR 13,0 TD ULI, 753 FOLK DECEMBER 1 2,3 200 GGC, AR 13,0 TD ULI, 754 FOLK DECEMBER 1 2,3 200 GGC, AR 2,3 TD ULI, 754 FOLK DECEMBER 1 2,3 2,0 TD TD ULI, 754 FOLK DECEMBER 1 2,3 2,3 TD TD ULI, 754 FOLK DECEMBER<		USL, PFS	MISC, FLEX HOSE	8	.25	05	GHE, AR	0.15	- TBD	OBI
ULI, PRES TEACH AND PRESENTED 1 .135 100 66.2 PD C6.2 PD ULI, PRES PRESSURA VASSELL, 6 .235 2000 ORD 26.0 PD 100 ULI, PRES PRESSURA VASSELL, PROCESSE MATCH 1 .235 2000 AM 36.4 PD ULI, PRES PRESSURA VASSELL, PROCESSE MATCH 1 .235 2000 AM 36.4 PD ULI, PRES PRESSURA VASSELL, PROCESSE MATCH 1 .235 100 <t< td=""><td></td><td>USE, PFS</td><td>HISC, PUMP</td><td>-</td><td>375.</td><td>100</td><td>HZO</td><td>11.4</td><td>TBD</td><td>130</td></t<>		USE, PFS	HISC, PUMP	-	375.	100	HZO	11.4	TBD	130
CLASTOR PARSENDE VASSELL, PRINCIPATION 1 7.73 100 HB 7.13 100 CLASTOR PRASSURE VASSELL, PRASSURE VASSELL, PORTMART 6 2.55 2000 ALI BRT 100 15.45 100 CLASTOR PRASSURE VASSELL, PORTMART 1 2.75 2000 ALI BRT 100 15.45 100 CLASTOR PRASSURE VASSELL, PORTMART 1 2.75 300 ALI BRT 100 12.45 100 CLASTOR PRASSURE VASSELL, PORTMART 2 2.75 300 CARL AR 17.5 100 CLASTOR STASTOR CARL AR 2.75 300 CARL AR 17.0 100 CLASTOR TRASTOR CARL AR 2.75 300 CARL AR 17.0 100 CLASTOR TRASTOR CARL AR 2.75 300 CARL AR 2.7 100 CLASTOR CARL AR CARL AR 2.75 300 CARL AR 2.7 100 CLASTOR CARL AR CARL AR 2.75 </td <td></td> <td>USL, PFS</td> <td>HISC, WATER PROCESSOR</td> <td></td> <td>.375</td> <td>100</td> <td>H20</td> <td>66.2</td> <td>130</td> <td>1360</td>		USL, PFS	HISC, WATER PROCESSOR		.375	100	H20	66.2	130	1360
UGL, FFS PRESSURE VASSEL, PROTOSE 6 25 2000 ALL FR.0 FR.		USL, PFS	PRESSURE VESSEL,		375	100	H20	33.1	OST	OST
ULI, FFF PRESSIDE VESELL, PORTABELL, PRESSIDE VESELL, PROCESS MATCH 1 .2 3000 ALL DET TOD ALL		USL, PFS	PRESSURE VESSEL,	•	.25	3000	ZHE	26.0	130	1360
USL, FFS PRESSIONE VESSEL, PORTABLE 1 .25 2000 ALL, BAT REGO TISS		USL, PFS	PRESSURE VESSEL,	•	.25	3000	ž	36.4	TBO	130 0
ULI, FFEST PRESENTAR VASSEL, PROCESS MATTER 1 .775 100 RED 100-3 IND IND IND ULI, FFEST REDILATOR, DOMESTEAL, STONGS CORT. 2 .755 .200 0.00 1.54 IND ULI, FFEST SERIORA, FLORI METTRA 2 .735 .200 0.00 1.50 IND ULI, FFEST SERIORA, FLORI METTRA 1 .735 .200 0.00 1.00 IND ULI, FFEST SERIORA, FLORI METTRA 1 .735 .200 0.00 1.00 IND IND ULI, FFEST SERIORA, FLORI METTRA METAL METAL 1 .735 .200 0.00 0.01 IND		USL, PFS	PRESSURE VESSEL, PORTABLE		.25	2000	ALL BUT H20	12.5	TBD	178D
UGL, FFS PRISSEMEN VASEAL, STONAG COOPT. 1 .775 50 EX.O. 15.4 ThD UGL, FFS SECOLATOR, DOMESTADAR 2 .755 3000 GGE, AR 2.9 100 UGL, FFS SENGOR, PRESONE DOPP 1 .775 100 GGE, AR 2.9 100 UGL, FFS SENGOR, PRESONE DOPP 1 .775 100 GGE, AR 2.9 100 UGL, FFS SENGOR, PRESONE DOPP 1 .775 100 GGE, AR 0.7 100 UGL, FFS SENGOR, PRESONE DOPP 1 .775 100 GGE, AR 0.7 100 UGL, FFS SENGOR, PRESONE DOPP 1 .775 100 GGE, AR 0.7 100 UGL, FFS VALVA, CREAT 1 .755 3000 GGE, AR 0.7 100 UGL, FFS VALVA, CREAT 1 .755 3000 GGE, AR 0.7 100 UGL, FFS VALVA, GGECA 1 .775 100		USL, PFS	PRESSURE VESSEL, PROCESS WATER		.375	100	H20	1080.3	1 13D	OEL -
USI, FFF ESCUILATOR, DOMESTREMA 2 -75 B000 GHZ, AB 2.9 FMD USI, FFF SESSOR, PLON METRIA 2 -7.35 100 60.0 2.0 PD USI, FFF SESSOR, PLON METRIA 1 -7.35 100 60.0 2.0 PD USI, FFF SESSOR, PLON METRIA 1 -7.35 100 60.0 2.0 PD USI, FFF VALVE, CHECK 2 -7.35 100 60.0 2.2 PD USI, FFF VALVE, CHECK 2 -7.35 100 GHZ, AR 1.1 PD USI, FFF VALVE, CHECK 2 -7.35 100 GHZ, AR 1.2 PD USI, FFF VALVE, CHECK 2 -7.35 100 GHZ, AR 0.2 PD USI, FFF VALVE, CHECK 2 -7.35 100 GHZ, AR 0.2 PD USI, FFF VALVE, CHECK 2 -7.35 100 GHZ, AR 0.2 PD<		USI, PFS	PRESSURE VESSEL, STORAGE CONT.		.375	90	H20	15.4	TBO	130
USI, FFS SERROR, FLOR METERS 2 .135 100 REO 2 0 DEC USI, FFS SERROR, PRESSURE 2 .135 100 REO 0.27 PDD USI, FFS SERROR, PRESSURE DROPE 1 .135 100 REO 0.27 PDD USI, FFS SERROR, PRESSURE DROPE 2 .25 900 REO 0.27 PDD USI, FFS WALVE, CREAT 2 .25 900 GRE, AR 1.71 PDD USI, FFS WALVE, CREAT 2 .25 900 GRE, AR 0.77 PDD USI, FFS WALVE, CREAT 2 .275 .900 GRE, AR 0.75 PDD USI, FFS WALVE, SCILDOLD 2 .275 .900 GRE, AR 0.75 PDD USI, FFS WALVE, SCILDOLD 2 .275 .900 GRE, AR 0.75 PDD USI, FFS WALVE, SCILDOLD 2 .275 .900 GRE, AR		USL, PFS	REGULATOR, DOMNSTREAM	~	.25	3000	GHE, AR	2.9	138D	130
USI, FFS SERROR, PRESENDE 17 35 300 GB, AA 0.7 TRD USI, FFS SERROR, PRESENDE DROP 1 .735 100 R20 0.3 TRD USI, FFS SERROR, CALLITY PETTAR 1 .735 300 GB, AA 0.7 TRD USI, FFS WALNE, CIRCAT 2 .735 300 GB, AA 0.7 TRD USI, FFS WALNE, CIRCAT 2 .735 300 GB, AA 0.7 TRD USI, FFS WALNE, CIRCAT 2 .735 100 GB, AA 0.7 TRD USI, FFS WALNE, CIRCATOR 1 .735 100 GB, AA 0.2 TRD USI, FFS WALNE, SULBOLID 1 .735 100 GB, AA 0.3 TRD USI, FFS WALNE, SULBOLID 1 .735 100 RAL AA 1.3 TRD USI, FFS USI, FFS LI .735 14.7 AA 1.4		USL, PFS	SENSOR, FLOW METER	7	.375	100	H20	2.0	1300	130
USI, PFS SENSOR, PRESSURE DORDER 1 135 100 EXD C.3 TRD USI, PFS SENSOR, CALLITY RETRA 1 .355 3000 GRE, AR 1.7 TRD USI, PFS VALVE, CRECK 1 .255 3000 GRE, AR 0.7 TRD USI, PFS VALVE, CRECK 2 .375 100 GRE, AR 0.7 TRD USI, PFS VALVE, CRECK 2 .375 100 GRE, AR 0.7 TRD USI, PFS VALVE, CRECK 2 .375 100 GRE, AR 0.2 TRD USI, PFS VALVE, SULBOID 2 .375 100 REO 0.9 TRD USI, PFS VALVE, SULBOID 1 .375 100 REO 0.6 TRD USI, PFS USI, PFS USI, PFS 1 .375 50 GRE, AR 2.5 TRD USI, PFS USI, PFS USI, PFS .375 14.7 ALL 1.6		USL, PFS	SENSOR, PRESSURE	~~-	.375	3000	GHE, AR	7.0	130	081
USI, PFS SENGRA, CALLITY METRR 1 .375 100 RED 2.2 RD USI, PFS SENGRA, CRECK 2 .35 NOO GRE, AR 1.1 PD USI, PFS WALVE, CRECK 2 .35 NOO GRE, AR 0.7 PD USI, PFS WALVE, CRECK 2 .375 100 RED 0.9 PD USI, PFS WALVE, SCIENCID 2 .375 100 RED 0.9 PD USI, PFS WALVE, SCIENCID 2 .375 100 RED 0.3 PD USI, PFS WALVE, SCIENCID 2 .375 100 RED 2 PD USI, PFS WALVE, SCIENCID 2 .375 100 RED A.6 PD USI, PFR OLIONARCI 1 .375 100 RED A.6 PD USI, PFR OLIONARCI 1 .375 A.1 A.1 A.1 A.1 A.1 A.1		USI, PFS	SENSOR, PRESSURE DROP		375	100	HZ0	0.3	TBD	
USI, PES SANSON, TEMPERATURE 2 .35 3000 GRE, AR 1.1 TID USI, PES VALVE, CIRCAT 1 .35 3000 GRE, AR 1.1 TID USI, PES VALVE, CIRCAT 2 .375 100 GRE, AR 0.75 TID USI, PES VALVE, FLOW RESTRICTOR 1 .775 100 GRE, AR 0.75 TID USI, PES VALVE, SOLEMOID 1 .775 100 REO 0.75 TID USI, PES VALVE, SOLEMOID 2 .375 100 REO 0.76 TID USI, PES VALVE, SOLEMOID 1 .375 100 REO 8.6 TID USI, PER USI, PES 1 .375 100 REO 8.6 TID USI, PER USI, PER 1 .375 1 TID TID TID USI, PER USI, PER 1 .375 LAL ALL 1 TID TID		USL, PFS	SENSOR, QUALITY METER		375.	100	HZO	2.2	TBD	9
USI, PFS WALVE, CRECK 1 .25 3000 GRE, AR 0.7 TRD USI, PFS WALVE, CRECK 2 .735 100 REO 0.9 PD USI, PFS WALVE, PLOM RESTRICTOR 2 .735 100 GRE, AR 0.2 PD USI, PFS WALVE, PLOM RESTRICTOR 1 .735 100 GRE, AR 0.2 PD USI, PFS WALVE, PLOM RESTRICTOR 1 .735 100 GRE, AR 0.2 PD USI, PFS WALVE, SOLEMOID 2 .735 100 REO 2.6 PD USI, PFH MALVE, SOLEMOID 3 .75 50 GRE, AR 2.5 PD USI, PFH DISCONRECT, 1 .75 14.7 AL 1.5 PD USI, PFH DISCONRECT, 1 .75 14.7 AL 1.5 PD USI, PFH DISCONRECT, 2 .75 14.7 AL 1.5 PD <		USI., PFS	SENSOR, TEMPERATURE	~	25	3000	GHE, AR	1.1	TBD	9
USI, PFS VMALVE, CHECK 2 .375 100 HZO 0.9 PRD USI, PFS VMALVE, PLOM RESTRICTOR 1 .375 100 GRE, AR 0.2 PRD USI, PFS VMALVE, SOLEMOID 1 .25 300 GRE, AR 2.5 PRD USI, PFS VMALVE, SOLEMOID 2 .375 100 HZO 2.6 PRD USI, PFS VMALVE, SOLEMOID 1 .375 100 HZO 2.6 PRD USI, PFS VMALVE, SOLEMOID 3 .375 100 HZO 2.6 PRD USI, PFS VMALVE, SOLEMOID 3 .25 50 GRE, AR 2.5 PRD USI, PFH DISCONNECT, 1 .25 14.7 ALL 0.9 PRD USI, PHH DISCONNECT, 1 .25 14.7 ALL 1.6 PRD USI, PHH DISCONNECT, 2 1 1.7 ALL 0.9 PRD		USL, PFS	VALVE, CHECK		.25	3000	GHE, AR	6.7	Tabo	<u>e</u>
USI, PFS VALUR, FLDM MESTRUCTOR 2 .375 3000 GHE, AR 0.2 TRD USI, PFS VALUR, FLDM MESTRUCTOR 12 .25 3000 GHE, AR 0.3 TRD USI, PFS VALUR, SOLEMOID 12 .25 3000 GHE, AR 2.5 TRD USI, PFS VALUR, SOLEMOID 1 .375 100 RZO 6.6 TRD USI, PFS VALUR, SOLEMOID 3 .25 50 GHE, AR 2.5 TRD USI, PFS VALUR, SOLEMOID 1 .10 14.7 ALL 0.6 TRD USI, PH DISCOMBECT, DISCORRECT, DISCO		USL, PFS	VALVE, CHECK	~	375.	100	H20	6.0	TBD	OST.
USL, PFS VALUE, FLOM RESTRICTOR 1 .375 100 REO GAB, AR 2.5 PDD USL, PFS VALUE, SOLEMOID 2 .375 100 REO 2.8 PD USL, PFS VALUE, SOLEMOID 1 .375 100 REO 2.8 PD USL, PFS VALUE, SOLEMOID 3 .25 50 GHE, AR 2.5 PD USL, PFH DISCORRECT, CALUE 1 1.0 14.7 ALL 0.9 PD USL, PHH DISCORRECT, CALUE 1 1.0 14.7 ALL 0.5 PD USL, PHH DISCORRECT, CALUE 1 2.2 14.7 ALL 0.5 PD USL, PHH DISCORRECT, CALUE 1 2.2 14.7 ALL 0.9 PD USL, PHH DISCORRECT, CALUE 1 2.2 14.7 ALL 0.9 PD USL, PHH DISCORRECT, CALUE 2 1 1 0.9 PD P		USL, PFS	VALVE, FLOW RESTRICTOR	~	.375	3000	GHE, AR	0.2	URT I	961
USI, PFS VALVE, SOLEMOID 12 .25 300 GHP, AR 2.5 TBD USI, PFS VALVE, SOLEMOID 2 .375 100 H2O 2.8 TBD USI, PFS VALVE, SOLEMOID 3 .25 50 GHE, AR 2.5 TBD USI, PFF DISCORNECT, 1 1.0 14.7 ALL 0.5 TBD USI, PMH DISCORNECT, 1 1.0 14.7 ALL 0.5 TBD USI, PMH DISCORNECT, 1 2.5 14.7 ALL 0.5 TBD USI, PMH DISCORNECT, 2 1.0 14.7 ALL 1.5 TBD USI, PMH DISCORNECT, 2 1.0 14.7 ALL 1.5 TBD USI, PMH DISCORNECT, 2 1.0 14.7 ALL 0.9 TBD USI, PMH DISCORNECT, 2 1.0 14.7 ALL 0.9 TBD USI, PMH		USL, PFS	VALVE, FIOW RESTRICTOR		375.	100	H20	0.3	Cer	OST.
USI, PFS UALIVE, SOLEMOLD 2 .375 100 HZO 2.9 TBD USI, PFS VALUK, SOLEMOLD 36 .25 50 GHE, AR 2.5 TBD USI, PRH DISCORNECT, 11 1.0 14.7 ALL 0.9 TBD USI, PMH DISCORNECT, 1 2.5 14.7 ALL 0.5 TBD USI, PMH DISCORNECT, 1 2.5 14.7 ALL 0.5 TBD USI, PMH DISCORNECT, 1 2.0 14.7 ALL 1.5 TBD USI, PMH DISCORNECT, 1 2.0 14.7 ALL 1.6 TBD USI, PMH DISCORNECT, 1 2.0 14.7 ALL 0.9 TBD USI, PMH DISCORNECT, 1 1.0 14.7 ALL 0.9 TBD USI, PMH DISCORNECT, 1 1.0 14.7 ALL 0.9 TBD USIS, PMH		USL, PFS	VALVE, SOLENOID	12	.25	3000	GHE, AR	2.5	TBD	OST.
USI, PFS UAILINE, SOLEMOLD 1 .375 100 RZO 6.6 TBA USI, PFS UAILINE, SOLEMOLD 36 .25 50 GHE, AR 2.5 TBA USI, PMH DISCONRECT, 11 1.0 14.7 ALL 0.9 TBA USI, PMH DISCONRECT, 1 .25 14.7 ALL 0.5 TBA USI, PMH DISCONRECT, 1 .25 14.7 ALL 1.5 TBA USI, PMH DISCONRECT, 1 .25 14.7 ALL 1.6 TBA USI, PMH DISCONRECT, 1 .20 14.7 ALL 1.6 TBA USI, PMH DISCONRECT, 1 .20 14.7 ALL 0.9 TBA USI, PMH DISCONRECT, 1 .2 .4 .2 .4 .2 .4 .4 .5 .8 .7 .8 .7 .8 .7 .8 .7 .8 .	76	USL, PFS	VALVE, SOLENOID	~	.375	100	HZO	2.8	Tab	OET.
USI, PFS VALIVE, SOLEMOTO 36 .25 50 GRE, AR 2.5 TBD USI, PMH DISCONNECT, 11 1.0 14.7 ALL 0.9 TBD USI, PMH DISCONNECT, 1 .25 14.7 ALL 0.5 TBD USI, PMH DISCONNECT, 1 .25 14.7 ALL 1.5 TBD USI, PMH DISCONNECT, 1 .2 14.7 ALL 1.6 TBD USI, PMH DISCONNECT, 1 .2 14.7 ALL 0.9 TBD USI, PMH DISCONNECT, 3 .25 14.7 ALL 0.9 TBD USI, PMH DISCONNECT, 1 0.9 TBD 0.9 TBD USI, PMH DISCONNECT, 1 0.9 TBD 0.9 TBD		USL, PFS	VALVE, SOLENOID		375.	100	HZ0	9.6	TBD	081
USL, PWH DISCORNECT, 11 1.0 14.7 ALL 0.9 TBD USL, PWH DISCORNECT, 4 .25 14.7 ALL 0.5 TBD USL, PWH DISCORNECT, 1 .25 14.7 ALL 1.5 TBD USL, PWH DISCORNECT, 10 2.0 14.7 ALL 1.9 TBD USL, PWH DISCORNECT, 12 1.0 14.7 ALL 0.9 TBD USL, PWH DISCORNECT, 3 .25 14.7 ALL 0.9 TBD USL, PWH DISCORNECT, 18 1.0 14.7 ALL 0.9 TBD USL, PWH DISCORNECT, 18 1.0 14.7 ALL 0.9 TBD USL, PWH DISCORNECT, 18 1.0 14.7 ALL 0.9 TBD USL, PWH DISCORNECT, 18 1.0 14.7 ALL 0.9 TBD		USL, PFS	VALVE, SOLENOID	36	.25	90	GHE, AR	2.5	TBD	178D
USL, PMH DISCONNECT, 4 .25 14.7 ALL 0.5 TRD USL, PMH DISCONNECT, 1 .25 14.7 ALL 1.5 TBD USL, PMH DISCONNECT, 10 2.0 14.7 ALL 1.8 TBD USL, PMH DISCONNECT, 12 1.0 14.7 ALL 0.9 TBD USL, PMH DISCONNECT, 3 .25 14.7 ALL 0.9 TBD USL, PMH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD USL, PMH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD USL, PMH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD		USL, PWH	DISCONNECT,	11	1.0	14.7	ALL	6.0	1360	TBD
USI, PWH DISCONNECT, 1 .25 14.7 ALL 1.5 TBD USI, PWH DISCONNECT, 10 2.0 14.7 ALL 1.6 TBD USI, PWH DISCONNECT, 72 1.0 14.7 ALL 0.9 TBD USI, PWH DISCONNECT, 3 .25 14.7 ALL 0.5 TBD USI, PWH DISCONNECT, 18 1.0 14.7 ALL 0.5 TBD USI, PWH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD USI, PWH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD		USL, PWH	DISCONNECT,		.25	14.7	ALL	0.5	TBD	780
USL, PMH DISCONNECT, 10 2.0 14.7 ALL 1.8 TBD USL, PMH DISCONNECT, 72 1.0 14.7 ALL 0.9 TBD USL, PMH DISCONNECT, 3 .25 14.7 ALL 0.5 TBD USL, PWH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD USL, PWH ENGINE, BUNNER, CATRLYTIC 2 2.0 TBD 60.01 TBD		UST, PWH	DI SCONNECT,		.25	14.7	YIT Y	1.5	OBT 1	1360
USL, PWH DISCONNECT, 72 1.0 14.7 ALL 0.9 TRD USL, PWH DISCONNECT, 3 .25 14.7 ALL 0.5 TBD USL, PWH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD USL, PWH ENGINE, BUNNER, CATRLYTIC 2 2.0 TBD 60.01 TBD		USI, PWH	DI SCONNECT,	<u>s</u>	2.0	14.7	ALL	1.8	TBD	130
USE, PWH DISCONNECT, 3 .25 14.7 ALL 0.5 TBD USE, PWH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD USE, PWH ENGINE, BUNNER, CATRIYTIC 2 2.0 TBD 60.01 TBD		USL, PWH	DI SCONNECT,	72	1.0	14.7	ALL	6.0	TBD	TBD
USIL, PWH DISCONNECT, 18 1.0 14.7 ALL 0.9 TBD USIL, PWH USIL, PWH TBD 1780 TBD 60.01 TBD 60.01 TBD		USL, PWH	DI SCONNECT,		.25	14.7	ALL	0.5	OEL -	TBD
USL, PMH ENGINE, BUINER, CATALYTIC 2 2.0 TBD 60.01 TBD 60.01 TBD		USI, PWH	DI SCONNECT,	8.	1.0	14.7	ALL	6.0	1780	OBT.
		USL, PWH	ENGINE, BURNER, CATALYTIC	~	2.0	OET	TBD	60.01	TBD	- TBO

Table 1.3-3 (Continued) USL Process Material Management System Component List

10 105, PM	THE AND THE AN		1900 300 300 300 14.7 14.7 100 14.7 14.7 14.7 14.7 14.7 11.7 11.7 11.7 11.7 11.7	NT N	1.0 c 8 0.3 0.8 0.8 0.8 0.8 0.8 0.8 0.8 0.8 0.3 0.8 0.8 0.3 0.8 0.8 0.8 0.8 0.8 0.8 0.8 0.8 0.8 0.8		087 087 087 087 087 087 087 087 087
	INE PRODUCTION SUCTION SUCTION TEFLON LINED TEFLON LIN		100 300 300 300 14.7 14.7 100 14.7 14.7 114.7 114.7 1100 1100	41 A A A A A A A A A A A A A A A A A A A	1.0 141.1 13.0 0.4 0.5 0.8 0.5 0.3 0.3	130 130 130 130 130 130 130 130 130 130	
USL, PWH CES, COMPRESSOR, REPLICERATION USL, PWH USC, COMPRESSOR, REPLICERATION USC, PWH USC, FLEX HOSE, SUCTION USC, PWH USC, FLEX HOSE, TREION LINED USC, PWH USC, FLEX HOSE, TREION LINED USC, PWH USC, FLEX HOSE, TREION LINED USC, PWH USC, PLEX HOSE, TREION LINED USC, PWH USC, PUSCH, UNIT, PORTABLE PRESSURE VESSEL, MASTE HOLDING USC, PWH SENSOR, PLCSWIRE USC, PWH SENSOR, PLCSWIRE USC, PWH SENSOR, PLCSWIRE USC, PWH SENSOR, PLCSWIRE USC, PWH SENSOR, PRESSURE USC, PWH SENSOR, PRE	LIAZ PRODUCTION LIAZ PRODUCTION SUCTION TEPLON LINED TEPL		100 300 300 300 14.7 14.7 14.7 14.7 14.7 14.7 100 11.7 100 11.7 100 11.7 100	ALL	141.1 13.0 0.4 0.5 0.8 0.8 0.8 0.8 0.9	1390 1390 1390 1390 1390 1390 1390 1390	067 067 067 067 067 067 067 067 067 067
HEST, COMPRESSOR, REPAIGNANGE, PARTICERATION HEST, CRYC ORIT, LAZ PRODUCTION HEST, CRYC ORIT, LAZ PRODUCTION HEST, FILEX HOSE, TETAN LINED HEST, FILEX HOSE, TETAN			300 300 300 14.7 14.7 14.7 14.7 14.7 14.7 14.7 100 17.7100 125 TORRV14.7 TBD	477 477 477 477 477 477 477 477 477 477	141.1 33.0 0.4 0.5 0.8 1.9 0.5 0.8 0.3	130 130 130 130 130 130 130 130 130 130	OET
HISC, CRYO UNIT, IAP PRODUCTION USI, PWH HISC, DIFFUSER, SUCTION USI, PWH HISC, FIEX HOSE TFILON LINED USI, PWH HISC, PIEX HOSE TFILON LINED USI, PWH HISC, PUER HOSE TFILON LINED USI, PWH HISC, PUER HOSE TFILON LINED USI, PWH HISC, PUER USI, PWH HISC, PUER USI, PWH HISC, PUER USI, PWH HISC, PUER USI, PWH HISC, VACUON UNIT, PORTBALE USI, PWH PRESSURE VESSEL, MATERIAL TRANS. CONT. USI, PWH SENSOR, PUESSUR, MATERIAL TRANS. CONT. USI, PWH SENSOR, PUESSUR USI, PWH SENSOR, PUESSURE USINGRA	LAZ PRODUCTION SUCTION TEPLON LINED TEPLON L		300 300 14.7 14.7 100 14.7 14.7 14.7 100 11.7/100 25 TORR/14.7 TBD	7 T	33.0 0.4 0.6 0.5 0.8 0.5 0.3 0.3	130 130 130 130 130 130 130 130 130 130	067 067 067 067 067 067 067 067 067 067
HISC, FIEX HOSE HISC, FIEX HOSE GET PART HOSE HISC, FIEX HOSE HISC, FIEX HOSE HISC, FIEX HOSE HISC, FIEX HOSE HISC, FIEX HOSE TFILON LINED HISC, PUMP HISC, PUMP HISC, PUMP HISC, PUMP HISC, PUMP HISC, PUMP HISC, PUMP	TEPLON LINED TEPLO		300 300 14.7 14.7 100 14.7 14.7 14.7 100 15.7/100 25 TORR/14.7 TBD		0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	130 130 130 130 130 130 130 130 130	087 087 087 087 087 087 087 087
HISC, FIEX HOSE HISC, FIEX HOSE TEVINA LINED HISC, FIEX HOSE, TEVINA LINED HISC, FUNE HISC, PUNE HISC	TEPLON LINED TEPLO		300 14.7 14.7 100 14.7 14.7 14.7 100 14.7/100 .25 TORR/14.7 TBD		0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	730 730 730 730 730 730 730 730 730 730	081 081 081 081 081 081 081 081
USI, PWH HISC, FLEX HOSE, TETON LINED	TEPLON LINED TEPLO		14.7 14.7 100 14.7 14.7 14.7 100 14.7 100 125 TORR/14.7 TBD		0.8 1.9 0.8 0.8 0.8 10.0	780 780 780 780 780 780 780 780 780 780	061 081 081 081 081 081 081
USI, PWH HISC, FLEX HOSE, TEPLON LINED HISC, PLUE HISC, PUPE, VACUUM HISC, PUPE, PUPE, VACUUM PURESCURE VESSEL, PUPE, PUPE	TEPLON LINED TEPLO		14.7 100 14.7 14.7 14.7 100 14.7/100 .25 TORR/14.7 TBD		0.8 1.9 0.8 0.8 0.8 10.0	130 CT 13	067 087 087 087 087 087 087
USI, PWH HISC, FLEX HOSE, TEPION LINED HISC, PLUE HISC, PUPE PUPE SURE VESSEL, PUPE PUPE SURE VESSEL, PUPE PUPE SURE VESSEL, PUPE HISCS, PUPE PUPE SURE VESSEL, PUPE HISCS, PUPE HISC	TEFLON LINED TEFLO		100 14.7 14.7 14.7 100 14.7/100 .25 TORR/14.7 TBD	T	1.9 0.8 0.3 0.8 10.0	TBD	080 080 080 080 080 080 080 080
USL, PWH HISC, FLEX HOSE, TEPLON LINED	TETON LINED TO THE TETON L		14.7 14.7 14.7 14.7 100 14.7/100 .25 TORRA/14.7 TBD	7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	0.5 0.3 0.8 10.0	130 130 130 130	081 081 081 081 081 081 081
HISC, FLEX HOSE, TEPION LINED HISC, FLEX HOSE, TEPION LINED HISC, FLEX HOSE, TEPION LINED HISC, PRETREATHENT UNIT, MASTE HISC, PUMP, VACUUM HISC, PUMP, PUSSEUR, PUSS	TEPLON LINED TEPLON LINED TEPLON LINED NT UNIT, MASTE LIM GAS/LIQUID T. PORTABLE		14.7 14.7 14.7 100 14.7/100 .25 TORAV14.7 TBD 100	X X X X X	0.8 0.8 0.0 10.0	130 130 130	081 081 081 081 081 081
USI, PWH HISC, FLEX HOSE, TETION LINED USI, PWH HISC, PRETREATHENT UNIT, MASTE HISC, PUMP HISC, PUMP USI, PWH HISC, PUMP, VACUUM USI, PWH HISC, PUMP, VACUUM USI, PWH HISC, PUMP, VACUUM MISC, TIMES UNIT PRESSURE VESSEL, USI, PWH PRESSURE VESSEL, USI, PWH PRESSURE VESSEL, LIQUID MASTE USI, PWH PRESSURE VESSEL, MASTE CONTAINENT USI, PWH PRESSURE VESSEL, MASTE ROLDING USI, PWH PRESSURE VESSEL, MASTE ROLDING USI, PWH SENSOR, PLOM METER USI, PWH SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE S	TEPION LINED TEPION LINED NT UNIT, MASTE UM GAS/LIQUID		14.7 14.7 100 14.7/100 .25 TORAV14.7 TBD 100	אַד אַד אַד	0.3 0.0 10.0 22.9	Oer	081 180 081 081 081 081
USI, PWH HISC, PLEE HOSE, TELON LINED USI, PWH HISC, PUMP USI, PWH HISC, PUMP USI, PWH HISC, PUMP USI, PWH HISC, PUMP USI, PWH HISC, TIMES UNIT MISC, TIMES UNIT PORTABLE MISC, TIMES UNIT PRESSURE VESEL, PRESSURE VESEL, LIQUID MASTE PRESSURE VESEL, LIQUID MASTE PRESSURE VESEL, MATERIAL TRANS. CONT. USI, PWH PRESSURE VESEL, MASTE CONTAINENT PRESSURE VESEL, MASTE CONTAINENT PRESSURE VESEL, MASTE CONTAINENT USI, PWH PRESSURE VESEL, MASTE ROLDING USI, PWH RECULATOR, SENSOR, FLOM METER SENSOR, FLOM METER USI, PWH SENSOR, PLOM METER SENSOR, PRESSURE SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE	HOSE, TEFION LINED REALFENT UNIT, MASTE , VACJUM BAITOR, GAS/LIQUID S. UNIT, PORTMALE	1.0 2.0 2.0 2.0 TBD	14.7 100 14.7/100 .25 TORAV14.7 TSD 100	NIT WIT	10.0	QE: 1	130 130 130 130 130
USI, PWH HISC, PURP USI, PWH HISC, PUMP USI, PWH HISC, PUMP, VACUUM USI, PWH HISC, SEPARATOR, GAS/LIQUID MISC, TIMES UNIT MISC, TIMES UNIT MISC, TIMES UNIT PORTBALE MISC, TIMES UNIT PORTBALE MISC, PWH PRESSURE VESEL, LIQUID MASTE PRESSURE VESEL, LIQUID MASTE PRESSURE VESEL, MATERIAL TRANS. CONT. USI, PWH PRESSURE VESEL, MASTE CONTAINENT PRESSURE VESEL, MASTE CONTAINENT PRESSURE VESEL, MASTE GAS USI, PWH PRESSURE VESEL, MASTE ROLDING USI, PWH RECULATOR, SENSOR, FLOM METER SENSOR, PLOM METER USI, PWH SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE SENSOR, PRESSURE	REALFENT UNIT, MASTE , VACJUM BAIOR, GAS/LIQUID S. UNIT, PORTABLE	2.0 2.0 2.0 TBD 335	100 14.7/100 .25 TORA/14.7 TBD 100	ALL	10.0		08T 18D 08T 18T 18T
HISC, PUNE HISC, PUNE	, VACJUM BATOR, GAS/LIQUID S UNIT PORTABLE	2.0 2.0 TBD .375	14.7/100 .25 TORA/14.7 TBD 100	ALL	22.9	OSL	
USI, PWH HISC, PUME, VACUUM USI, PWH HISC, SEPARATOR, GAS/LIQUID USI, PWH HISC, TIMES UNIT USI, PWH HISC, TIMES UNIT MISC, PWH HISC, WACUUM UNIT, PORTABLE PRESSURE VESSEL, LIQUID MASTE PRESSURE VESSEL, LIQUID MASTE USI, PWH PRESSURE VESSEL, MATERIAL TRANS. CONT. USI, PWH PRESSURE VESSEL, MASTE CONTAINENT USI, PWH PRESSURE VESSEL, MASTE CONTAINENT USI, PWH PRESSURE VESSEL, MASTE GAS USI, PWH PRESSURE VESSEL, MASTE GAS USI, PWH SENSON, FLOM METER USI, PWH SENSON, PLOM METER USI, PWH SENSON, PRESSURE	RATOR, GAS/LIQUID S. UNIT. PORTABLE	3.0 TBD .375	.25 TORK/14.7 TBD 100	1.14		ORT	OET
USI, PWH HISC, SEPARATOR, CAS/LIQUID USI, PWH HCSC, TIMES UNIT USI, PWH HCSC, VACUM UNIT, PORTABLE USI, PWH PRESSURE VESSEL, PRESSURE VESSEL, LIQUID MASTE PRESSURE VESSEL, MATERIAL TRANS, CONT. USI, PWH PRESSURE VESSEL, MATERIAL TRANS, CONT. USI, PWH PRESSURE VESSEL, MASTE CONTAINENT PRESSURE VESSEL, MASTE CONTAINENT PRESSURE VESSEL, MASTE CONTAINENT USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH SENSON, FLOM METER USI, PWH SENSON, FLOM METER USI, PWH SENSON, PRESSURE USI, PWH SENSON, PRESSURE USI, PWH SENSON, PRESSURE USI, PWH SENSON, PRESSURE USI, PWH SENSON, TEMPERATURE USI, PWH SENSON, TEMPERATURE USI, PWH SENSON, TEMPERATURE	RATOR, GAS/LIQUID S. UNIT. UN UNIT, PORTABLE	.375	100	1	550.1	1780	CELL -
USI, PWH HTSC, TIMES UNIT USI, PWH PRESSURE VESEL, USI, PWH PRESSURE VESEL, PRESSURE VESEL, LIQUID MASTE LIGUID WASTE USI, PWH PRESSURE VESEL, MATERIAL TRANS. CONT. USI, PWH PRESSURE VESEL, MASTE CONTAINENT USI, PWH PRESSURE VESEL, MASTE CONTAINENT USI, PWH PRESSURE VESEL, MASTE CANTAINENT USI, PWH SENSOR, FLOM METER USI, PWH SENSOR, FLOM METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, TOW METER USI, PWH SENSOR, TOW METER USI, PWH SENSOR, TOW METER USI, PWH SENSOR, TEMPERATURE USI, PWH VALVE, CHECK	S UNIT. UH UNIT, PORTABLE	. 375 TBD	100	MIL	12.0	130	
USI, PWH HTSC, VACUM UNIT, PORTABLE USI, PWH PRESSURE VESEL, USI, PWH PRESSURE VESEL, LIQUID MASTE USI, PWH PRESSURE VESEL, MATERIAL TRANS. CONT. USI, PWH PRESSURE VESEL, MASTE CONTAINENT USI, PWH PRESSURE VESEL, MASTE CONTAINENT USI, PWH PRESSURE VESEL, MASTE CONTAINENT USI, PWH PRESSURE VESEL, MASTE COLLING USI, PWH PRESSURE VESEL, MASTE HOLDING USI, PWH SENSOR, FLOM METER USI, PWH SENSOR, FLOM METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH USI, PWH	UM UNIT, PORTABLE	OET		H20	95.0	HAMILTON STANDARD	130
USI, PWH PRESSURE VESEL, USI, PWH PRESSURE VESEL, USI, PWH PRESSURE VESEL, LIQUID WASTE USI, PWH PRESSURE VESEL, MATE CONTINEXT USI, PWH PRESSURE VESEL, MASTE CASA USI, PWH PRESSURE VESEL, MASTE CASA USI, PWH PRESSURE VESEL, MASTE CONTINEXT USI, PWH PRESSURE VESEL, MASTE HOLDING RECULATOR, RECULATOR, USI, PWH SENSOR, FLOM METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH USI, PWH		_	OEL.	ALL	10.0	1780	1380
USI, PWH PRESGURE VESEL, USI, PWH PRESSURE VESEL, LIQUID MASTE USI, PWH PRESSURE VESEL, MASTE CONTINHENT USI, PWH PRESSURE VESEL, MASTE CONTINHENT USI, PWH PRESSURE VESEL, MASTE GAS USI, PWH PRESSURE VESEL, MASTE HOLDING USI, PWH PRESSURE VESEL, MASTE HOLDING USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, PLOW METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE	יייים פריי	5.0	OBL	MIL	14.0	1780	TBD
USI, PWH PRESSURE VESEL, LIQUID MASTE USI, PWH PRESSURE VESEL, MASTE CONTINHENT USI, PWH PRESSURE VESEL, MASTE CONTINHENT USI, PWH PRESSURE VESEL, MASTE GAS USI, PWH PRESSURE VESEL, MASTE HOLDING USI, PWH REGULATOR, RESSURE VESEL, MASTE HOLDING USI, PWH REMOR, FLOW METER USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, PRESSURE VESEURE USI, PWH SENSOR, PRESSURE VESEURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE	ESSEL,	.375	OBT.	BRINE	7.5	13D	TBO
USI, PWH PRESSURE VESSEL, MASTE CONTAINENT USI, PWH PRESSURE VESSEL, MASTE CONTAINENT USI, PWH PRESSURE VESSEL, MASTE GAS USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH VALVE, CHECK		.25	OBT	MIL	5.0	TBD	136D
USI, PWH PRESSURE VESSEL, MASTE CONTAINENT USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH PRESILIATOR, FLOW METER USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, OUALITY MONITOR USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH VALUE, CHECK	MATERIAL TRANS.	OBT	OET.	MIL	6.6	1360	OBT
USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH PRESSURE VESSEL, MASTE HOLDING USI, PWH PRESULTOR, PLOM METER USI, PWH SENSOR, FLOM METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, QUALITY MONITOR USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH VALUE, CHECK		 52:	OET.	MIL	16.0	1780	TBO
USI, PWH PRESULEDING USI, PWH REGULATOR, USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, FLOW METER USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, PRESSURE USI, PWH SENSOR, QUALITY MONITOR USI, PWH SENSOR, TEMPERATURE USI, PWH SENSOR, TEMPERATURE USI, PWH VALUE, CHECK	ESSEL, WASTE GAS	5.0	OBT	ALL	703.4	130	TBD
USL, PWH REGULATOR, USL, PWH SENSOR, FLOM METER USL, PWH SENSOR, FLOM METER USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, OLALITY MOLITOR USL, PWH SENSOR, TEMPERATURE USL, PWH SENSOR, TEMPERATURE USL, PWH VALVE, CHECK	ESSEL, WASTE HOLDING	5.0	ORL	MLL	15.0	TBO	1380
USL, PWH SENSOR, FLOW METER USL, PWH SENSOR, FLOW METER USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, TEMPERATURE USL, PWH SENSOR, TEMPERATURE USL, PWH VALVE, CHECK		1:0	OBT	MLL	2.0	TBD	OBT -
USI, PWH SENSOR, PLOM METER USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, QUALITY WONITOR USL, PWH SENSOR, TEMPERATURE USL, PWH VALVE, CHECK	ON METER	TBO	14.7	MLL	8.0	1780	OBT
USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, PRESSURE USL, PWH SENSOR, QUALITY WANTOR USL, PWH SENSOR, TEMPERATURE USL, PWH VALVE, CHECK	ON METER	12 TBD	14.7	MIL	0.8	TBD	OBT
USL, PMH SENSOR, PRESSURE USL, PMH SENSOR, QUALITY MONITOR USL, PMH SENSOR, TEMPERATURE USL, PMH VALVE, CHECK	ESSURE	65 TBO	14.7	ALI.	•·•	1360	OBT
USL, PWH SENSOR, QUALITY MONITOR USL, PWH SENSOR, TEMPERATURE USL, PWH SENSOR, TEMPERATURE USL, PWH VALUE, CHECK	ESSURE.	OBT 1	OFF.	ALL	7.0	TBD	OBL
USL, PMH SENSOR, TEMPERATURE USL, PMH SENSOR, TEMPERATURE USL, PMH VALVE, CHECK	ALITY MONITOR	2 TBO	Off	H20	22.1	130	TBO
USL, PWH	PPERATURE	14 TBO	OBEL	MIL	0.1	TBD	1380
USI, PWH	PREMATURE	OET + 1	OET	H20	1.1	TBD	1780
	CK	3	OET	ALL	9.0	TBD	OBT
71 USL, PMH VALVE, CHECK 3		3 1375	OET	ALL	6.0	TBD	TBD
52 USL, PMR VALVE, RELIEF 1	IEF	. 25	OEL .	ALL	1.5	1380	TBD
53 USL, PWH VALVE, RELIEF 2	LEF	Z TBD	OST.	ALL	3.9	TBD	13D
79 USL, PWH 1 VALVE, RELIEF	TEF	. 25	TBO	ALL	1.5	TBD	TBD

All includes HE, AR, H20, R, CO2

Table 1.3-3 (Continued) USL Process Material Management System Component List

M	PROGRAM APPLICATON	COMPONENT TYPE	QUAN REQD	SIZE (in)	PRESSURE MEOP (pola)	USAGE	APPROX HASS (1b)	VENIOR NAME	VENDOR PART NUMBER
	38 USL, PWH	VALVE, SOLENOID		1.0	130	VII.	2.5	UBC .	oer -
.	63 USL, PWH	VALVE, SOLENOID	~	TBO	OBT.	ALL	1.7	Tab	OBT
	74 USL, PWH	VALVE, VENT ASSY	~	2.0	OET	VET.	3.9	1380	

All includes HE, AR, H20, FR, C02

Process Fluids Storage

Process fluids can be separated into three separate storage categories; .

1) USL dedicated PMMS storage, 2) Space Station integrated fluids storage and user unique storage. Fluids which require USL dedicated storage include helium, argon, carbon dioxide gases and some water. Potable water will be obtained through excess potable water generation from the ECLSS and Orbiter fuel cells. A separate dedicated storage facility will be located in the laboratory to provide for the necessary water accumulation.

Integrated fluids include excess oxygen and possibly excess hydrogen generated from the ECLSS which may be available for payload use. These fluids, along with nitrogen, transferred from the integrated nitrogen system, will not require dedicated storage in the USL. User unique fluids refer to the remainder of the fluids required by USL payload equipment which also do not require dedicated storage and must be provided by the users.

Helium, Argon, carbon dioxide, and water will be stored in a combination of racks located in the USL floor. Figure 1.3-2 shows the general design concept for the storage and fluid distribution of these fluids. The three gases will be stored under pressure in two types of vessels. Carbon dioxide, and small quantities of helium and argon will be stored in small portable pressure vessels (PPV) at 2000 psia. These vessels will be approximately 14 inch by 6 inch cylinders designed to fit both the fluid storage rack and the fluid user rack. The other gas storage vessel will be a high operating pressure vessel which feeds helium and argon into a general hardline distribution system to the experiments. These vessels will be approximately 30 inch by 9 inch cylinders which operate up to 3000 psia. Nitrogen will be supplied by the Integrated Nitrogen System (INS) located on the station truss structure.

Providing hydrogen presents several safety related design concerns. Hydrogen gas is explosive in nature, therefore large concentrations of hydrogen gas quantities should be avoided. Hydrogen supplied from the ECLSS will be transferred to the USL module and stored in tanks that are approximately 33.7 ft³ in volume.

Oxygen will also be supplied from the ECLSS system. Presently, this is the only source necessary to meet the 90 day resupply requirement.

Water may be supplied to the dedicated storage facility from the integrated water system which receives excess water from several sources. These sources include excess potable water generated from the ECLSS and the Orbiter fuel cells. The dedicated water storage tank will be capable of holding 992.3 1bm of water at a storage pressure of 100 psia.

Process Fluid Distribution

The PMMS will supply fluids to user equipment by two methods. Water, nitrogen, oxygen, argon and helium will be transferred directly from the storage facility to the user. Carbon dioxide and portions of argon and helium will be supplied from portable pressure vessels (PPV), which can be plugged directly into the user rack.

Processed Water Design Concept

Water quality requirements vary among different users. Twenty-six users require various water purities ranging from potable to deionized and pyrogen-free water as shown in Table 1.3-4. The potable water in the storage tank must be purified to meet the needs of the deionized/pyrogen free water users.

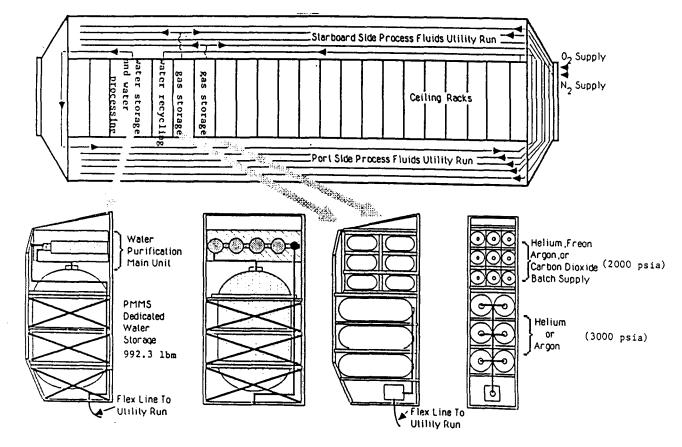


Figure 1.3-2 General Design Concept for USL Storage and Distribution

Table 1.3-4 Process Water Purity Requirements

Equipment Name	Potable	Distilled	Deionized	Pyrogen-free
Automated Cutting and Polishing	X			
Analytical Scale			X	X
Acoustic Levitator		X		
Atmospheric Microphysics Facility			X	
Optical Fiber Pulling	TBD	TBD	TBD	TBD
High Temperature Furnace		X	X	
Auto Ignition			X	
Droplet Spray Burning			. X	
Continuous Flow Electrophoresis			X	X
Free Float		X		
High Performance Liquid				
Chromatograph	TBD	TBD	TBD	TBD
Isoelectric Focusing			X	X
Organic and Polymer			X	X
Membrane Production			X	
Microwave Steam Autoclave	TBD	TBD	TBD	TBD
Protein Crystal Growth			X	X
Solution Crystal Growth			X	
Small Bridgeman	X			
Electrostatic Levitator		X		
EM Levitator		X		
Float Zone	TBD	TBD	TBD	TBD
Fluid Physics			X	
Premixed Gas Combustion			X	
Rotating Spherical Convection		X		
Solid Surface Burning			X	

Figure 1.3-3 shows the water supply design concept for the PMMS. Potable water will be mixed in a common line which feeds the main deionized/depyrogenation unit. The main unit which will be a combination of multifiltration units linked in series with an ultrafiltration device. The output water, which will meet all purity specifications, will then transferred to the users through utility runs in 3/8 inch tubing.

Cryogenics

The cryogenic facility shown in Figure 1.3-4 will be a closed loop helium system designed to provide cooling to the experiments. The hardware that will comprise the refrigeration system includes a compressor package, a cold head and a distribution line. The compressor package will include a water cooled reciprocating compressor, a heat exchanger, and the associated electrical controls. The cold head will be composed of one or two stage Sterling Cycle expansion device for LN2 generation and the distribution line will provide a means for the supply and return of helium. This closed loop cryogenic refrigeration cycle will not require helium resupply with the exception of makeup for helium leakage.

A small quantity of liquid nitrogen has been requested to support the Critical Point Facility. Gaseous nitrogen will be supplied from the ECLSS system and transferred into the cold head dewar. Cooled by the helium refrigeration system, the nitrogen will then be transferred to users.

1.3.3.2 Process Waste Handling System - The Process Waste Handling System (PWHS) will be responsible for the safe removal, storage and disposal of USL payload waste by-products. An overview of the (PWHS) is provided in Figure 1.3-5. The source of waste will be from payload experiments, support equipment, and processes including a laminar flow work bench, fluids and particular glovebox, emergency shower, and eyewash. A component list of the PWHS is provided in Table 1.3-3.

Figure 1.3-6 shows a layout of a typical rack in which three phase waste will be produced and the associated hardware required to provide the necessary waste management functions. The associated hardware will make up the waste handling assembly which will be required in all payloads requiring gas/liquid separation.

The waste handling assembly will be a vacuum contained housing for the waste handling hardware. The system provides a dynamic recirculation loop for removing liquids from waste gases. When the liquid has been removed, the waste gas is diverted to the Waste Gas Handling System and the experiment is purged.

Gas/Liquid Separation

Spacelab water separators, modified for corrosive conditions will be used to provide gas/liquid separation. The separators are capable of providing three times the liquid pumping capability required in the USL and are physically larger than is desired for the USL. The predicted efficiency of the separator is approximately 99% which means that approximately 1% of all the liquid waste listed in Table 1.3-5 will be transferred into the waste gas handling system and possibly in the integrated waste management system. Liquid/gas separators will be provided in three facilities, the life science glove box, the crystal growth experiment and the materials glove box.

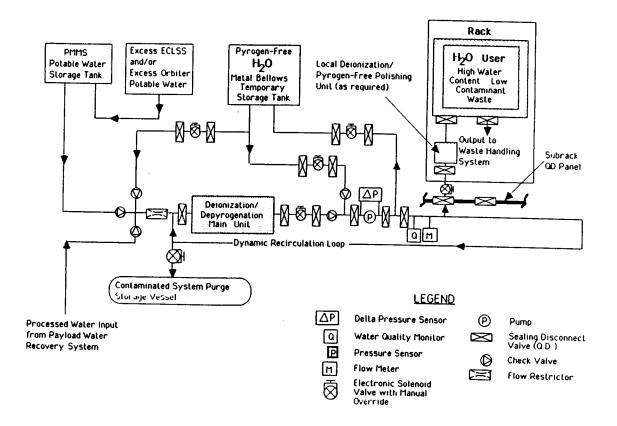


Figure 1.3-3 PMMS Water Supply Design Concept

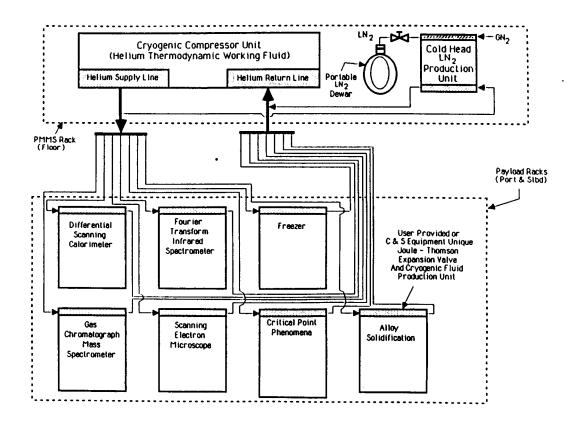


Figure 1.3-4 USL Cryogenic Refrigeration System

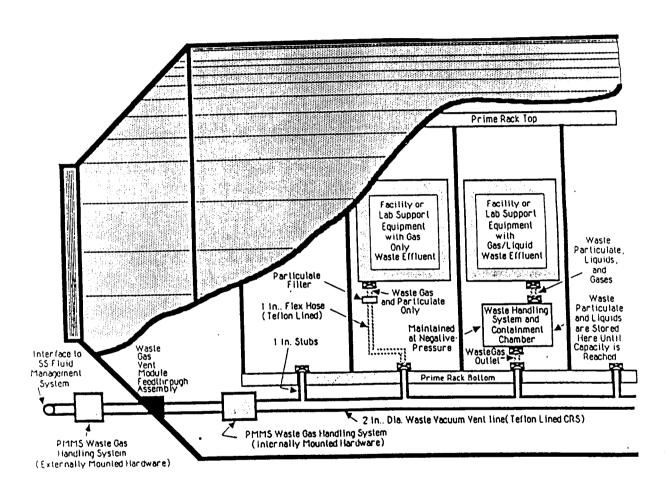


Figure 1.3-5 Overview of the Process Waste Handling System

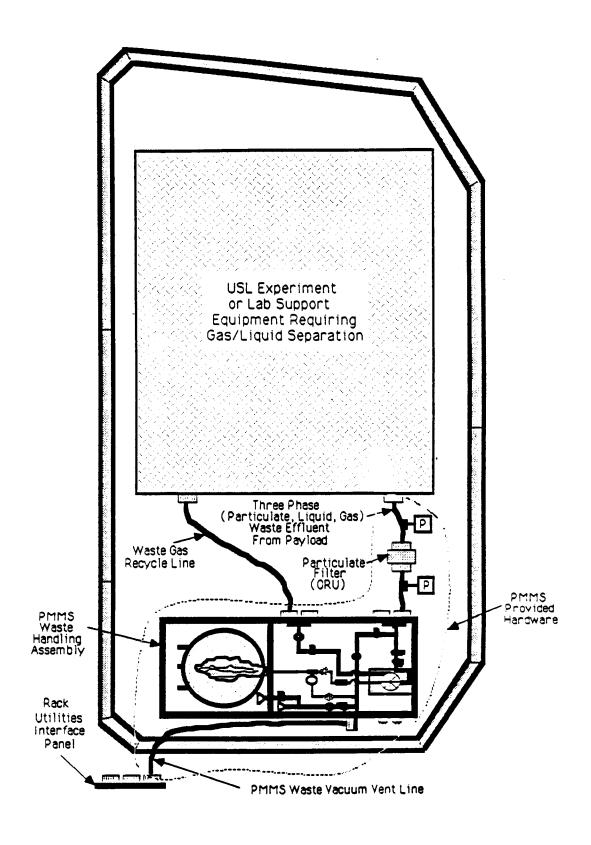


Figure 1.3-6 Process Waste Handling System Design Concept

Table 1.3-5 Liquid and Gaseous Wastes from USL Experiments

LIQUIDS

ORGAN	ICS

Toluene
Freon 22(Chlorodifluoromethane)
Freon 113(Trichlorotrifluoroethane)
Allyl Alcohol

N-Butyl Alcohol
Cyclohexanol
Isopropyl Alcohol

Phenol Acrolein

Trimethyl Benzene

Indene Xylene Diisebutyl Ketone Methylethyl Ketone

Furan
Butyl Lactate
Dichloromethane
Trichloroethane

Polyphenylene Sulfides TGS Solution (Triglycene Sulfate)

Spent TGS Solution Gluderaldehyde

INORGANICS

Ammonia Latex Solution Water

SOLVENTS

Benzene Trichloroethylene Acetone

ETCHANTS (USED PRIMARILY IN THE GLOVEBOX)

Hydro-fluoric Acid [HF] Nitric Acid (HNO3) Acetic Acid [(CH3CO)20] Silver Nitrate [AgNO₃] Magnesium Iodide [MgI₂] Hydrogen Peroxide [H₂O₂] Water [H₂O] Sodium Hydroxide [NaOH] Cupric Nitrate [Cu(NO₃)₂] Bromine [Br₂] Sodium Hypochlorite [NaOCl] Potassium Hydroxide [KOH] Potassium Ferricyanide [K3Fe(CN]6 Hydrochloric Acid [HC1] Methanol [CH3OH] Perchloric Acid

OTHER LIQUID WASTE SOLUTIONS

Buffer Solution
Culture Medium
Staining Solution
Liquid Chromatography Carrier
Ultra Pure Wash Water
Raw Protein Solution
Cleaning Solution
Developer
Fixer
Biocide/Disinfectant
Quench Solution
Burn Catalytic and
Suppressant Compounds
Polishing Solution
Monomer Solution

GASES

MONATOMIC, DIATOMIC, AND LIGHT GASES

 $\begin{array}{ccc} \mathrm{O}_2 & & \mathrm{He} \\ \mathrm{N}_2 & & \mathrm{Ar} \\ \mathrm{H}_2 & & \mathrm{H}_2\mathrm{O} \\ \mathrm{CO}_2 & & \mathrm{Xe} \\ \mathrm{CO} & & \end{array}$

OTHER GASES

Light Hydrocarbons
Halogens:
Cl₂
F₂
Freon 22
Freon 113
Organic Vapors
Halon

Unrecoverable Liquid Waste Storage

Liquid waste will consist of both organic and inorganic solvents, acids, bases, buffer solutions, and etchants with the majority of the liquid waste as water. The waste liquid, once separated from the gas stream will be pumped by the output pressure of the gas/liquid separator to a storage tank. The storage tank will be a 13.8 inch I.D. spherical tank. The outter structure will be aluminum with a Teflon lining. Also a butyl rubber bladder and a pressure port on the dry side of the bladder will enable waste liquid discharge and ground refurbishment. When the tank has reached its storage capacity it will be removed by the crew and transferred to the logistics module and replaced with an empty tank. Provisions must be made in the logistics module to accommodate the waste liquid quantities.

Water recovery from these waste fluid mixtures reduces the weight and cost of de-orbiting waste fluid quantities. There are several candidate facilities for waste water recovery including the Continuous Flow Electrophoresis (CFE), Protein Crystal Growth, Solution Crystal Growth, Organic and Polymer Crystal Growth and Isoelectric Focusing. The water recovery system presented in Figure 1.3-7 will be included in the water supply concept to illustrate how the systems will be integrated. User equipment which meets recoverable water standards will be connected to the system through a 3/8 inch waste line. At the point of leaving the multifiltration unit, the water will be pure enough to be mixed in with the main supply water for processing and delivery back to the users.

Gaseous Waste Handling

A major function of the PMMS will be the disposition of USL waste gases. Due to recent tightening of external contamination requirements, continuous venting from the waste handling system was restricted. As a result, the Waste Gas Handling System (WGHS) will be designed to store all waste gases generated by USL payloads for a 14 day period. This requirement was devised to accommodate the external attached payload's viewing clarity and duration.

Compatible gases will be transferred into the integrated waste fluid system at ambient temperatures and pressures ranging from .005 to 14.7 psia through a two-inch interface. As shown in Figure 1.3-5 unburned combustibles, from combustion experiments, air and inert gases are all dumped into a waste gas vacuum vent line. To minimize the possibility of a combustion reaction taking place in the WGHS vent lines and storage tanks, oxidizers and fuels will be segregated at their source.

Gas phase chemical reactions in the transfer line could result in potential hazards. Potential reactants from specified fuels and oxidizers and possible reaction avoidance methodology is presented in Table 1.3-6.

Waste fluids which are determined to be compatible with the Integrated Waste Fluid System (IWFS) will be delivered through dedicated lines. The PMMS will provide the necessary vacuum pumps, and safing hardware as required for delivery of safe low pressure gases to the IWFS. The IWFS will be responsible for gas compression, storage and disposal. Waste gases that are incompatible with the IWFS and that cannot be vented will be stored until deorbited in the Shuttle.

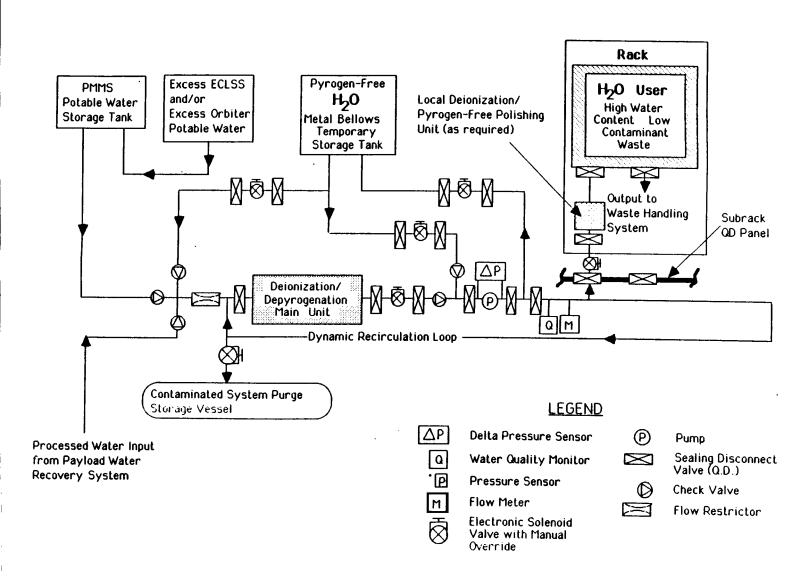


Figure 1.3-7 PMMS Water Supply and Recovery System

Table 1.3-6 Potential Gas Phase Chemical Reactions in a Common Vent Line

Potential Che Reaction Ty		Reactants	Reaction Avoidance Methodology
Combustion	Fuels H2 C0 Aliphatic Organ (e.g., Acetyler Aromatic Organi (e.g. Toluene)	ne) Peroxide)	Timeline venting for common vent line configuration. Segregation of fuels and oxidizers.
Neutralizatio	Acid Vapors HN03 HF HCL	Caustics NaOH KOH	Timeline venting of incompatible payload gases. Negligible gas quantities or normally liquid etchants. Utilize operational constraints to avoid mixing.
Halogenation	Halogens Cl ₂ F ₂	Hydrocarbons & Metals Aliphatic Organics (e.g., Acetylene) Aromatic Organics (e.g., Toluene) Cadmium Tellurium Aluminum Berylium	Timeline venting for common vent line configuration. Utilize effective particulate filtration. Segregation of halogens (oxidizer line) and organics (fuel line).

1.3-4 Vacuum Vent System

The function of the USL experiment vacuum vent system is to maintain a high quality resource for the USL user community. Experiment chamber purge and waste dump functions are the responsibility of the USL Process Material Management System (PMMS) and are not to be confused with the high quality vacuum vent system.

Figure 1.3-8 shows the vacuum vent system design concept in a cutaway view of the USL module.

The USL experiment vacuum vent will provide the user with a 10^{-3} torr standard vacuum resource. A higher quality vacuum may be obtained by augmenting the system with user provided turbomolecular pumps located in the racks where necessary.

Only small amounts of the waste fluids discussed in Section 1.3.3.2 will be vented to purge experimental chambers. The present design vent rate is approximately .004 $\rm ft^3/h$ at pressures ranging from .25 torr to nearly vacuum. As venting constraints become more severe the quantities and types of fluids being vented will need to be reevaluated.

A components list of the vacuum vent system is provided in Table 1.3-7.

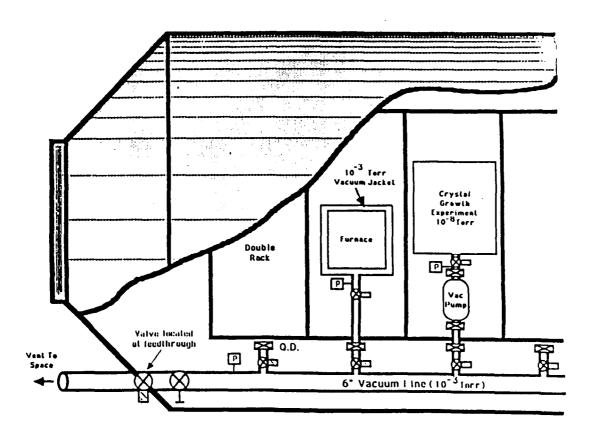


Figure 1.3-8 Experiment Vacuum Vent System Design Concept

Table 1.3-7 Vacuum Vent System Component List

PROGRAM APPLICATON	COMPONENT	RECO	SIZE (1n)	PRESSURE MEOP (paie)	USAGE	APPROK	VENDOR NAME	VENDOR PART
3 USL, WS	DI SCONNECT,	2	2	.25 (TORR)	ALL	1.45	TRO	TBD
1 USL, WS	SENSOR, PRESSURE	~	yj.	. 25 (TORR)	Y.	1.95	TBO	1380
2 USL, WS	VALVE, MANUAL SHUTOFF	52	7	. 25 (TORR)	ALL	1.42	TBD	Tab
5 UST, WS	VALVE, MANUAL SHUTOFF	~~	•	. 25 (TORR)	TT V	6.7	130	130 081
4 USL, WS	WALVE, SOLENOID	-	•	. 25 (TORR)	ALI.	15.0	TBD	180

1.4 UNITED STATES LABORATORY REFERENCES

- Peterson, T., Space Station Fluid Inventories of the Integrated Waste Fluid and Integrated Water Systems, PIR No. 191. NASA Lewis Research Center, Cleveland, OH, March 1987.
- 2) Space Station Definition and Preliminary Design, WP-01, Book 3 US Lab Module, SSP-MMC-00031, Rev. B, NAS8-36525. Martin Marietta Denver Aerospace, Denver, CO, Oct. 31, 1986.
- 3) Fluids Technical Integration Panel Data, Presented at Marshall Spaceflight Center, Huntsville, AL, October 1986.

2.0 HABITATION MODULE AND AIRLOCKS

HABITATION MODULE AND AIRLOCKS OVERALL REQUIREMENTS 2.1

The Habitation Module will be a common module outfitted for use as the Space Station (SS) crew living quarters. The airlocks will be nodes which allow for Extra-vehicular Activity (EVA) operations.

2.2 HABITATION MODULE AND AIRLOCKS FLUID SYSTEMS REQUIREMENTS

The current IOC for SS calls for use of two airlocks, one access airlock and one hyperbaric airlock. The access airlock must pump up to 90% of the usable air back into the Space Station before venting the remainder of the air to space. The pumping system that does this is considered part of the structures work package and has no fluid requirements of its own. The hyperbaric airlock has the same requirements as the access airlock and additionally must be capable of maintaining structural integrity up to six atmospheres for repressurization of personnel injured due to a damaged Extra-vehicular Excursion Unit (EEU) during EVA operations. The fluid system requirements for hyperbaric operations and the safe-haven operations are both covered in the ECLSS section. As such, the Habitation Module and Airlocks have no unique fluid system requirements which are not covered by the Integrated Systems. For detailed fluid requirements refer to the appropriate section in the system write-ups as follows:

Section 6.0 Integrated Waste Fluid System (IWFS)

Section 7.0 Integrated Water System (IWS)

Section 8.0 Integrated Nitrogen System (INS)

Section 9.0 Environmental Control and Life Support System (ECLSS)

Section 10.0 Thermal Control System (TCS)

2.3 HABITATION MODULE AND AIRLOCKS FLUID SYSTEMS DESCRIPTIONS AND CONFIGURATIONS

Fluid system descriptions and configurations for the Habitation Module, access airlock and hyperbaric airlock have been included in the following sections:

Section 6.0 Integrated Waste Fluid System

Section 7.0 Integrated Water System

Section 8.0 Integrated Nitrogen System
Section 9.0 Environmental Control and Life Support System

Section 10.0 Thermal Control System

2.4 HABITATION MODULE AND AIRLOCKS REFERENCES

- 1) Space Station Definition and Preliminary Design, WP-01, Book 2, SSP-MMC-00031, Rev. B, NAS8-36525. Martin Marietta Denver Aerospace, Denver, CO, October 31, 1986.
- 2) Space Station Definition and Preliminary Design, WP-01, Book 10 Airlocks, SSP-MMC-00031, Rev. B, NAS8-36525. Martin Marietta Denver Aerospace, Denver, CO. October 31, 1986.

3.0 LOGISTICS ELEMENTS

Logistics elements will be used for transporting the needed equipment, fluids, and raw materials to support Space Station crew and user operations. The logistics elements will also serve to transport experiment products and waste of all kinds back to earth. Two types of logistics elements have been defined as Pressurized Logistics Carriers (PLC's) and Unpressurized Logistics Carriers (ULC's) for carrying dry goods, fluids, and propellants. Both of these element types have been defined for transporting specific categories of logistics resupply items.

The PLC's will transport items for crew, station or user resupply which are to be used inside the pressurized environment. The PLC will be launched in the NSTS shuttle cargo bay and will be docked to one of the interconnecting nodes on the Space Station. This will allow "shirt sleeve" access to the PLC's payload from the other Space Station modules.

The ULC's are also launched in the shuttle, but they will transport goods and equipment to the Space Station for use outside the pressurized environment. Dry goods will be transported on dry goods pallets, which can be removed from the ULC and docked at locations outside the pressurized environment. The goods are removed from the pallet as necessary and transferred to Space Station experiments or subsystems located outside the pressurized modules.

The ULC's will also transport necessary fluids to the Space Station and other fluids users in the Space Station architecture. The fluids are transported to the Space Station on fluids pallets in much the same way as the dry goods are transported. The fluids pallets will be connected with umbilicals to the proper user subsystem or experiment. In the event that propellants must be supplied to users, additional fluids pallets will be constructed and designated as propellant pallets.

3.1 LOGISTICS ELEMENTS OVERALL REQUIREMENTS

The logistics elements will consist of several independent cargo transport vehicles designed for use with the other Space Station elements. They will provide a means for securing cargo within the NSTS Shuttle and for storing the same cargo before and after use on the Space Station structure. The Pressurized Logistics Carrier (PLC) will provide a means for resupplying internal Space Station crew and experiment supplies without the use of airlock or space suits.

The Unpressurized Logistics Carriers (ULC's) will allow transport of goods and materials that will be used outside the pressurized environment or fluids that will be transferred to internal systems through umbilical connections. The use of the UPC's with no pressure shell provides a means for cutting down the mass of structure which must be launched in the shuttle.

The overall requirements for the Logistics Elements are presented in Table 3.1-1.

Table 3.1-1 Overall Requirements for the Logistics Elements

- 1) The logistics elements must resupply consumables to the Space Station every 90 days.
- 2) The logistics elements shall remain operational for a minimum of 10 years or 40 flights.
- 3) The logistics elements shall provide a 50" by 50" hatch with 12" radius corners to accommodate transfer of equipment between modules.
- 4) The weight of logistics elements shall be kept to a minimum.
- 5) The logistics elements shall provide a pressurized volume.
- 6) The logistics elements shall provide facilities for storing supplies, spares, equipment an fluids to support Space Station and users.

3.2 LOGISTICS ELEMENTS FLUID SYSTEMS REQUIREMENTS

Fluid system requirements for the logistics elements are presented in Table 3.2-1.

Table 3.2-1 Logistics Elements Fluid System Requirements

Element	Requireme	nts
Environmental Control and Life Support System	1) Prov	ide temperature and humidity rol.
for PLC	2) Prov	ide atmospheric control and supply.
		ide atmosphere revitalization.
	4) Prov	ide fire detection and suppression.
	5) Prov cons unit	ide resupply and return of umables and orbital replacement elements for other functions in the Space Station Program.
Fluid Resupply Pallets	dist nece	ide capability to unload, ribute, and dispose of all fluids ssary for Space Station operations, support, and user support.
	 Some flui 	Japanese Experimental Module ds will be supplied by the rimental Logistics Module.

3.3 LOGISTICS ELEMENTS FLUID SYSTEMS DESCRIPTIONS AND CONFIGURATIONS

The descriptions and configurations of the Logistics Elements vary greatly with the size and number of experiments on Space Station, the size of the crew, and the venting requirements imposed on disposal systems. The fluids requirements imposed on the Logistics Elements are directly related to these configurations. The data presented in Table 3.3-1 is extracted from Fluids

Technical Interchange Panel data dated 15 August 1986. The configurations presented are no longer correct; i.e., Space Station propulsion no longer requires hydrazine. However, this is the latest tabulation of logistics requirements available. When new data becomes available it will be added to this database.

Table 3.3-1 Logistics Elements Delivery and Return Requirements

Fluid User	Fluid	Requirement (Purpose)	Maes Up (Ibm)	Mass Down (ibm)	Volume Up (cu. ft.)	Volume Down (cu. ft.)	Logistics Element	Remarks
ECLSS	02	Module repress.	444	444	24.8	24.8	TBD	Contingency only. Not every 90 days.
ECLSS	02	Hyperbaric chamber	622	622	34.8	34.8	TBD	Contingency only. Not every 90 days.
ECLSS	N2	Module repress.	1,396	1,396	27.6	27.6	TBD	Contingency only. Not every 90 days.
ECLSS	N2	Hyperbaric chamber	1,272	1,272	25.2	25.2	TBD	Contingency only. Not every 90 days.
ECLSS	N2	Leakage makeup	1,368	-	27.2	-	Fluids Pallet	
ECLSS	N2	MMU operations	1,144	-	19.6	-	Fluids Pallet	
ECLSS	N2	Airlock repress.	968	-	15.2	-	Fluids Pallet	
ECLSS	H2O	Waste	•	1,750	-	28.0	PLC.	
Station	N2H4	Propellant	5,000	-	80.0	-	Propellant Pallet	No longer a requirement but incl. in 8/86 data.
USL	H2O	Materials processing	1,400	-	22.4		Fluids Pallet	Assumes 75% recycling and CFES
USL	N2	Materials processing	1,256	-	21.2	-	Fluids Pallet	
USL	Ar	Materials processing	224	-	7.6		Fluids Pallet	
USL	02	Materials processing	80		4.4		Fluids Pallet	
USL	He	Materials processing	16	-	0.8		Fluids Paliet	
USL	Cleaning Fi.	Mat. process. cleanup	128	-	1.8		PLC	No information on fluid constituents.
Columbus	Multiple	Lab resupply	14,712	14,712	568.0	568.0	PLC	Volume estimated. These are the only quantities supplied for fluids and all other materials. There is no current breakdown of individual fluids.
JEM	H2O	Life sciences	240		4.0	-	PLC	
JEM	N2	Life sciences	44		5.0	-	PLC	
JEM	Multiple	Materials processing	TBD	TBD	TBD	ТВО	PLC,Fluids Pallet	JEM will have materials processing experiments. Most resupply will be done by ELM but there may be additional logistics elements requirements.
Customer Serv.	N2H4	Propellant resupply	14,830		237.0		Propellant Pallet	Includes Spartan, GRO, COP. These requirements may be obsolete.

^{*} Pressurized Logistics Carrier

3.3.1 Pressurized Logistics Carrier Fluid Systems

3.3.1.1 Environmental Control and Life Support System

Temperature and Humidity Control (THC)

The temperature and humidity of the atmosphere and other equipment will be controlled within the PLC. These control functions will provide ventilation throughout all areas of the PLC. The heat collected will be transferred to the Thermal Control System for dissipation. Specialized equipment (refrigerators/freezers) will also dissipate their waste heat to the Thermal Control System.

Atmosphere Control and Supply (ACS)

Atmosphere pressure and composition control functions will provide for monitoring and regulating the partial and total pressure of oxygen and nitrogen in the PLC atmosphere. Vent and relief pressure functions will also be provided along with the distribution and storage of O_2 and O_2 for the PLC, and the resupply of O_2 .

Atmosphere Revitalization (AR)

Monitoring of atmospheric constituents and control of particulates and bacteria will be provided.

Fire Detection and Suppression (FDS)

Fire detection and suppression equipment will be provided for the pressurized volume with both fixed and portable extinguishers and emergency portable breathing equipment as required.

Resupply/Return

Resupply consumables and emergency provisions for the entire Space Station Program ECLSS will be provided. Tankage for H₂O is located in the PLC. Replacement kits/ORU's for all ECLSS functions will be included such as filters, wipes, and water treatment resupply. Waste return will also be provided for waste water (brine), fecal material, trash, and carbon filters.

Additional information on the Space Station ECLSS can be found in Section 9.0 of this document.

3.3.1.2 Laboratory Process Fluids Rack

Resupply of process fluids for the U.S. Laboratory (USL) will consist of fluids racks carried internally in the Pressurized Logistics Carrier. The racks may be transported in the Unpressurized Logistics Carrier (ULC), but this require the use of an airlock to have the rack inside. The requirements for process fluids vary greatly with the number and type of experiments on board. As the requirements are further developed, the configuration of the laboratory process fluids racks will be better defined. The laboratory process fluids configuration equipment list is TBD.

3.3.2 Unpressurized Logistics Carrier Fluid Systems

3.3.2.1. Fluids Pallet - The fluids pallet will be configured to transport fluids other than propellants to the Space Station. One fluids pallet configuration will be used to transport nitrogen in to the station for resupply of the ECLSS system by means of the integrated nitrogen distribution system. The logistics of resupplying nitrogen to the space station program is discussed in Section 8.0 of this report. A second configuration may be used to resupply U.S. Laboratory (USL) process fluids when the USL fluids racks are transported in the Unpressurized Logistics Carrier (ULC).

The resupply of propellants will be accomplished with the Orbital Spacecraft Consumable Resupply System as discussed in Section 12.0 of this report.

3.4 LOGISTICS ELEMENTS REFERENCES

- 1) Fluids Technical Integrated Panel, presented at Marshall Space Flight Center, Huntsville, AL, October, 1986.
- 2) Space Station Definition and Preliminary Design, WP-01, Book 4 Logistics Module. SSP-MMC-00031 (Rev. B). Martin Marietta Denver Aerospace, October, 1986. (Contract NAS8-26525).

4.0 JAPANESE EXPERIMENTAL MODULE (JEM)

The Japanese Experimental Module (JEM) will be a Japanese built and outfitted laboratory module which will be part of the permanent Space Station. This module, funded by the National Space Development Agency of Japan (NASDA), will give the Japanese the capability to run their own experiments in microgravity environments and will permit them to conduct them in privacy by closing the hatch between modules. The JEM will house both life sciences and materials processing experiments, some of which are considered proprietary by NASDA. The privacy provided by a closed hatch will allow the Japanese to keep this information to themselves.

The Japanese Experimental Module will be supplemented by the Experiment Logistics Module (ELM), another NASDA element of the Space Station architecture. The ELM is a small replaceable module that will carry supplies needed by the JEM but not necessarily available from the core station or carried on the Logistics Module. The ELM will be transported by the NSTS Shuttle and docked to the JEM. The ELM will be considered a part of the JEM for this discussion.

4.1 JAPANESE EXPERIMENTAL MODULE OVERALL REQUIREMENTS

The JEM is a multidiscipline facility for payload accommodation both within a pressurized habitable volume and outside, exposed to space. The principal functions of the JEM include materials research and development that is sensitive to acceleration, research in life sciences relating to the behavior and adaptation to long term exposure to extremely low acceleration levels, and observation of the effects of exposure to space.

The overall requirements for the Japanese Experimental Module (JEM) are presented in Table 4.1-1.

Table 4.1-1 Overall Requirements for JEM

- 1) Accommodate the performance of selected complements of experiments both in a pressurized volume and exposed to space.
- 2) Provide cooling of TBD kW.
- 3) Provide for isolated operations during proprietary experiments.
- 4) Provide a process fluids system.
- 5) Provide a vacuum vent system.
- 6) Provide a waste management system.
- 7) Provide airlock operations to allow access to exposed facilities and external payloads.
- 8) Provide storage and transport capabilities with the Experimental Logistics Module (ELM).

4.2 JAPANESE EXPERIMENTAL MODULE FLUID SYSTEMS REQUIREMENTS

Fluid resupply and disposal requirements for the JEM are provided in Table 4.2-1 and fluid system requirements are provided in Table 4.2-2.

Table 4.2-1 JEM Fluid Resupply and Disposal Requirements

Resupply Requirement Fluid Types No, Oo, Air, Water Supplied by Space Station Core through docking port transfer lines. Supplied by JEM ELM for Thermal control. Water, Freon Supplied by JEM ELM for material processing and Ar, Dry Air, He, Kr, life science experiment gases from common gas supply unit. Supplied by JEM ELM for material processing H_2 , O_2 , C_3H_8 , and life sciences experiment from gas supply NH3, CL2, SiH4 units integrated inside the experiment equipment as mission peculiar. Supplied by JEM ELM for life sciences water to be Water supplied in cartridges. Disposed of using the JEM ELM. C3H8, NH3, CL2, SiH4, NH4C1, HCL,

Table 4.2-2 Fluid System Requirements for the JEM

Fluid	System	Fluid	System	Requirements	

Environmental
Control and Life
Support System

H₂0

- 1) Provide atmospheric pressure and composition control.
 - a) Primary control will be monitored and maintained by Space Station Core.
 - Partial pressure oxygen: 2.83 psia to 3.35 psia.
 - Total pressure: 14.7 to 0.2 psia.
 - b) Secondary control and control during closed hatch operations will be monitored and maintained by JEM with gases supplied by SS core and ECLSS.
- 2) Provide temperature and humidity maintenance.
 - a) Primary control will be maintained by Space Station Core ECLSS.
 - Nominal temperature range will be 65°F to 80°F.
 - b) Secondary control and control during closed hatch operations will be monitored and maintained by JEM.

Table 4.2-2 Fluid System Requirements for the JEM (Continued)

Environmental Control and Life Support System

- 3) Provide atmospheric revitalization.
 - a) Primary revitalization duties will be performed by Space Station core ECLSS.
 - Regenerate module atmosphere to provide a safe and habitable environment for the crew using intermodule ventilation.
 - Primary source of oxygen is electrolysis of recovered water.
 - Nitrogen supply provided by storage and resupply.
 - Removal and processing of CO₂ will be accomplished through a regenerative process.
 - b) Secondary revitalization and closed hatch revitalization.
 - Oxygen and nitrogen will be transferred from Space Station with emergency storage in bottles.
 - CO₂ will be removed in JEM and transferred to the Space Station for reduction.
- 4) Provide water and waste management.
 - Primary water supply and waste management is performed by Space Station core ECLSS.
 - Collect, process, and dispense potable and hygiene water to meet crew and experimental needs.
 - Ensure proper water quality through pretreatment and post treatment. Trace gas analyzer line provided.
 - Provide a closed-loop recovery system for drinking water.
 - b) Secondary water supply and waste functions are performed by JEM ECLSS.
 - Potable and hygiene water from Space Station ECLSS are dispensed by JEM.
 - Eyewash and handwash water and condensate is returned to Space Station waste water recovery.
- 5) Provide thermal control for module and experiments.
 - a) Coolant water is recycled within Thermal Control System.
 - b) Freon is recycled within Thermal Control System.
- 6) Provide fire detection and suppression.

Table 4.2-2 Fluid System Requirements for the JEM (Continued)

Mission Fluids System Requirements (Including Fluid Storage, Supply Disposal and Vacuum Vent System

-) Material Processing Fluids
 - a) Provide storage and distribution of JEM material processing fluids.
 - b) Provide safe handling, removal, storage, and disposal of JEM payload waste by-products.
 - c) Provide a minimum of 1 x 10⁻² torr vacuum pressure for waste gas removal from all JEM internal payloads.
 - d) Prevent overall Space Station dump rate from exceeding TBD sccf.
 - e) Prevent disturbances to microgravity research throughout the Space Station.
 - f) Comply with Space Station external contamination constraints. If vented; will be non-propulsive.
 - g) Interface with Space Station IFMS.
 - h) Capable of storing all non-FMS compatible gases for a minimum of 90 days if fluid does not meet contamination requirements.
- 2) Life Sciences Experiment Fluids
 - a) Provide all life sustaining fluids to plant and animal life in the JEM.
 - b) Provide for removal and disposal of plant and animal waste.

JAPANESE EXPERIMENTAL MODULE FLUID SYSTEMS DESCRIPTIONS AND CONFIGURATIONS

4.3.1 Housekeeping Fluids System

The JEM Housekeeping Fluids System will combine the tasks of Environmental Control and Life Support, Thermal Control, and Fire Detection and Suppression. Any fluids that are not used for experiments will be included in Housekeeping Fluids. The housekeeping fluids system will consist of the six main subsystems as described below:

- a) Temperature and Humidity Control (ECLSS)
 - 1) Cabin air temperature and humidity
 - 2) Ventilation
 - Equipment air cooling
- b) Atmosphere Control and Supply (ECLSS)
 - 1) $0_2/N_2$ pressure control (total and partial) during closed hatch operations
 - 2) Vent and Relief
 - 3) $0_2/N_2$ storage and distribution for closed hatch and emergency operations

- c) Atmosphere Revitalization (ECLSS)
 - 1) CO₂ removal
 - 2) CO₂ sent to Space Station ECLSS for reduction
 - 3) 02 supplied by electrolysis in Space Station core ECLSS
 - 4) Contaminant control
 - 5) Contaminant monitoring
- d) Water Recovery and Management (ECLSS)
 - 1) Condensate water returned to Space Station ECLSS for processing
 - 2) Hygiene water returned to Space Station ECLSS for processing
 - 3) Water distribution
 - hygiene water to hand washer
 - potable water to eye wash
- e) Fire Detection and Suppression
 - 1) Fire detection
 - 2) Fire suppression
 - 3) Crew protection
- f) Thermal Control
 - Cooling of experiments up to TBD kW, using water and freon cooling loops.
 - 2) Passive thermal control of JEM module by multilayer insulation (MLI) and thermal coatings.

Figure 4.3-1 shows a schematic diagram of the Environmental Control and Life Support Subsystem of the JEM and its interfaces with the Space Station and ELM. Figure 4.3-2 shows a schematic diagram of the Thermal Control System for the JEM. Tables 4.3-1 and 4.3-2 provide fluids requirements for the Housekeeping Fluids System.

After use by the Housekeeping System, Housekeeping Fluids will either be returned to the Space Station ECLSS for reprocessing or, in the case of battery leakage fluids, $(N_2, 0_2, H_2)$ will be vented to space. The latter occurs only under emergency conditions.

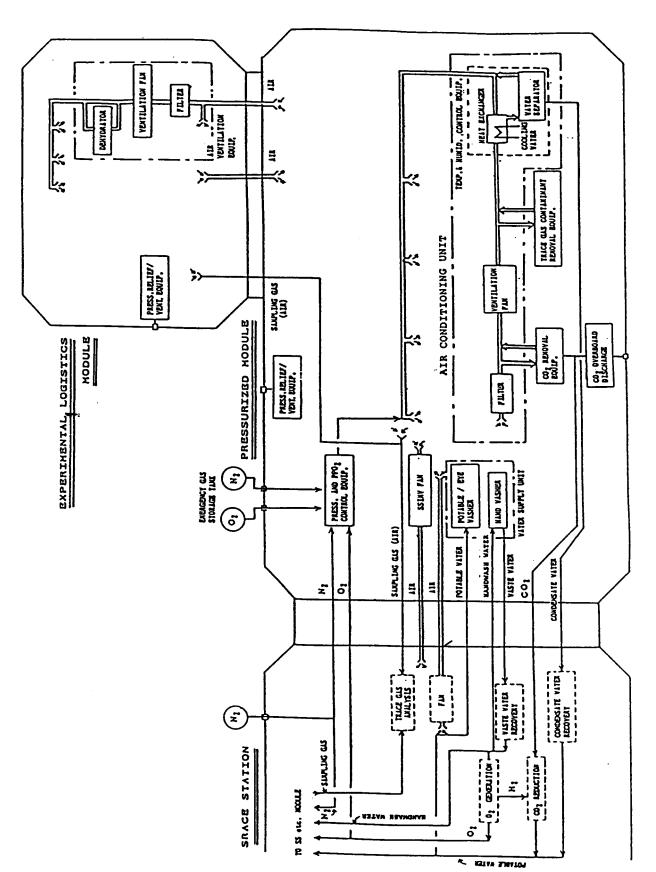


Figure 4.3-1 JEM ECLSS Schematic

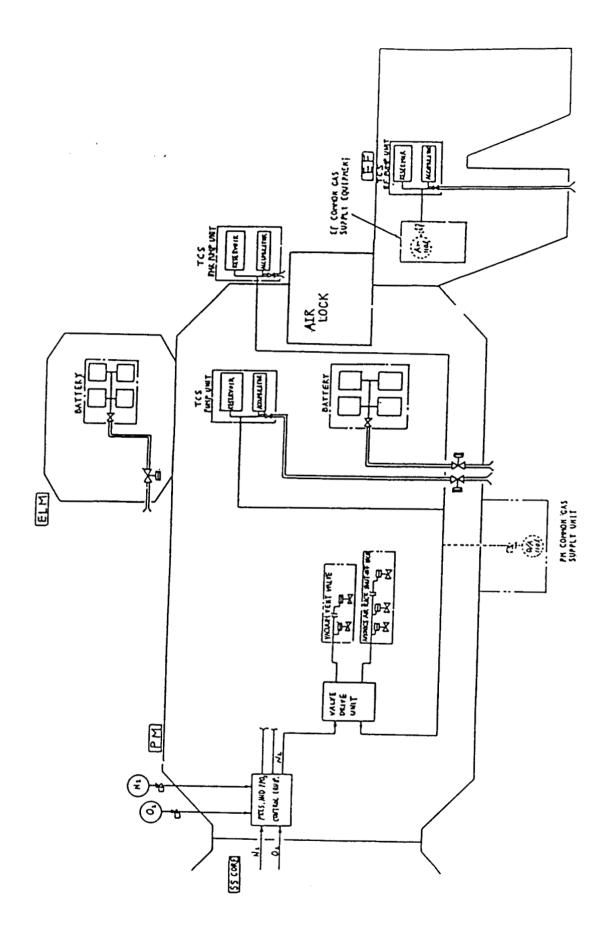


Figure 4.3-2 Thermal Control System and Emergency Battery Vent

Table 4.3-1 Fluid Inventory Requirements for the JEM Housekeeping Fluid System

8	FLUID	FIUID	FLUID	CHANTITY	USAGE	RESUPPLY QUANT	RESUPPLY QUANTITY (LB/90 DAYS)	RESUPLY	FILID	REMARKS
2	NE SYSTEM	SOBSTSTEM	TIFE	a store	1107 417	THE STATE	247			
					(LB/HK)	MEAN	Š			
, %	JEM	HOUSEKEEPING	H20	130	TBO	368	OEL .	PIPED FROM SS CORE ECLSS	POTABLE	POTABLE WATER IS USED FOR ECLSS FUNCTIONS
<u>*</u>	JEM	HOUSEKEEPING	H20		TBO	359		PIPED FROM SS ECLSS	HYGIENE WATER	HYGIENE WATER IS USED FOR ECLES FUNCTIONS.
	M3C	HOUSEKEEPING	H20		OBT NOW TBD	TBD	OEL .	JEM EIM	COOLANT ONLY	RECYCLED WITHIN TCS. RESUPPLY IS ONLY FOR CONTINGENCY REFILL OF COOLANT.
*	- JEW	HOUSEKEEPING	FREON			NOM TBD	OBT -	лем елм	OET:	FRECH IS USED FOR REFRIGERATION.
.	JEM	HOUSEKEEPING	AIR		1100-220 CU M/HR	TBO	<u> </u>	RECYCLED BY ECLSS	130	AIR IS USED FOR VENTILATION AND BREATHING.
\$	МЗС	HOUSEKEEPING	1002	087	TBO	37.2	OE .	PIPED FROM ECLAS	130	OXYGEN IS MIXED WITH NITROGEN DURING CLOSED HATCH OPS TO PROVIDE ATMOSPHERE FOR BREATHING.
₽	JEM	HOUSEKEEPING		Ogr I	081	_=	O84	PIPED FROM SS ECLESS	TBO	INZ USED FOR MIXING WITH OZ DURING CLOSED HATCH OPS TO PROVIDE BREATHABLE ATMOSPHERE
7	NZIC _	HOUSEKEEPING WASTE	H20	QE QE	TBO	450	TBO	CONDENSED FROM ATMOSPHERE	OST.	MATER IS CONDENSED FROM ATMOSPHERE. PRESENT DUE 170 RESPIRATION.
 -	JEM JEM	HOUSEKEEPING WASTE	HZO	<u> </u>	OET.	1272	087	WASTE WASH WATER	HYGIENE WATER	HYGIENE WASTE WATER IS COLLECTED AND RETURNED TO SS BCLSS
	1EM	HOUSEKEEPING WASTE	_85	OEF -	TBO		081	BYPRODUCT OF RESPIRATION	1780	COZ IS REMOVED FROM ATMOSPHERE AND RETURNED TO SELLSS THROUGH PIPING.
 &		HOUSEKEEPING WASTE	- AIR	<u> </u>	1100-220 CU M/HR	-E	OBT.	CABIN VENTILATION	081	CABIN AIR IS DUCTED BACK TO SS ECISS FOR PROCESSING.
.	, JEW	HOUSEKEEPING WASTE	 AIR	- E	OET	 115 	1180	SS ECLSS	26	AIR IS FOR RESUPPLY OF THAT LOST TO SPACE BY ILEANAGE, AIR LOCK AND DOCKING PORT USE ONLY.
+		HOUSEKEEPING WASTE	AIR/GN2	<u></u>	TBO	_ .	OBT -	ss Eclas	OST I	USED ONLY FOR MAKEUP OF TCS MAINTENANCE AND COOLANT RESUPPLY GASES LOST TO SPACE
		HOUSEKEEPING WASTE	- GN -	<u>e</u>	OBT OBT	OET OET	THO	SS ECLSS	DE	EMERGENCY VENT FROM BATTERY CELL CHAMBER
_										

ORIGINAL PAGE IS OF POOR QUALITY

Table 4.3-2 Fluid Interface Requirements for the JEM Housekeeping Fluid System

REMARKS			ALL WASTE WATER PROCESSING IS DONE BY SS CORE ECLSS.	ALL MASTE MATER PROCESSING IS DONE BY SS CORE ECLSS.	MATER IS ONLY FOR LEAKAGE MAKEUP. RESUPPLY IS ONLY FOR QUANTITY REQUIRED WHEN REQUIRED.	FRECH IS ONLY PUGED FOR DERBIT OR LEAKED OUT. RESUPPLY IS ONLY FOR CONTINGENCY.	AIR IS REVITALIZED BY SS CORE ECLSS (SCRUBBING, CO2 REDUCTION) AND RECYCLED.	OZ IS MIXED WIRH NZ ONLY FOR CLOSED HATCH OPS.	OZ IS MIXED WIRA NZ ONLY FOR CLOSED HATCH OPS.	ALL WASTE WATER PROCESSING IS DONE BY SS ECISS	HYGIENE WASTE COMES FROM WASH WATER ETC. IT IS RECYCLED BY SS ECISS.	JEM ECLISS REMOVES COZ FROM ATMOSPHERE. REDUCTION OCCURS IN SS ECLISS.	AIR IS REVITALIZED BY SS CORE ECLSS	AIR MUST BE HADE UP WIEN LOST TO SPACE	AIR/NZ USED FOR HAINTENANCE AND COOLANT MAKEUP IN TCS	EMENGENCY VENT ONLY FROM BATTERY CELL CHAMBER
TOLERANCE				<u> </u>	ORL	OE		Off	TBO	730 2	OH.	<u> </u>	QL .	9	2	081
METHOD OF WASTR	MANAGEMENT		RETURN TO ECLSS THRU PLUMBING THE	RETURN TO ECLSS THRU PLUMBING	LEAKAGE ONLY	PURGE TO TANK FOR DEORIT	RETURN TO ECLSS THRU PLUMBING THE	RETURN TO SS CORE ECLAS	RETURN TO SS CORE ECLSS	PIPED TO SS CORE ECLISS	PIPED TO SS CORE ECLSS	PIPED TO SS ECUSS	RETURN TO SS CORE ECLSS	LEAKAGE AND VENT TO SPACE	VENT TO SPACE	VENT TO SPACE
	LINE SIZES	(Turning)	88	OBT	TBD	OUT	96	55	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	5 <u>1</u> 5 <u>1</u>	99	22	55	55	55	55
CONDITIONS	TENE.		6 E	99	61 E	96	99	22	Off	65 E	O CE	55	0.67	OET.	OST	
INLET AND OUTLET FLUID CONDITIONS	PRESSURE	(Kath)	55	99	05 05 05 05 05 05 05 05 05 05 05 05 05 0	5 E	OUT OUT	55	22	91.01	55	929	55	55	O OF	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
INTEL AND O	FIGH	3	SS ECLSS CREW, USERS	SS ECLAS CREH, USERS	JEM RESUPLY (ELM)	JEM ELM RESUPPLY LEAKAGE, PURGE	SS ECLSS	SS ECLSS CABIN AIR	SS ECLSS	CREM, USERS ISS CORE ECLAS	CREM, USERS ISS ECLES	RESPIRATION SS ECLSS	CABIN VENTILATION	CABIN VENTILATION	SS ECLSS	BATTERY CELL
FLUID	1		н20	H20	Н20	FREON	AIR	200	GNZ	120	021	202	KI)		IIR/GN2	X
i GIUIJ			HOUSEKEEPING	HOUSEKEEPING	HOUSEKEEPING	HOUSEKEZPING	HOUSEKEEPING	HOUSEKEEPING	HOUSEKEEPING	HOUSEAGEPING WAST HZO	HOUSEKEEPING WAST HZO	HOUSEKEEPING WAST CO2	HOUSEKEEPING WAST AIR	HOUSEKEEPING WASTIAIR	HOUSEGREPING MASTIAIR/GN2	HOUSEKEEPING WAST GN2
GIOTA			ЭЕН	JEH	JEK	JEH	ЭЕН	JEN	JEM	NEW CEN	JEH	H215	JEM	JEM	JEM	JEM
8	i		- 56 - 15	- <u>5</u>	- <u>5</u>	- <u></u> -	-5 66 	- <u>5</u>	- <u>5</u>	2	- <u>5</u>	-5- 	- <u>5</u>	- <u>-</u>	-5- 	- <u>5</u>

4.3.2 Mission Fluids System

The JEM Mission Fluids System combines the tasks of Experiment Gas Supply, Gas and Vacuum Venting, and Experiment Water Supply and Waste Water Management. The following subsystems make up the Mission Fluids System:

a) Experiment Gas Supply

A schematic of the Experiment Gas Supply subsystem is shown in Figure 4.3-3, and its fluids requirements are shown in Tables 4.3-3 and 4.3-4. The Experiment Gas Supply subsystem will provide process fluids for the experiments which use common types of gas. There will actually be two pieces to the subsystem, one within the pressurized module for supplying those experiments operated in the shirtsleeve environment, and one that will provide fluids to the Exposed Facility Units outside the module.

The internal system will supply krypton, helium, argon, and dry air to the materials experiment racks from a payload module (PM) common gas supply unit. Carbon dioxide from the PM common gas supply unit will be supplied to the life science experiment racks as will be oxygen and nitrogen gases from the Space Station core.

The external system will supply helium and argon to the exposed facility units outside the JEM from separate exposed facility common gas supply equipment which will be enclosed in one of several interchangeable payload modules.

b) Gas and Vacuum Venting

The reference configuration of the gas and vacuum vent systems is shown in Figure 4.3-4 as designed by the NASDA. This diagram shows the waste gas and vacuum vent systems being vented to space. More recent studies have shown a concern that the constituents of waste fluids vented to the surrounding environment may exceed column density or deposition requirements. This concern creates a need for eliminating the waste fluids by a method other than on demand venting. There are several alternative ways of eliminating waste fluids including propulsively venting through resistojets on a continuous basis, storing the fluids for 14 days and then venting them to space at one time, or storing them and returning them to earth on the NSTS Shuttle. Previous studies indicate that the most effective method of disposal is to combine the waste fluids from all the Space Station elements into one integrated waste fluids system (IWFS). This system would then be used to dispose of all the fluids using the chosen method. This eliminates the problems associated with having several venting systems operated at different times by different users.

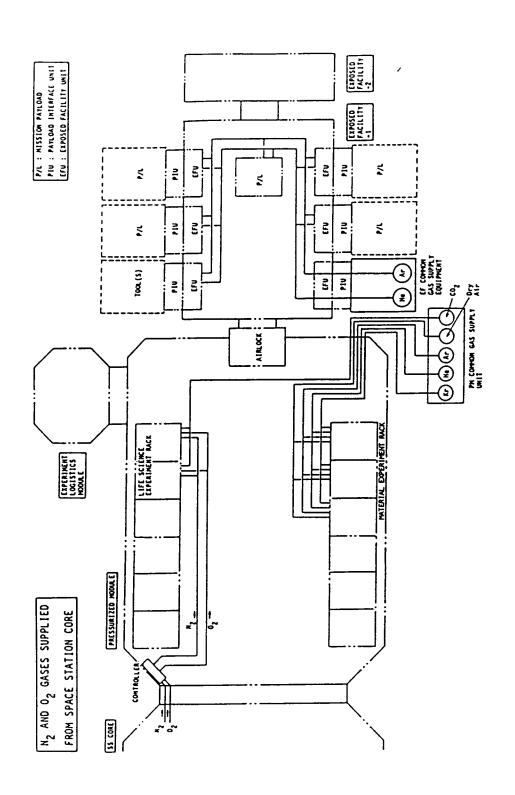


Figure 4.3-3 Experiment Gas Supply Schematic

Table 4.3-3 JEM Experiment Supply and Disposal Fluid Requirements

					50.00	THEIN CHANT	PESTIDETY CHANTITY (18/90 DAYS)	RESUPPLY	FLUID	REMARKS
5	GIITIS	FILUTO	TOTOLS	CUNNTITY	RATE	AESOFFEE COMMI	200	METHOD	COMPOSITION	
9	SYSTEM	SUBSYSTEM		a long	(LB/HR)	MEAN	X			
		SOLUTA TARMINGONO	AIR	SE.	TED	17.6	ORL	ELM	DRY AIR	USED FOR REACTIONS IN MATERIALS PROCESSING EXPERIMENTS. STABLE GAS
2	O.E.				TBO	151.8	1180		OBT.	USED FOR MATERIALS PROCESSING EXPERIMENT ATMOSPHERE PREPARATION. STABLE GAS. INERT
8	JEM	EXPERIMENT FLOADS			TBD	6.6	180	ELM COMMON GAS SUPPLY	TBD	USED FOR MATERIALS PROCESSING EXPERIMENT ATMOSHPERE PREPARATION. STABLE GAS. INERT.
3	NEW CIEN	EXPENITENT FLORES			OHI	• •	TBO	ELM COMMON GAS SUPPLY	TBD	USED FOR MATERIALS PROCESSING EXPERIMENT COOLING: INERT
25 5	JEM	EXPENDENT FLUIDS	G#2		TBD	.22	TBO	ELM TANK CHANGEOUT	OBT.	USED AS REACTANT FOR MATERIALS PROCESSING EXPERIMENTS. REDUCER. EXPLOSIVE WITH 02 AND C12.
3 :		SCIUL FLUIDS	005	130	TBO	13.3	OBT.	SS CORE ECLISS	130	USED AS REACTANT IN MATERIALS PROCESSING. OXIDIZER. FLAMMABLE. EXPLOSIVE MITH PROPANE.
র :	F	SOLUTION THE FILLINGS	PROPANE	OET	TBO	.3.3	- 11BO	EIM TANK CHANGEOUT	OBT	USED AS REACTANT IN MATERIALS PROCESSING. CORROSIVE, EXPLOSIVE WITH C12 AND SIH4.
ห ว		EXPERIMENT FIUIDS	MECHIA	3	OET	1:1	TBO	ELM TANK CHANGEOUT	130	USED AS REACTANT FOR MATERIALS PROCESSING. (TOXIC, CORROSIVE.
۶ : 		SOLUTA PROTESTA	C12	130	OBLI	<u>:</u>	780 OBL	ELM TANK CHANGEOUT	130	USE AS REACTANT IN MATERIALS PROCESSING. CORNOSIVE. TOXIC. EXPLOSIVE WITH PROPANE.
a 8	JEM	EXPERIMENT FIUIDS	SIH4 (SIIANE)	- I		- - 3 -	OBL -	ELM TANK CHANGEOUT	1380	USED AS REACTANT FOR MITERIALS PROCESING, TOXIC IAND CORNOSIVE, ISOLATE FROM H20.
						5.13.5	Off	ISS CORE	TBD	N2 IS MIXED WITH O2 FOR RESPIRATION. STABLE.
) SEM	LIFE SCIENCE FLUIDS GN2	S C 2	<u> </u>			<u>[</u>	286		USED FOR RESPIRATION. FLAMMABLE.
	- JEM	LIFE SCIENCE FLUIDS GO2	si 002	TBD	TBO	151.7	<u> </u>			UGED FOR RESPIRATION, CORNOSIVE.
	JEN JEN	LIFE SCIENCE FLUIDS CO2	s co2	OET	ORTI	=_	OB.	FLIM COMPON GAS SUPPLY		and the second
	B	LIFE SCIENCE FLUIDS H20	S1H20	-130 -130	1730	183.6	0 <u>1</u>	JEM ELM SELE PROVISION	TBD	POTABLE NATER MAY BE BROWNT OVER FROM OUR
:	,	STILL STILLING	INHACI	ZINON	SPALL	NONE	NONE	N/N	TBO	BY PRODUCT OF REACTION.
ا 		SULITIES POLYGODISH	<u></u>	NONE	SMIL	NONE	NONE	N/A	1380	BY PRODUCT FROM EXPERIMENT
3		SOLUTION OF THE PROPERTY OF TH	<u> _</u> 8	NOME	SMIL	NONE	NONE	N/A		EXPERIMENT BY PRODUCT
 2 2	3 JEM 	SUBPRODUCE FLUIDS		NONE	SPOLL	- INONE	NONE	N/A	1 TBD	EXPERIMENT BYPRODUCT
			_							

Table 4.3-4 JEM Experiment Supply and Disposal Fluids Interface Requirements

REMARKS		(VENT TO SPACE MAY NOT BE ALLOWED, WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOHED, WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLONED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED MASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLONED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED MASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED, WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOMED. MASTE WOULD BE COLLECTED AND SENT TO INTEGRATED MASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOMED, WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED MASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED, WASTE MOULD BE COLLECTED AND SENT TO INTEGRATED MASTE SYSTEM.	MUST BE CAPTURED AND RETURNED TO EARTH ON SHUTTLE.	VENT TO SPACE MAY NOT BE ALLOMED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED. WASTE WOULD BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.	VENT TO SPACE MAY NOT BE ALLOWED, MASTE MOUID BE COLLECTED AND SENT TO INTEGRATED WASTE SYSTEM.
FALLURE		130	TBO	TBO	TBD	TBD	OST	TBO	TBO	TBO	TBO	TBD	6	TBO	TBD	TBD	Ö	TBO	TBO
METHOD OF WASTE	MANAGEMENT	VENT TO SPACE	VENT TO SPACE	VENT TO SPACE	VENT TO SPACE	VENT TO SPACE	VENT TO SPACE	VENT TO SPACE AFTER TREATING	VENT TO SPACE AFTER TREATING	VENT TO SPACE AFTER PROCSSING	VENT TO SPACE AFTER TREATING	VENT TO SPACE	VENT TO SPACE	VENT TO SPACE	VENT TO SPACE	CAPTURE	VENT TO SPACE AFTER TREATING	VENT TO SPACE AFTER TREATING	VENT TO SPACE AFTER TREATING
s	LINE SIZES (INCHES)	OET OET	OUT	98	081	92	567	22	OET	087	081	85	087	<u> </u>	0.01	50	OBT	OBT	TBO
INLET AND OUTLET FLUID CONDITIONS	TEMP.	08T	<u> </u>	<u> </u>	<u>66</u>			22	22	92 EE	0.67	5E 5	55	<u> </u>	0. Et -	OET OET	6 6 6 6	<u> </u>	0.61
VILET FLUI	PRESSURE (PSIA)	19 TBD	19 780	719 7180	13 to 10 to	et of E	130 130	<19 780	120 130 130	419 TBO	<19 TBO	14.7 TBD	14.7 TBO	14.7 TBD	14.7-30 TBD	1BO TBO	787 087	08T 08T	TBO
I INLET AND O	FROM TO	EXPERIMENTS	EXPERIMENT ATMOSPHER TRO	ELM COMMON GAS SUPP.	ELM COMMON GAS SUPP.	EXPERIMENT	SS CORE	ELM INDIVIDUAL TANK EXPERIMENT	ELM INDIVIDUAL TANK EXPERIMENT	EXPERIMENT	ELM INDIVIDUAL TANK EXPERIMENT	SS CORE	SS CORE	ELM COMMON SUPPLY LIFE EXPERIMENT	ELM TANK CHANGEOUT	EXPERIMENT DI SPOSAL	EXPERIMENT DI SPOSAL	EXPERIMENT DI SPOSAL	EXPERIMENT
FLUID		AIR	¥	Ä	GH6	GH2	200	PROPANE	APPONIA	C12	SIH4 (SILANE)	GN 2	2005	200	H20	NB4C1	Ę	200	нго
FLUID		EXPERIMENT FLUIDS AIR	EXPERIMENT FLUIDS AF	EXPERIMENT FLUIDS KE	EXPERIMENT FLUIDS GRA	EXPERIMENT FLUIDS GH2	EXPERIMENT FLUIDS GO2	EXPERIMENT FILIDS PROPANE	EXPERIMENT FLUIDS AMEONIA	EXPERIMENT FLUIDS C12	EXPERIMENT FLUIDS SIH4 (SILANE)	LIFE SCIENCE FLUI GN2	LIFE SCIENCE FLUI GOZ	LIFE SCIENCE FLUI CO2	LIFE SCIENCE FLUI H20	SUBPRODUCT FLUIDS NH4C1	SUBPRODUCT FLUIDS HC1	SUBPRODUCT FLUIDS 002	SUBPRODUCT FILLIDS H20
FLUID		JEM	Mag/	ЛЕМ	Mac Mac	JEN	JEM	HZIC	NZV.	Mac	Han	JEH	изи	лем	JEW JEW	ЛЕН	ж	ЭЕМ	JEM
음 일 일		• • • • • • • • • • • • • • • • • • •	 8	- <u>-</u>	- 	 8	 3	 82 	- <u>-</u>	- <u>5</u>	3	8	· · · · · · · · · · · · · · · · · · ·	<u>-5</u>	-5 3	-3	- 5	- 	2

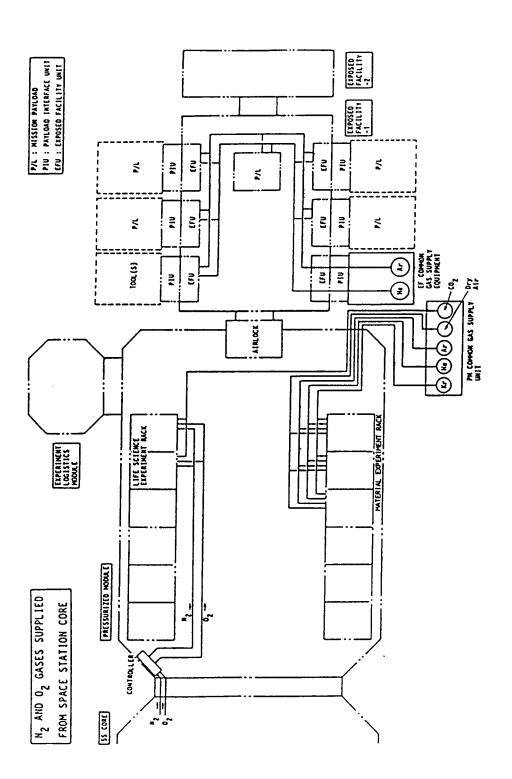


Figure 4.3-4 Vacuum and Gas Vent

The Space Station baseline IWFS will accept only specific gases for disposal. These gases are shown in Table 4.3-5 along with the quantities of each expected to be discarded by the JEM. The fluids that cannot be disposed of by IWFS will be stored in portable pressure vessels (PPVs) and returned to earth on the NSTS Shuttle. A compilation of all the fluids to be disposed of by the JEM is shown in Table 4.3-4.

The vacuum vent system will be is used for venting experiments at pressures from .25 torr on down. It will remove such a small quantity of fluids from the experiments that they will be vented directly to space. This provides a ready source of vacuum down to 1×10^{-3} torr. Higher quality vacuum will be obtained by augmenting the system with user provided pumps located in the racks where necessary.

c) Experiment Water Supply and Waste Water Management

The experiment Water Supply and Waste Water Management Experiment are shown in Figure 4.3-5. Experiment water will be supplied only to life sciences experiments in the JEM. The materials experiments will be required no water supply. The water requirement for the life sciences experiments is included in Table 4.3-2. An optional water supply line is shown in Figure 4.3-4. This would eliminate some or all of the need for experimental water supply from the ELM by using excess water from Space Station ECLSS and other sources in the core Space Station. This remains as merely an option. Disposal of experiment water after use in the life sciences experiments will be to contaminant waste cartridges. These PPVs will be returned to earth in the ELM on the space shuttle. There are no plans to process this waste or to integrate it with other Space Station systems.

Table 4.3-5 JEM Waste Fluids (1bm/year)

Fluid	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004
Argon	608	608	608	608	608	608	608	608	608	608
CO2	0	0	0	0	0	0	0	0	0	0
CO2/CH4	0	0	0	0	0	0	0	0	0	0
Freon	0	0	0	0	0	0	0	0	0	0
Helium	18	18	18	18	18	18	18	18	18	18
Hydrogen	1	1	1	1	1	1	1	1	1	1
Nitrogen	54	54	54	54	54	54	54	54	54	54
Oxygen	30	30	30	30	30	30	30	30	30	30
Xenon	0	0	0	0	0	0	0	0	0	0
Krypton	40	40	40	40	40	40	40	40	40	40
Totals:	751	751	751	751	751	751	751	751	751	751

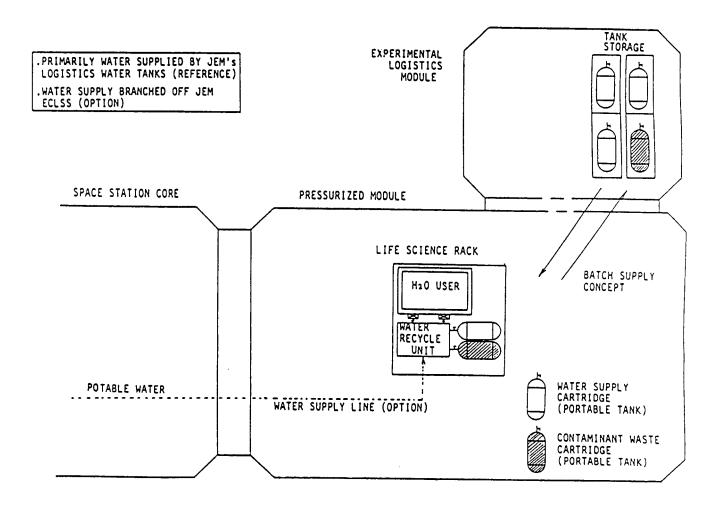


Figure 4.3-5 Experiment Water Supply and Waste Water Management

4.4 JAPANESE EXPERIMENTAL MODULE REFERENCES

- 1) Fluids Technical Integration Panel, presented at Marshall Space Flight Center, Huntsville, AL, October, 1986.
- 2) Peterson, T., Space Station Fluid Inventories of the Integrated Waste Fluid and Integrated Water Systems, PIR No. 191. NASA Lewis Research Center, Cleveland, OH, March, 1987.

5.0 COLUMBUS MODULE

The Columbus module will be a laboratory module outfitted for both materials processing and life sciences experiments. The Columbus module will be built and funded by the European Space Agency (ESA) providing the Europeans the opportunity to perform their own experiments without building their own space station.

At present, almost no information is available about the requirements, descriptions, and configurations of the Columbus module. However, Mr. Hans D. Schmitz, in the European Space Agency, has offered his assistance in providing data associated with the Columbus Module. As data becomes available, it will be added to the database and used to update the commonality study.

5.1 COLUMBUS MODULE OVERALL REQUIREMENTS

The fixed, overall requirements for Columbus are unavailable.

Requirements that can be derived for Columbus are presented in Table 5.1-1.

Table 5.1-1 Columbus Derived Requirements

- Provide an environment which allows crew members to perform a selected group of experiments within a "shirt sleeve" environment.
- Provide a process fluids system.
- Provide a waste management system.
- Provide a vacuum vent system.

5.2 COLUMBUS MODULE FLUID SYSTEMS REQUIREMENTS

Columbus Fluids Subsystem requirements are TBD.

5.3 COLUMBUS MODULE FLUID SYSTEMS DESCRIPTIONS AND CONFIGURATIONS

5.3.1 Environmental Control and Life Support (ECLSS)

The Columbus Module ECLSS configuration is TBD.

5.3.2. Process Fluids Supply System

The Columbus Module Process Fluids Supply System configuration is TBD. The quantities of fluids to be resupplied are also unavailable, but can be derived for some fluids based on waste quantities established for the Japanese Experimental Module and the United States Laboratory. These quantities are shown in Table 5.3-1.

5.3.3. Waste Fluids System

The Columbus Module Waste Fluids System configuration is TBD. The quantities of fluids available for disposal to the Space Station Integrated Waste Fluids System are shown in Table 5.3-1.

Table 5.3-1 Columbus Module Waste Fluids (1bm/year)

Fluid	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004
Argon	167	167	167	167	167	167	167	167	167	167
CO2 **	104	104	104	104	104	104	104	104	104	104
CO2/CH4	0	0	0	0	0	0	0	0	0	0
Freon	3	3	3	3	3	3	3	3	3	3
Helium	9	9	9	9	9	9	9	9	9	9
Hydrogen	1	1	1	1	1	1	1	1	1	1
Nitrogen	54	54	54	54	54	54	54	54	54	54
0xygen	30	30	30	30	30	30	30	30	30	30
Xenon	44	44	44	44	44	44	44	44	44	44
Krypton	40	40	40	40	40	40	40	40	40	40
Totals	452	452	452	452	452	452	452	452	452	452

^{*} Waste gas amounts not specified by ESA; assumed quantities are the smaller amounts of USL and JEM quantities

5.4 COLUMBUS MODULE REFERENCES

Peterson, T., Space Station Fluid Inventories of the Integrated Waste Fluids and Integrated Water Systems, PIR No. 191. NASA Lewis Research Center, Cleveland, OH, March, 1987.

^{**} CO2 amounts assumed the same as USL; ESA has specified Columbus as having biological experiment activities

6.0 INTEGRATED WASTE FLUID SYSTEM (IWFS)

6.1 INTEGRATED WASTE FLUID SYSTEM OVERALL REQUIREMENTS

The overall requirements for the IWFS are presented in Table 6.1-1.

Table 6.1-1 Overall Requirements for the Integrated Waste Fluid System

- 1) Collect waste fluids discarded by the station elements that are compatible with safe collection and storage.
- 2) Transfer, condition and allocate the collected fluids for disposal or return systems.
- 3) Control and monitor collection, transfer, storage, conditioning, allocation and disposal of waste fluids.
- 4) Will not preclude the ability of individual station elements to provide a vacuum resource to the user interface.
- 5) Waste fluids that cannot be accepted by the IWFS must be disposed of by the Space Station Program Element (SSPE) or system associated with or operating from a SSPE, provided that the requirements of waste handling and venting are met.

6.2 INTEGRATED WASTE FLUID SYSTEM REQUIREMENTS

Integrated fluid system requirements are presented in Table 6.2-1.

Table 6.2-1 Integrated Fluid System Requirements

Parameter	Requi	irements
Growth	1)	IOC systems shall have growth and on-orbit reconfiguration capability to accommodate changing demands in user fluid quantities. System shall incorporate scarring to accommodate additional integrated system at logical full operational capability.
Integrated Design	1)	System shall be integrated to minimize fluid management hardware development and operational cost.
Interface Hardware	1)	Fluid interface components shall be standarized, and fluid transfer interface hardware shall be designed to preclude mating to the wrong connector.
Fluid Storage Requirements	1)	A fluid quantity measurement capability shall be provided in both the storage and resupply systems. Leakage detection, isolation, and control
		shall be provided and shall comply with station environmental and contamination requirements.

Table 6.2-1 Integrated Fluid System Requirements (Continued)

Acce	eleration
and	Orientation
Cons	straints

The resupply/transfer of fluids shall be independent of the gravitational environment and/or specific orientation of any interfacing element.

Waste Fluid Handling

- 1) No overboard dumping of solids or liquids.
- 2) No particles released from vents shall exceed TBD micron in diameter.
- 3) The integrated overboard venting of gases, at any time, shall comply with the external contamination requirements.
- 4) Accumulative venting or dumping from all SSPE's shall be inventoried to support the integrated contamination control analysis.
- 5) A system will be provided to manage potential venting and dumping from all SSPE's and systems associated with or operating from an SSPE.
- 6) Design will comply with contamination and micro-gravity requirements. Controllable to permit scheduling of the dumps with minimum impacts to observer and microgravity activity scheduling. Minimize the frequency and duration of nonoperational dumps.

6.3 INTEGRATED WASTE FLUID SYSTEM DESCRIPTION AND CONFIGURATION

Possible waste fluid sources on the IOC Space Station include the four core Modules (United States Laboratory (USL), Habitation, Japanese Experiment (JEM), and Columbus), the integrated nitrogen and water systems, attached payloads, environmental control and life support system (ECLSS), airlocks and in future, the fluids servicing facility. Fluid interfaces between these systems and the IWFS are presented in Figure 6.3-1. At this time, only the ECLSS, USL, attached payloads and JEM have identified quantifiable waste gas data. Columbus Module waste gas quantities may be derived from waste quantities generated for the JEM and the USL. Waste fluid quantities generated from the remaining sources are either minimal or cannot be estimated at this time. Therefore, the fluid inventory data includes only the five Space Station elements previously mentioned.

Collection of Waste Fluids

Multiple deployable waste gas collection lines were recommended to capture and route all waste gases from Station elements to a central storage facility. Fluid waste system segregation was not recommended because of the wide variety of single and mixed type waste quantities expelled from the experiment labs, the relatively small amount of fluids, the presence of unwanted mixtures such as CO2 and methane produced in the Sabatier ECLSS and the time availability of attached payload waste gases.

Therefore, separate lines will be used to transfer reducing gases (hydrogen and methane) and oxidizing gases (oxygen) from each gas source to separate storage tanks in the central waste gas storage facility. Inert gases will be collected in either line depending on storage availability and the need to dilute either oxidizers or reducers at the central storage facility.

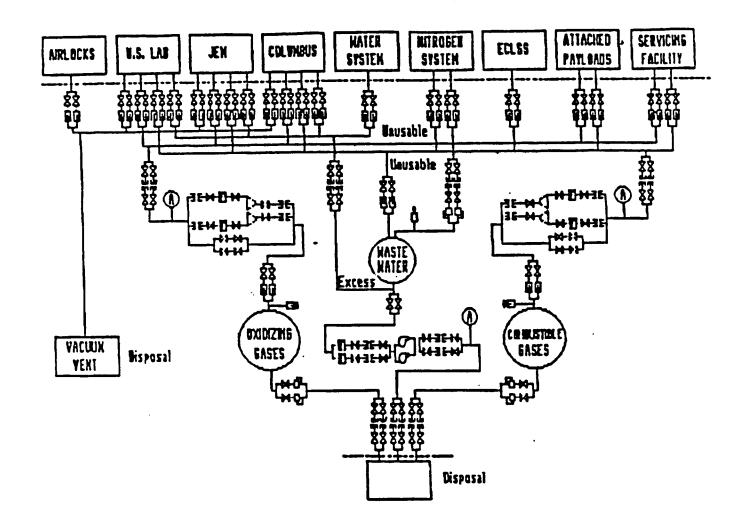


Figure 6.3-1 Integrated Waste Fluid System

Waste fluid collection will operate from 10 to 15 psia. Two low pressure compressors will be activated when the collection system reaches 15 psia which transfers fluids into a 35 psia accumulator. Fluid system requirements for the IWFS collection system are presented in Tables 6.3-1 and 6.3-2. The waste gases presented in Tables 6.3-1 and 6.3-2 represent only those gases suitable for IWFS storage and resistojet propulsion system use. Solvents, acids, oils and brine-type fluid mixtures will not be allowed to enter the IWFS.

Table 6.3-1 Integrated Waste Fluid System Fluid Inventory Requirements

QI QI	FIUID	TIMID	DIMIA	OUNTITY	USAGE	RESUPPLY QUANTITY (LB/90 DAYS)	TY (1.B/90 DAYS)	RESUPPLY	FLUID	REMARKS
<u>ģ</u>	SYSTEM	SUBSYSTEM	TYPE	a di di	(LB/HR)	MEAN	MAX			
53	IWFS	ATT. PAYLOADS	1	80.5	TBD	TBO	TBD	FLUID TRANSFER FROM AIT. P/L	081	Presently no requirement to integrate attached Paylonds fluids with space station.
8	IWFS	ATT. PAYLOADS		6.09	TBD	3	TBO	FLUID TRANSFER FROM AIT. P/L	DET	PRESENTLY NO REQUIREMENT TO INTEGRATE ATTACHED PAYLOADS FLUIDS WITH SPACE STATION.
8	IWES	ATT. PAYLOADS	GHO	180.4	1380	<u>8</u>	TBD	FLUID TRANSFER FROM ATT. P/L	130	PRESENTLY NO REQUIREMENT TO INTEGRATE ATTACHED PAYLOADS FLUIDS WITH SPACE STATION.
86	IMES	ATT. PAYLOADS	10012	54.3	730	er –	TBO	FLUID TRANSFER FROM AIT. P/L.	200	PRESENTLY NO REQUIREMENT TO INTEGRATE ATTACHED PAYLOADS FLUIDS WITH SPACE STATION.
116	IWFS	ATT. PAYLOADS	GN2	79.6	TBD	TBO	TBO	FLUID TRANSFER FROM ATT. P/L	TBO	PRESENTLY NO REQUIREMENT TO INTEGRATE ATTACHED PAYLOADS FLUIDS WITH SPACE STATION.
=======================================	IMES	00I	Ŋ.	TBD	1180	41.75	41.75	FIUID TRANSFER FROM COLUMBUS	1380	
115	IWFS	10	82	130 	_TBO		26	FLUID TRANSFER FROM COLUMBUS	130 0	
116	IMES		FREON	OE.		10.75	0.75	FIUID TRANSFER FROM COLUMBUS	130	
111	INFS	. <u>1</u> 80	- <u>e</u>	OE .	TBO	2.25	2.25	FILID TRANSFER FROM COLUMBUS	- T-	
119	INFS	1 <u>8</u>	TOTAL INERTS	OET	OHT -	105.25	105.25	FILID TRANSFER FROM COLUMBUS		
120	IMES	<u>18</u>	100	130	TBO	5.	7.5	FILID TRANSFER FROM COLUMBUS	OEE -	
121	TIMES] 		OB.	.051 NOP	NOM . 25	 57.	FILID TRANSFER FROM COLUMBUS	TBD	
122	IMES	ECLSS, BOSCH	GH2	OBT	. 018 NOM	35	0,1	FLUID TRANSFER FROM ECLSS	1780	
123	IMFS	ECLSS, SABATIER	002/CH4	96	.443 NO	NOM 935	1870	FIUID FRANSFER FROM ECLSS	1780	
125	IMES	LINS	GN2	130	081	27	27	FIUID TRANSFER FROM IWS	138D	
105	IWFS	JEM	Ār	1380	Off	152	152	FLUID TRANSFER FROM JEM	TBD	
106	IMES	JEN	CER®	. T. T. D. C. T.	OET		s: -¥-	FIUID TRANSFER FROM JEM	081	
101	INFS) EM	FREON	1780 1	TBO	10.75	10.75	 FIUID TRANSFER FROM JEM	OET	
	IWES	NSI -	- GN2		TBO	 13.5 	 13.5 	FIUID TRANSFER FROM JEM	TBO	
100	INFS	C	<u> </u>	08.	TBO	_=_	_11_	 FLUID TRANSFER FROM JEM 	0ET	
110	IMFS) JEN	코	18 0	TBD	-110	110	FIUID TRANSFER FROM JEM	130	
=======================================	IMES	JEM	TOTAL INERTS	TBD	1.082 NO	NOM 1194	134	FIUID TRANSFER FROM JEM	TBD	
112	IWFS	JEN JEN	200	TBD	1.003 NO	NOM 7.5	7.5	FIUID TRANSFER FROM JEM	TBD	
-			٠			-	:			

Table 6.3-1 (Continued) Integrated Waste Fluid System Fluid Inventory Requirements

											-
REMARKS											
OINTA I		OST.	1	1780	OSET						_
RESUPPLY METHOD		FILID TRANSFER FROM JEM	FLUID TRANSFER FROM USL	FILUID TRANSFER FROM USL	FIUID TRANSFER FROM USL	FIUID TRANSFER FROM USL	FLUID TRANSFER FROM USL	FIUID TRANSFER FROM USL	FIUID TRANSFER FROM USL	FLUID TRANSFER FROM USL	
(TY (LB/90 DAYS)	XM	0.25	83.5	25_	1.5	657.5	_ 52	1821	91.5	11.5	_
RESUPPLY QUANTITY (LB/90 DAYS)	MEAN	NOM 0.25	41.75	36	51.	320.75	11	NOM1410.5	NOM 45.75	.75	
USAGE	(LB/HR)	NOM NOM	Off	Offi	-E	OET		HOM 275.	.042 NOH	NOM .75	_
STORED		OE.	08T	730 	TBO 08T	- E -	- II-	-i-	- <u>:</u> -		_
FTUID		CH2	Ŋ.	83	FREON	GN2		TOTAL INERTS	305	GH2	_
FLUID		, Ag	TSO	180	Tsn	150	TSN	150	150	150	-
FIUID	i	I IVES	Times	INFS	IMFS IU	INTES 104	IMES IUK	TMES	IMES CO	- SAMI	-
a 9	 i	811	*	 -	 8	100 100	<u></u> _	102	103	- <u></u> -	-
_	-										

Table 6.3-2 Integrated Waste Fluid System Fluid Interface Requirements

REMARKS																	
FAILURE		SINGLE	SINGLE	SINGLE	SINGLE	SINGLE	SINGLE	SINGLE	SINCLE	SINGLE	SINGLE	STAGLE	SINGLE	SINGLE	SINGLE	SINGLE	
METHOD OF	HAVAGEHENT	RESISTOJETS	RESISTOJETS	RESISTOJETS	RESISTOJETS	RESISTOJETS	resistojets	RESISTOJETS	RESISTOJETS	RESISTOJETS	RESISTOJETS	RESISTOJETS	RESISTOJETS	RESISTOJETS	RESISTOJETS	resistojets	
	LINE SIZES	.375 18 .5/.25	5 5	.25	.5/.25	375 -	.25	.375		.375	.375	.375	: :::	.375	.375	52.	
CONDITIONS	TEMP. 1	88	26	22	22	22	88	22	88	56 	22	22	2 g	55	88	22	
INIET AND OUTLET FLUID CONDITIONS	PRESSURE (PSIA)	300	150	300	15	300	300	88	300		15 300	300	115	15 300	15.0	115	
INIET AND	FROM	ATT PAYLOADS INFS STORAGE	ATT PAYLOADS INFS STORAGE	ATT PAYLOADS IMFS STORAGE	COL INFS STORAGE	COL IMÉS STORAGE	COL INFS STORACE	ECLSS, BOSCH IMPS STORAGE	ECLSS, BOSCH INFS STORAGE	eciss, sabatier Infs Storace	JEM INFS STORAGE	 JEM INFS STORACE	JEM INFS STORAGE	USL IMFS STORAGE	 USI. IWFS STORAGE	 USL IMFS STORAGE	
FLUID	 	INERTS	OKIDIZERS	REDUCERS	INERTS	OXIDIZERS	REDUCERS	INERTS	REDUCERS	REDUCERS	INERTS	OXIDIZERS	REDUCERS	INERTS	OXIDIZERS	REDUCERS	
FLUID	SUBSTSTEM	AFT PAYLOADS I	ATT PAYLOADS 10	ATT PAYLOADS R	18	- S - - 18 _	700	ECISS	ECLSS	ECISS II	JEM	JEM -	JEM	TSO	Inst	Instruction	
FLUID	SYSTEM	IMPS	- Ci	TWES	INFS	INFS	IMES		IMES		IWES	IMES	IMES	IMES	INFS	IMPS	
<u>a</u>	<u></u>	135	136 I	137 11	132	-51	- <u>-</u>	138 IWES	139	140 INFS	129	- ge	E1	126	127	128	

Storage

The IWFS storage subsystem will provide separate tanks for oxidizing/inert gas mixtures, reducing/inert gas mixtures and excess water. Previous studies have assumed that the storage subsystem will be mounted near the core module area on the transverse boom structure. To meet long duration hold times imposed by external environment criteria, the storage facility must accommodate a 15 day hold time allowing propulsive venting to be delayed until quiescent station operation.

Dual string compressors are used to raise the gases stored in the accumulators at 35 psia to a 300 psia storage tank pressure. The storage pressure of 300 psia was chosen based on the compressor technology developed for the Manned Orbiting Research Laboratory (MORL). A component list, including both collection and storage subsystems of the IWFS is presented in Table 6.3-3.

6.4 INTEGRATED WASTE FLUID SYSTEM REFERENCES

- Peterson, T., Space Station Fluid Inventories of the Integrated

 Waste Fluid and Integrated Water Systems, PIR No. 159. NASA Lewis
 Research Center, Cleveland, OH, March 25, 1987.
- 2) Fluids Technical Integration Panel Data. Presented at Marshall Space Flight Center, Huntsville, AL, October 1986.
- 3) Data provided by John Griffin at Johnson Space Center, April 1987.

Table 6.3-3 Integrated Waste Fluid System Component List

-									
- INSERT	PROGRAM APPLICATON	COMPONENT	RECO	SIZE (1n)	PRESSURE MEOP (psia)	USAGE WEDIA	APPROX HASS (1b)	VENDOR NAME	VENDOR PART NUMBER
161 - 161 - 161	IWES,	NEGULATOR,	9	CELL	OBT.	GW2	2.2	TBD	OBT
192	IWFS,	SENSOR, PRESSURE	5	OHL	300	RE/OX/INERIS	9.0	TBO	Tago
193	INFS,	SENSOR, PRESSURE	7	OHT	30	H20		TRD	130 130
<u>₹</u>	IMPS,	FILTER, INLINE	•	κį	300	ALL	0.5	TBO	OET
198	IMPS,	DISCONNECT,	91	.375	15	OXIDIZERS	0.5	TBD	OBT -
201	INFS,	PRESSURE VESSEL,	~	۸i	300	OXIDIZERS	101.8	DET	OET -
202	INFS,	PRESSURE VESSEL,	•	.25	300	REDUCERS	101.6	136D	138D
203	IMFS,	PRESSURE VESEL,	,-	.25	30	HZ0	42.0	130	OBT.
204	IWFS,	PRESSURE VESSEL, ACCUMULATORS	~	.25/.5	35	REDUCERS		130	OBT -
205	INFS,	PRESSURE VESSEL, ACCUMULATORS	-	.25	OET	H20	3.2	130	OET
506	IMFS,	HISC, COMPRESSOR	7	s:	300	OXIDIZERS	30.0	138 D	OEL -
207	INFS,	MISC, COMPRESSOR	8	25.	300	REDUCERS	30.0	130	rac Ogu
508	IWFS,	MISC, PUMP	~	OBT	TBD	H20	35.0	TRD	OBT
8 -	IMFS,	REGULATOR,	8	TBO	300	OXIDIZERS	5.0	TBD	rao
- 2	INFS,	PRESSURE VESSEL, ACCUMILATORS	8	.25/.5	35	OXIDIZERS	6 .3	130	061
	IWFS,	VALVE, RIECTRIC	¥.	375.	15	OXIDIZERS	1.5	TBO	TBO
176	INFS,	VALVE, RIECTRIC	ş	ĸ.	15.0	REDUCERS	1.5	TB D	067
13.	IMFS,	VALVE, RIECTRIC	~	.25	180	REDUCERS	1.5	13 D	08T
178	IMFS,	VALVE, ELECTRIC	•	.25	30	GN2	2.2	TRD	OBT
	IMFS,	VALVE, ELECTRIC	8	25.	008	GH2	1.5	TBD	TBD
	IMFS,	VALVE, ELECTRIC	2	%	30	H20	3.0	1780	1380
181	IWFS,	VALVE, ELECTRIC	6	'n	15	ALL	1.5	13 D	TBO
182	IMFS,	VALVE, RELIEF	~	æ.	300	OXIDIZERS	5.0	TBD	TBO
183	IMFS,	VALVE, RELIEF		52:	300	REDUCERS	5.0	130	ORL .
185	IMFS,	VALVE, RELIEF	-	.25	30	H20	3.5	TBD	TBD
186	IWFS,	VALVE, CHECK	12	ν.	300	OXIDIZERS	1.0	TRD	1360 1
187	IMES,	VALVE, CHECK	7	.25	300	REDUCERS	1:0	1780	Off
188	IWFS,	VALVE, CHECK		52.	30	H20	1.5	TBD	T30
189	IMFS,	REGULATOR,	~	Our	300	REDUCERS	5.0	TBO	CELL
138	IWFS, ATT PAYLOADS	DI SCONNECT,	~	.25	80.0	REDUCERS	1.0	TBD	TBO
197	IMFS, ECLSS	DI SCONNECT,	8	.25	180	REDUCERS	0.7	T8D	730 1730
2001	IWES, INS	DI SCONNECT,	-	.25	750	3 85	1.0	TBD	TBD
199	IWES, IWS	DI SCONNECT,	16	.25	30	H20	6.0	TBD .	TBD
1961	196 IWFS, LABS	DI SCONNECT,	12	. 25	15	REDUCERS	9.9	TBD	TBO

7.0 INTEGRATED WATER SYSTEM (IWS)

7.1 INTEGRATED WATER SYSTEM OVERALL REQUIREMENTS

The integrated water system will be responsible for providing water to the U.S. Laboratory, Japanese Experimental Module, Columbus Module and propulsion system. The system will be capable of accepting excess potable water from the Environmental Control and Life Support System (ECLSS) and the Orbiter and will also be capable of transferring excess water to the IWFS.

7.2 INTEGRATED WATER SYSTEM REQUIREMENTS

Integrated water system requirements are presented in Table 7.2-1.

Table 7.2-1 Integrated Water System Requirments

Parameter		Requirements
Growth	1)	IOC systems shall have growth and on-orbit reconfiguration capability to accommodate changing demands in user fluid quantities.
·	2)	
Integrated Design	1)	System shall be integrated to minimize fluid management hardware development and operational cost.
Interface Hardware	1)	Fluid interface components shall be standardized and fluid transfer interface hardware shall be designed to preclude mating to the wrong connector.
Fluid Storage Requirements	a)	A fluid quantity measurement capability shall be provided in both the storage and resupply systems.
	2)	Leak detection, isolation, and control shall be provided and shall comply with station environmental and contamination requirements.
	3)	No liquids will be vented overboard.

7.3 INTEGRATED WATER SYSTEM DESCRIPTION AND CONFIGURATION

A schematic of the IWS is presented in Figure 7.3-1. The IWS will capture all water available from the NSTS Orbiter, the ECLSS and, if necessary, water resupplied from the Logistics module to meet water resupply requirements. The system will consist of a collection subsystem, a storage subsystem, and a distribution subsystem to supply all station users including the United States Laboratory, Japanese Experimental Module, Columbus, Propulsion, and the Integrated Waste Fluid System. The bladder type water storage tanks of the IWS will be pressurized by nitrogen from the integrated nitrogen system. When the water tanks are resupplied, excess nitrogen pressurant will be channeled to the integrated waste fluid system for propulsive disposal. An alternate solution to disposing the water would be to channel it through the electrolysis unit for a more efficient means of propulsive disposal through the oxygen/hydrogen thrusters.

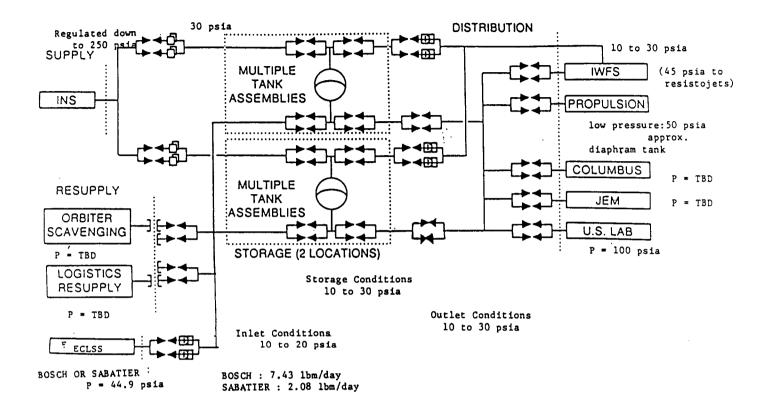


Figure 7.3-1 Schematic of the Integrated Water System

Parameters that affect the water balance of the integration system are listed in Table 7.3-1.

Table 7.3-1 Variables that Affect Space Station Water Balance and the Baseline Configuration

Parameters	Baseline Configuration
CO. Peduation Process in FCISS	Bosch
CO ₂ Reduction Process in ECLSS Station Crew Size	8
EVA's per 90 days	39
EVA duration	6
EMU Loop Closure	Closed
Food Water Content (1bm/man/day)	1.1
Orbiter Crew Size	8
Orbiter Crew on Station	4 .
Orbiter Power Level (kW)	10.0
Orbiter Stay Duration (days)	5
Orbiter Visits per 90 Days	2
Percentage of Water Recovery	85%
from Laboratory Experiments	

The configuration baselined for this study will be the BOSCH $\rm CO_2$ reduction process in the environmental control and life support system. This system will be capable of generating excess potable water at a rate of 7.43 lbm each day. This prediction is based on an eight person crew with 1.1 lbm of water in the food per man day. Alternatively, if the Sabatier $\rm CO_2$ reduction process was used only 2.08 lbm of excess potable per day would be generated.

Shuttle operations that have a major effect on the water balance include mission duration, power availability to the fuel cells while the shuttle is docked to the station, and the number of shuttle flights per year.

A NASA study indicated that excess potable water generated from the Orbiter may range from 342 lbm/visit (with the Space Station to orbiter $10~\rm kW$ power cord for a five day mission) up to 2538 lbm/visit (without the $10~\rm kW$ power cord for an eight day visit).

The NSTS orbiter also generates hygiene water which accumulates in the orbiter waste tanks during ascent to docking with the Station. This quantity of 254 1bm per visit is independent of mission duration and power cord use. Available potable and hygiene quantities generated under various operations are summarized in Table 7.3-2. The current shuttle operation scenario is a five day orbiter mission with a 10 kW station to orbiter power cord, and eight flights per year.

The present fluids inventory for the integrated water system is presented in Tables 7.3-3 and 7.3-4, and a component list is presented in Table 7.3-5. As water requirements become more apparent, fluid inventories will be revised to implement changes in the water balance and the integrated configuration.

Potable Water Hygiene Water Generated Per Flight Generated Per Flight (1bm/flight) Option (1bm/flight) 342 254 1) 5 Day Mission 10 kW Power Cord 254 1860 2) 5 Day Mission No Power Cord 254 2040 3) 8 Day Mission 10 kW Power Cord 2538 254 4) 8 Day Mission No Power Cord

Table 7.3-2 Excess Water Generated from the Orbiter

7.4 INTEGRATED WATER SYSTEM REFERENCES

- 1) Peterson, T., Space Station Fluid Inventories of the Integrated Waste Fluid and Integrated Water Systems, PIR No. 159. NASA Lewis Research Center, Cleveland, OH, March 25, 1987.
- 2) Fluids Technical Integration Panel Data. Presented at Marshall Space Flight Center, Huntsville, AL, October 1986.
- 3) Data provided by John Griffin at Johnson Space Center, April 1987.

Table 7.3-3 Integrated Water System Fluid Inventory Requirements

REMARKS		MATER ACCUMULATEION FROM LOG MODULE, ORBITER, AND ECLSS.	
		WATER ACCUMULATEION I	
FILID		POTABLE	OBT
RESUPPLY METHOD		FROM ORBITER AND EXCESS ECLSS POTABLE	FLUID TRANSFER FROM INS
RESUPPLY QUANTITY (IB/90 DAYS)	MAX	OET.	081
RESUPPLY QUANT	MEAN	TBD	TBO TBO
USAGE RATE	(LB/HR)	TBD T.BC	78C T.BC
QUANTITY		809	- F2
FLUID		1420	i GN2
FLUID		STORAGE	STORAGE
GIUIA		86 IWS	INS
2 S		8	a

Table 7.3-4 Integrated Water System Fluid Interface Requirements

The control of the	B	FLUID	I TLUID	divir	INIET AND	INIET AND CUTLET FLUID CONDITIONS	D CONDITION	SN	METHOD OF	FAILURE RE	KEMAKKS
THE	ģ 		SUBSTSTEE	3	TO	PRESSURE (PSIA)		(INCHES)			
IMS	2			H20		22	55	55.0	FILTER	SINGLE	
IMS	- 8		DISTRIBUTION			22	22	OBT	FILTER	SINGLE	
IMS	- 56 		DISTRIBUTION	H20	TWS	22	22	087	FILTER	SINGLE	
IMS DISFRIBUTION HZO IMS 10 TO 30 70 TBD FILTER 10 TO 30 70 TBD RESISTOJET 10 TO 30 70 TBD TBD	- -		DISTRIBUTION	H20	INS PROPULSION	22	22	08T	FILTER	SINCLE	
INS STORMAGE H20 LICG MODULE 10 TO 20 70 TBD RESISTOJET 10 TO 30 70 TBD TBD			DISTRIBUTION	H20	INS	22	22	TBO CBT	FILTER	SINGLE	
INS STORAGE HZO RELES 110 TO 20 70 TEBD RESISTOJET TWO TO 70 TEBD RESISTOJET	-		STORAGE			22	88	65 E	RESISTOJET	SINGLE	
	2			1H20	ECLSS TMS	110 170 20	22_	TBO CBT	 RESISTOJET 	SINGLE	

Table 7.3-5 Integrated Water System Component List

VENDOR PART NUMBER

NAME

213 IMS, SENSO 214 IMS, SENSO 211 IMS, VALVE 210 IMS, VALVE	REGULATOR, SENSOR, PRESSURE SENSOR, TEMPERATURE VALVE, CHECK VALVE, RELIEF	8 6 28 4	081 130 130 180 180	9 9 9 9 9 9	H20 H20 H20 H20	10.0 0.6 0.1 1.5	OET
2001 INS	TATUS SOLEMOTO TATCUTAG	 88	OH.	30	H20	3.0	TBO

8.0 INTEGRATED NITROGEN SYSTEM (INS)

8.1 INTEGRATED NITROGEN SYSTEM OVERALL REQUIREMENTS

At IOC, the INS will provide nitrogen to the Environmental Control and Life Support System (ECLSS), Integrated Waste Fluid System (IWFS), Integrated Water System (IWS), U.S. Laboratory (USL), Columbus, and the Japanese Experimental Module (JEM). The INS will be scarred at IOC for high pressure requirements relative to Extravehicular Activity (EVA) Systems such as the Extravehicular Excursion Unit (EEU) and the Enhanced Mobility Unit (EMU) with additional high pressure requirements for the Orbital Maneuvering Vehicle (OMV) and the Servicing Facility. The Servicing Facility will also require scarring of the INS for a low pressure port for post IOC.

8.2 INTEGRATED NITROGEN SYSTEM REQUIREMENTS

Fluid system requirements for the integrated nitrogen system are presented in Table 8.2-1.

Table 8.2-1 Integrated Nitrogen System Fluid System Requirements

<u>Parameter</u>		Requirements
Growth	1)	IOC systems shall have growth and on-orbit reconfiguration capability to accommodate changing demands in user fluid quantities.
	2)	System shall incorporate scarring to accommodate additional integrated system at logical full operational capability.
Integrated Design	1)	System shall be integrated to minimize fluid management hardware development and operational cost.
Interface Hardware	1)	Fluid interface components shall be standardized and fluid transfer interface hardware shall be designed to preclude mating to the wrong connector.
Fluid Storage	1)	A gas quantity measurement capability shall be provided in both the storage and resupply subsystems.

8.3 INTEGRATED NITROGEN SYSTEM DESCRIPTION AND CONFIGURATION

The INS will consist of a resupply subsystem, emergency storage subsystem, and a distribution subsystem, and will include all hardware and software required to provide the functions of resupply, transfer, storage, conditioning, distribution, as well as control and monitoring of the nitrogen within the INS. A functional diagram is shown as Figure 8.3-1. The INS fluid resupply requirements are shown in Table 8.3-1 and the INS fluid interface requirements are shown in Table 8.3-2.

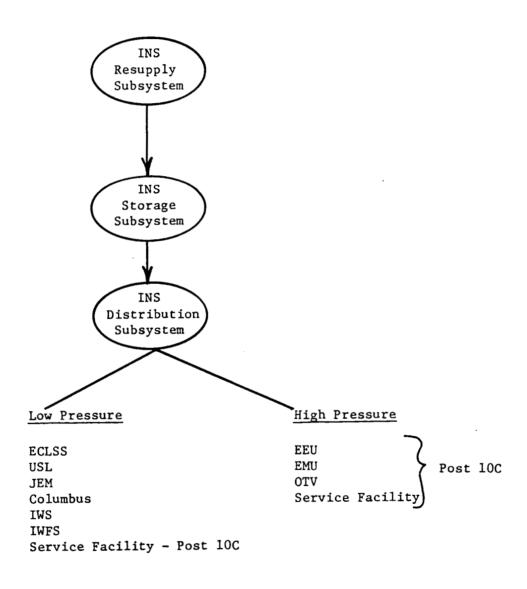


Figure 8.3-1 Integrated Nitrogen System Functional Diagram

Table 8.3-1 Integrated Nitrogen System Inventory Requirements

Ž	NO. SYSTEM	SUBSYSTEM	TYPE	STORED	RATE			METHOD	COMPOSITION	_	
						MEAN	MAX				
	60 INS	DISTRIBUTION	GN2	N/A	TBD TBD	TBO TBO	L TBO	UNPRESSURIZED LOGISTICS MODULE GN2	W2	SEE SECTION 8.1.3	
	18 TNS	DISTRIBUTION	GN2	- N	TBO TBO	TBO TBO	OEL -	 UNPRESSURIZED LOGISTICS MODULE GN2 	-N2	SEE SECTION 8.1.3	
	62 INS	DISTRIBUTION	- GN2	- N/A	1180 TBD		Off	 UNPRESSURIZED LOGISTICS MODULE GN2 	.w2	 SEE SECTION 6.1.3	
	63 IINS	DISTRIBUTION	GN2		 TBO TBO			UNPRESSURIZED LOGISTICS MODULE GN2		SEE SECTION 8.1.3	
	64 INS	DISTRIBUTION	- CN2	 	1180 TBD	TBO TBO	OET -	UNPRESSURIZED LOGISTICS MODULE GN2	-N2	SEE SECTION 8.1.3	
	65 INS	DISTRIBUTION	GN2	W/W	1390 1390	OBTIONT	9	UNPRESSURIZED LOGISTICS MODULE GN2	28	SEE SECTION 0.1.3	
٠	70 INS	RESUPPLY	GN 2	65	TBO TBO	TBO TBO	Off	UNPRESSURIZED LOGISTICS MODULE GN2		PER PALLET DATA, 2 PALLETS ON STATION BROUGHT UP BY THE UMFRESSURIZED LOGISTICS MODULE SEE 8.1.1	
<u> </u>	SNI 6L	STORAGE	<u> </u>	780	TBO TBO	TBD N/A	N/A	UNPRESSURITED LOGISTICS MODULE (ON 2		PER PALLET DATA, 2 IDENTICAL PALLETS ON STATION, SEE SECTION 8-1.2	

Table 8.3-2 Integrated Nitrogen System Fluid Interface Requirements

a	OINTA I	GIOTA I	FLUTD	INLET AND OUTLET FLUID CONDITIONS	OTLET FLUIL	CONDITION	s	METHOD OF	FAILURE TOLERANCE	REMARKS
ġ	SYSTEM	SUBSTSTEM	3311	PROM	PRESSURE (PSIA)	TEMP.	(LINE SIZES)	2		
8	INS	DISTRIBUTION	GN2	INS, RESUPPLY ECLES	4000 250/750	67 67	85	N/A	SINGLE	SEE SECTION 8.1.3
81	INS	DISTRIBUTION	 	INS, RESUPPLY	4000	22	TBO	W/N	SINGLE	SEE SECTION 8.1.3
83	INS	DISTRIBUTION	- CW2	INS, RESUPPLY INFS	4000	88	OBT.	IN/A	SINGLE	SEE SECTION 8.1.3
83	INS	DISTRIBUTION	CN2	INS, RESUPPLY	4000	22	0E 0E	N/A	SINGLE	SEE SECTION 6.1.3
2	INS	 DISTRIBUTION 	- Canz	INS, RESUPPLY JEM	4000 250/750	88	OUT	N/A	SINGLE	SEE SECTION 8.1.3
22	INS	DISTRIBUTION	- GW 2	INS, RESUPPLY COLUMBUS	4000 250/750	55	OBT	N/A	SINGLE	SEE SECTION 8.1.3
2	INS	RESUPPLY	25	INS, RESUPPLY INS, DISTRIBUTION	4000	07 07	TBO TENO	N/A	SINGLE	PER PALLET DATA, 2 PALLETS ON STATION BROUGHT UP BY THE UNPRESSURIZED LOGISTICS MODULE SEE 0.1.1
85	INS	STORAGE	ON 2	INS, RESUPPLY INS, DISTRIBUTION	4000	66	TBO TBO	N/A	STWEETE	PER PALLET DATA, 2 PALLETS ON STATION, W/BOTH PALLETS THREE FAILURE TOLERANCE EXISTS.SEE 8.1.2

8.3.1 Resupply Subsystem

The INS resupply subsystem will consist of the tankage, mounting hardware, conditioning, thermal control, transfer, and control and monitoring hardware for delivery of the nitrogen to the Space Station (SS). The resupply hardware will be integrated and delivered to the SS by the Logistics System. The INS resupply subsystem will be capable of being located at two interface locations on the truss that are optimized for on-orbit operations including EVA operations. The INS resupply subsystem performs the dual function of resupply and storage of the nitrogen delivered to SS to satisfy all user requirements. The resupply subsystem will be a GN2 blowdown supply system that at full tankage conditions is at 3000 to 4000 psi to optimize tankage mass fraction. At depletion of the first pallet the second resupply pallet mounted on station would take over the resupply operation and the depleted pallet would be removed and replaced. Figure 8.3-2 shows the schematic of the INS resupply subsystem with the corresponding components listing shown as Table 8.3-3.

8.3.2 Storage Subsystem

The INS storage subsystem will provide sufficient storage capacity to satisfy emergency ECLSS requirements for hyperbaric airlock and safe-haven operations. The INS storage subsystem is located external to the modules in the truss. Each pallet will retain 780 lbm of GN₂ stored at 3000 to 4000 psi and used only for safe haven or hyperbaric airlock operations. The schematic is shown as Figure 8.3-3 with the corresponding components list shown as Table 8.3-4.

8.3.3 Distribution Subsystem

The INS distribution subsystem will transfer the nitrogen from the INS storage subsystem at 3000 to 4000 psi and will reduce the pressure to 250 to 750 psi for low pressure use and will then route the nitrogen to the various user interfaces. The INS distribution subsystem consists of the plumbing. connectors, thermal control, conditioning, structural attachment, and control and monitoring hardware to distribute nitrogen to both high and low pressure users. All high pressure users at the present time are post 10C and therefore the INS is scarred for eventual high pressure applications as indicated. The schematic shown as Figure 8.3-4 reflects the potential hardware to reduce the 3000 to 4000 psi supply to 3000 psi for use, but is only a tentative solution pending further requirement definition. For this reason the component listing shown as Table 8.3-5 list the scarring requirements and not the potential future growth hardware. The INS distribution subsystem and will be located both internal to the pressurized portions of SS as well as eventual future growth externally along the truss system to supply the Servicing Facility and OMV requirements.

8.4 INTEGRATED NITROGEN SYSTEM REFERENCES

- 1) Architectural Control Document Fluid Management System; Section 1: Integrated Nitrogen System, NASA JSC 30264. December 1, 1986.
- 2) Space Station Program Definition and Requirements, Section 3, System Requirements Rev. A, SS-SRD-0001. January 12, 1987.

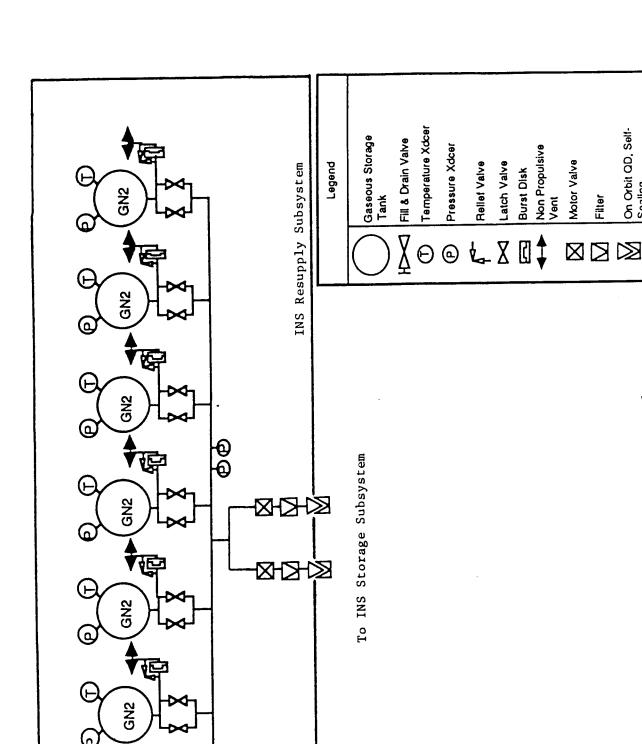


Figure 8.3-2 Integrated Nitrogen System Resupply Subsystem Schematic

On Orbit QD, Self-Sealing

Filter

Table 8.3-3 Integrated Nitrogen System Resupply Subsystem Component List

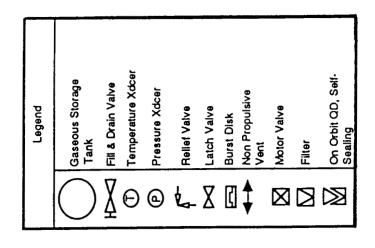
125 11	APPLICATON	OMEONENT TYPE	N CON	SIZE (in)	PRESSURE MEOP (psia)	USAGE MEDIA 	APPROX MASS (1b)	VENDOR NAME	VENDOR PART NUMBER
- - -	INS, RS	DI SCONNECT,	7	er.	4000	GN2	136	130	OET.
	INS, RS	FILTER, INLINE		OET.	4000	CM2	OET.	OET	D
123	INS, RS	MISC, VENT ASSY, NON-PROPULSIVE	•	180	0004	CN2	OBT	130	OBT
-1011	INS, RS	PRESSORE VESSEL,	• 	1180	000	GN2	OEL C	OE:	
126	INS, RS	SENSOR, PRESSURE	.	1180	000+	SM2		061	9
127 I	INS, RS	SENSOR, TEMPERATURE	• 	180	000+	GN2	OEL	130	TBD
- [611	INS, RS	VALVE, MANUAL, SERVICE		TBD	0000	GN2	OB.	061	OET -
н 	122 INS, RS	VALVE, RELIEF W/BD	• - - -	OBT	000+	GN2	OEL OEL	061	081
1201	INS, RS	VALVE, SOLENOID, LATCHING	12	1380	000+	GN2	OE .	OET	OET.
121	INS, RS	VALVE, TORQUE MOTOR		087	0004	GN2	OET.	130	OET

Table 8.3-4 Integrated Nitrogen System Storage Subsystem Component List

PROGRAM APPLICATON	COMPONENT TYPE	RECO	SIZE (in)	PRESSURE MEOP (psia)	USAGE	APPROX MASS (1b)	VENDOR NAME	VENDOR PART	
134 INS, SS	DI SCONNECT,	-	Off	4000	98	OET	1380	- TE	
133 INS, SS	FILTER, INLINE		OET	4000	SK2	OB.	OET	1380	
INS, SS	MISC, VENT ASSY, NON-PROPULSIVE		TBO	4000	GN2	ÖE	TBO	1360	
INS, SS	PRESSURE VESSEL,		TIBO C	4000	8	Ē	OET .	OE .	
135 INS, SS	SENSOR, PRESSURE	· ·	TBO	4000	GN2	OET	OET	OBT	
136 INS, SS	SENSOR, TEMPERATURE	e	TBO	4000	GN2	OET	TBD	130	
INS, SS	VALVE, RELIEF W/BD	 m	TBO	4000	GN2	OET.	OET 1	04ET	
129 INS, SS	VALVE, SOLENOID, LATCHING	•	OET	4000	GN2	OET.	TBD	DET .	
130 INS, SS	VALVE, TORQUE MOTOR		TBO	4000	GW2	OET .	_ T80	Off.	
		APPLICATON	APPLICATON DISCONNECT, FILTER, INLINE HISC, VENT ASSY, NON-PROPULSIVE PRESSURE VESSEL, SENSOR, TEMPERATURE VALVE, RELIEF W/RD VALVE, SOLEMOID, LATCHING VALVE, TORGUE NOTOR	TYPE TYPE	APPLICATON	PRESCUE PRESCUE PRODUCED PRESCUE PRODUCED PRESCUE PRODUCED PRESCUE PRODUCED PRODUCED PRODUCED PRODUCED PRODUCED PRODUCED PRODUCED PRODUCED PRESCUE PRE	PRESCUE NO. TYPE REQ (1A) (psis) DISCONNECT, 4 TRD (psis) DISCONNECT, 4 TRD (psis) DISCONNECT, 4 TRD (psis) DISCONNECT, 4 TRD (4000 GAIZ G	DISCONNECT, TYPE RED. (1n) (pais) USAGE (1b) (APICATON APICATON CANAGE (1b) MASS (PRESSURE TYPE

Table 8.3-5 Integrated Nitrogen System Distribution Subsystem Component List

PROGRAM APPLICATON	142 INS, DS DISCONNECT,	141 INS, DS FILTER, INLINE	143 INS, DS REGULATOR	144 INS, DS SENSOR, B	145 INS, DS SENSOR, E	146 INS, DS SENSOR, 1	139 INS, DS VALVE, SC	140 INS, DS VALVE, SC	137 INS, DS VALVE, TC	_
COMPONENT TYPE	, E	INLINE	REGULATOR, ELECTRONIC, M/RELIEF	SENSOR, PRESSURE	SENSOR, PRESSURE	SENSOR, TEMPERATURE	VALVE, SOLENOID, LATCHING	VALVE, SOLENOID, LATCHING	VALVE, TORQUE MOTOR	
RECO	2		~~-	- -		~			 	-
SIZE (11)	TBD	TBD	TBO	CBT	1180	TBD	TBO	TBO	TBD	
PRESSURE MEOP (psia)	4000	4000	4000/150	4000	750	750	4000	150	4000	
USAGE	GN 2	GN2	GN 2	GN2	GN2	SZ SZ	GN2	GN2	GN2	
APPROX MASS (1b)	TBO	QE .	9	138 OE	92	OET		7.30	OET.	
VENDOR NAME	1300 1300	UST	TBD	TBD	TBO	TRD	TBD	TBD	TBD	CQ.
VENDOR PART NUMBER	- 1 0E	OST.	13 0	OBT.	TBD	TBD	08T	TBD	1780	Car



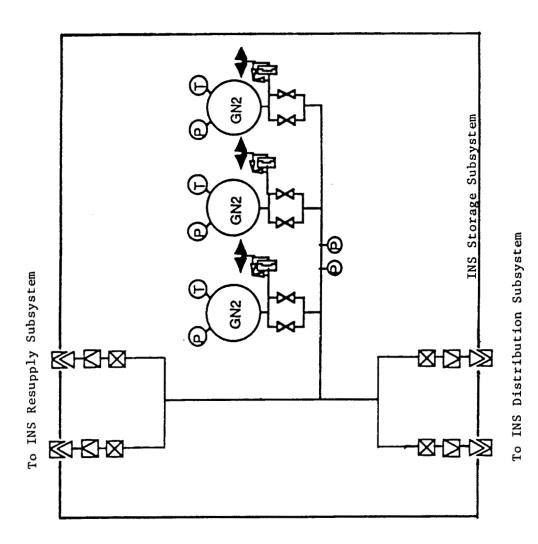


Figure 8.3-3 Integrated Nitrogen System Storage Subsystem Schematic

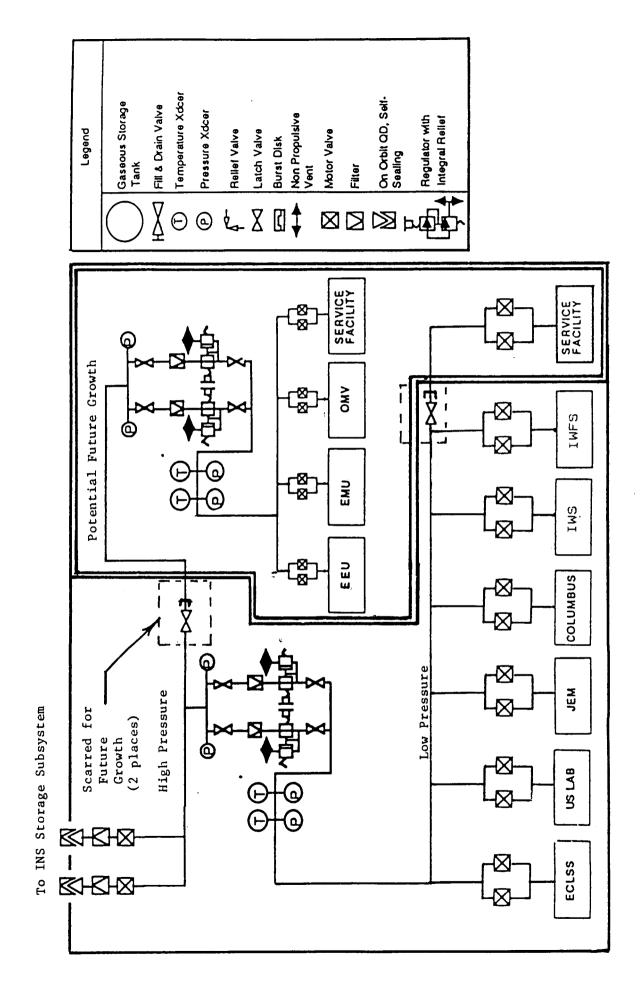


Figure 8.3-4 Integrated Nitrogen System Distribution Subsystem

9.0 ENVIRONMENTAL CONTROL AND LIFE SUPPORT SYSTEM

9.1 ENVIRONMENTAL CONTROL AND LIFE SUPPORT SYSTEM OVERALL REQUIREMENTS

The Environmental Control and Life Support System (ECLSS) is an integrated system that services the entire Space Station. It provides a safe and habitable environment for the entire crew, including the international modules. Due to the high degree of commonality in the system, the ECLSS provides each module with the necessary environmental control. The system also interfaces with the nodes, airlocks, and logistics carrier. Because the ECLSS is functionally a regenerative closed system, only those fluids and gases piped into and out of the entire system will be discussed and quantitatively presented. The function and operation of each component will be briefly presented. The primary function of the ECLSS is to provide a shirt sleeve environment for the Space Station crew members. The ECLSS is divided into six subsystems; 1) Temperature and Humidity Control (THC), 2) Atmosphere Control and Supply (ACS), 3) Atmosphere Revitalization (AR), 4) Fire Detection and Suppression (FDS), 5) Water Recovery and Management (WRM) and 6) the Waste Management (WM). Fluid requirements for these subsystems are presented in Table 9.2-1.

9.2 ENVIRONMENTAL CONTROL AND LIFE SUPPORT SYSTEM FLUID SUBSYSTEMS REQUIREMENTS

Table 9.2-1 ECLSS Subsystem Fluid Requirements

ECLSS Subsystem	<u>Flu</u>	id Requirements
Temperature and Humidity Control	1)	Cabin air temperature and humidity control. (nominal module temperature range 65°F - 80°F)
	2)	Intermodule ventilation.
	3)	Avionics Air Cooling.
Atmospheric Control and	1)	
Supply		a) PPO ₂ ; 2.83 psia to 3.35 psia b) PPN ₂ ; 11.35 psia to 11.87 psia
	2)	c) Total pressure; 14.7 ± .2 psia Vent and relief.
	3)	O ₂ /N ₂ storage and distribution.
Atmospheric Revitalization	1)	CO ₂ removal through regenerative process.
	2)	•
	3)	O ₂ generation (KOH Static Feed). Electrolysis Unit as primary source of O ₂ .
	4)	Contaminant control.
	5)	Contaminant monitoring.
Fire Detection and	1)	
Suppression	2)	Fire suppression.
	3)	Crew protection.

Table 9.2-1 ECLSS Subsystem Fluid Requirements (Continued)

Water Recovery and Management

- Potable and hygiene water processing.
 Collect, process and dispense water to meet crew needs.
- Urine/flush processing. Process and dispose of urine an fecal matter from crew members.
- Water storage and distribution. Provide a closed-loop recovery system for potable and hygiene water. (TIMES)
- 4) Water thermal conditioning.
- 5) Water quality control and monitoring.
 Ensure proper water quality through pretreatment, post-treatment, and monitoring.
- Trash collecting and processing.
 - 2) General housekeeping.
 - 3) Commode and Urinal.
 - 4) Storage of brine, solid carbon, and feces canister in pressurized logistics carrier.

Waste Management

9.3 ENVIRONMENTAL CONTROL AND LIFE SUPPORT SYSTEM FLUID SUBSYSTEMS DESCRIPTIONS AND CONFIGURATIONS

The primary function of the ECLSS system will be to maintain a habitable environment for the entire station. A schematic of the entire ECLSS is shown in Figure 9.3-1. The system will be comprised of six separate subsystems including a Temperature and Humidity Control (THC), Atmosphere Control and Supply (ACS), Atmospheric Revitalization (AR), Fire Detection and Suppression (FDS), Water Recovery and Management, and Waste Management. Each subsystem will interface with one or all the other subsystems so that they will comprise a functionally closed loop system that will require scheduled fluid resupply of nitrogen only, for leakage makeup and airlock losses.

The primary ECLSS user interfaces are in areas of avionics air cooling and air contamination control. The thermal control interfaces include cabin heat exchangers, avionics heat exchangers, and air revitalization equipment. Manned Systems interfaces include the commode, shower, hand wash, and both clothes and dish washers.

Tables 9.3-1 and 9.3-2 provide fluid storage, resupply and interface requirements. Table 9.3-3 provides a list of all the components included in the ECLSS.

9.3.1 Temperature and Humidity Control (THC) Subsystem

The THC subsystem will be capable of providing three primary functions. The first will be to remove heat produced by equipment racks through the avionics air cooling system. The second will be to provide intermodule ventilation by moving air from one cabin to the next to ensure complete mixing of the station air. Finally, the THC will provide a shirt-sleeve environment in the station. By maintaining the required nominal humidity level, the cabin cooling package will provide condensate that is passed to the condensate water loop of the Water Recovery and Management (WRM) subsystem.

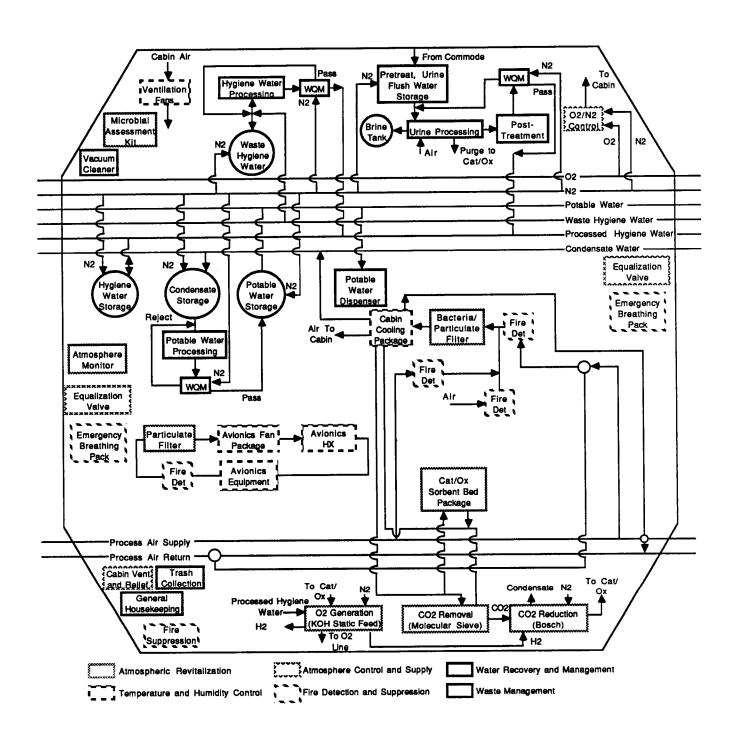


Figure 9.3-1 Environmental Control and Life
Support System (ECLSS) Schematic

Table 9.3-1 ECLSS Fluid Inventory Requirements

REMARKS		MODULE LEAKAGE 6 AIRLOCK LOSSES	MODULE LEAKAGE & AIRLOCK LOSSES	STORED FOR TRANSPORT TO EARTH	FROM WEIT FOOD	USING BOSCH COZ REDUCTION	USING BOSCH COZ REDUCTION	USING BOSCH CO2 REDUCTION	USING SABATIER CO2 REDUCTION	NOT STOICHIOMETRIC REACTION IN SABATIER
COMPOSITION		PURE MODUI	PURE (MODU)	36% SOLIDS STOR	FROM	POTABLE USIN	PURE USIN	NISO!	 POTABLE USIN	INOT
RESUPPLY		FILID TRANSFER FROM INS	ELECTROLYSIS	TAKE TO EARTH	FOOD FROM PLC	ECLSS EXCESS	EXCESS FROM ELECTROLYSIS	FROM BOSCH	ECLSS EXCESS	FROM SABATIER
(I.B/90 DAYS)	MAX	<u> </u>				-=-	_ <u>=</u> _	-=-	-=-	
RESUPPLY QUANTITY (LB/90 DAYS)	HEAN	432								
USAGE I	(IB/HR)	LEARAGE MAKEUP 43	LEAKAGE MAKEUP	0.220 NOM	0.046 NOM	0.310	0.018	0.203	0.067	0.443
QUANTITY	2	N/A	216	90				_==-		
GIMIA	11111	GN2	89	BRINE	H20	H20	CH2	CARBON, SOLID	1420	002/СН4
FLUID	SUBSYSTEM	ACS	ACS	¥	WRH		MECH	MEN	MSW	
FLUID	SYSTEM	ECLSS	ECISS IN	ECISS	ECLSS	ECLSS IN	ECLSS	BCLSS IN	BCISS IN	ECLSS W
- QI	 2		2 2	=	2		7	25	9.	F

Table 9.3-2 ECLSS Fluid Interface Requirements

CLISS ACS CW2 RESULTAN FROM PRESURE TRAP. LINE SITES MANAGENT	9 2	FLUID	I FLUID	TYPE	INIET AND	INLET AND OUTLET FILLID CONDITIONS	CONDITION		METHOD OF WASTE	FAILURE	REMARKS
MCS GR2 INS INS 14.7 10 3/6 LOSSES AND VENTING 14.7 14.7 19.0 3/6 LOSSES AND VENTING 14.7 14.7 180-200 170 3/6 LOSSES 4 VENTING 14.7 14.8 14.					FROM	PRESSURE (PSIA)		LINE SIZES	MANAGEMENT		
ECLES ACS CO2 CO STOTANGE PALLET 180-200 TBD 3/6 LOSSES 4 VENTING			I NCS	GN2	INS HODULE/NODE/AL	750 OR 250	2,2	3/8	LOSSES AND VENTING		DURING SAFE-HAVEN AND HYPERBARIC AIRLOCK OPERATIONS THE SUPPLY JUMPS FROM 250 TO 750 PSIA
ECISS Net IRRINE ITIMES TITMES STORE IN TANUS TO TRANSPORT ECISS NRM H2O POCO 107 NB POCO 111 NB ECISS NRM H2O BCLSS 141.9 NABIENT ITIMES ECISS NRM ICARBON, SOLID BOCCH 100 90 INFS ECISS NRM ICARBON, SOLID BOCCH 141.9 NABIENT STORE IN PLC ECISS NRM ICARBON, SOLID BOCCH 141.9 NABIENT STORE IN PLC ECISS NRM ICARBON, SOLID BOCCH 141.9 NABIENT STORE IN PLC ECISS NRM ICARBON, SOLID BOCCH 141.9 NABIENT STORE IN PLC ECISS NRM ICACHA ICACHA ICACHA ICACHA ICACHA			- ACS	- C00 C00	OZ STORAGE PALLET MODULE/NODE/AL		TBD AMBIENT	13/8	LOSSES & VENTING		
NECLES NRW HZO FOOD FOOD FOOD TITHES TITHES			I		TIMES				STORE IN TANKS TO TRANSPORT		
NELLSS NEW HZO ECLSS 141.9 MBIENT NELLSTROLYSIS 100.30 MBIENT NELLSTROLYSIS 180 200 NELLSTROLYSIS 180 200 NELLSTROLYSIS 100 90 100			MRM	H20	FOOD URINE PROCESSING				TIMES		
ECLES INCH CGH2 INCH ELECTROLYSIS 180 200 INFS IN			MEN	H20	BCLSS	144.9	AMBIENT				Воѕсн
ECLES WRM CARBON, SOLID BOSCH 900-1340 STORE IN PLC INCLUDIO PLC IAMSIENT IAM			- 148. H	- C#3	KOH ELECTROLYSIS	100	8.00		IMES		BOSCH, STORED IN HYDRIDE TANK
ECLES NEW			WRW	CARBON, SOLID	BOSCH		980-1340 AMBIENT		STORE IN PLC		Воѕся
ECLSS WRM CO2/CH4 SABATER TBD 600-900 IMPS 114.7 70 10 10 10 10 10 10 1			MR.M.	1 H20	ECLSS IWS	144.9	AMBIENT AMBIENT				SABATIER
			- MRM	(CO2/CH4	SABATIER IWES	TBD 14.7	000-900 170		IMPS		SABATIER

Table 9.3-3 ECLSS Component List

VENDOR PART NUMBER 8 8 ê **E E** VENDOR NAME 8 8 8 APPROX MASS (1b) 1000.0 5.0 5.0 8.0 AIR AIR AIR AIR AIR H20, G02, GH2 HALON 1301 HALON 1301 URINE BRINE AIR, CO2 ALR ALR USAGE AIR PRESSURE MEOP (psia) 30 200 30 14.9 200 **E E** 17B0 .375 17B0 17B0 SIZE (1n) Ö E OF 05 2: OF 05 0F X E SE SE ONT ONT REGO PRESSURE VESSEL, PROCESSED HYGIENE MATER PRESSURE VESSEL, EMERGENCY WASH WATER MISC, PROCESSING UNIT, POTABLE WATER MISC, PROCESSING UNIT, WASTE HYGIENE PRESSURE VESSEL, WASTE HYGIENE WATER CONTROL, N2 RESUPPLY PRESSURE PRESSURE VESSEL, CONDENSATE WATER PRESSURE VESSEL, FIRE SUPPRESSANT PRESSURE VESSEL, HYGIENE WATER PRESSURE VESSEL, POTABLE WATER HISC, DISPENSER, POTABLE WATER MISC, PRESSURE CONTROL SYSTEM MISC, MONITOR, WATER QUALITY COMPONENT FILTER, AVIONICS PARTICULATE MISC, ELECTROLYSIS UNIT, KOH MISC, MOLECULAR SIEVE, 4-BED FILTER, BACTERIA/PARTICULATE HISC, CO2 REDUCTION, BOSCH MISC, REFRIGERATOR/FREEZER MISC, MONITOR, ATMOSPHERE MISC, CATALYTIC OXIDIZER MISC, CABIN COOLING PKG MISC, CONTROLLER, PYRO REGULATOR, DOWNSTREAM VALVE, EQUALIZATION MISC, BRINE STORAGE MISC, FECAL STORAGE MISC, SORBENT BED PRESSURE VESSEL, VALVE, RELIEF PROGRAM APPLICATON 100 ECLSS, FDS 89 ECLSS, ACS 113 ECLSS, ACS 101 ECLSS, FDS 91 ECLSS, THC 104 ECLSS, WRM ECLSS, ACS 90 ECLSS, ACS ECISS, ACS ECLSS, WRM ECLSS, WRM 106 ECLSS, WRUM 108 | ECLSS, WRM ECLSS, WRM 105 ECLSS, WRM 112 ECLSS, WRM ECLSS, AR 116 ECLSS, WM 117 ECLSS, WM ECLSS, AR ECLSS, AR ECLSS, AR DCLSS, AR 96 ECLSS, AR ECLSS, AR ECLSS, AR 103

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9.3.2 Atmosphere Control and Supply (ACS) Subsystem

The ACS subsystem will maintain the partial and total pressures of $\rm O_2$ and $\rm N_2$ in the modules and will be responsible for storage and distribution of both $\rm O_2$ and $\rm N_2$. The ACS subsystem provides $\rm N_2$ for leakage makeup, airlock losses, tank back pressurization/water transfer, and purge for the air revitalization and waste management systems.

The oxygen required for daily use, i.e., leakage makeup and airlock uses will be generated by the electrolysis unit in the Atmospheric Revitalization (AR) subsystem. This oxygen will be stored in accumulators at 3000 psia. The nitrogen required for daily use will be stored as part of the Integrated Nitrogen System (INS) resupply subsystem (see Section 8.1-1). Nitrogen storage will also be provided for safe-haven or emergency conditions as part of the INS storage subsystem. There will be an oxygen storage tank for safe-haven or emergency conditions that will require resupply only if the oxygen is exhausted during adverse conditions. The oxygen and nitrogen will be distributed to the ACS subsystem as needed at 180-200 psia and 200-250 psia respectively.

9.3.3 Atmospheric Revitalization (AR) Subsystem

The AR subsystem will perform several vital functions. The first will be to both monitor and control any contaminants in the modules. The other functions will interface with both the WM and ACS subsystems. The AR subsystem will generate oxygen using a KOH Static Feed Electrolysis Unit. To do this, the unit will use processed hygiene water from the WRM subsystem and N2 from the ACS subsystem. The oxygen produced will be transferred to the ACS 02 line, and the hydrogen will be transferred to the CO2 reduction system as needed, with the remaining H2 going to the Integrated Waste Fluid System.

The AR subsystem will also remove $\rm CO_2$ from the atmosphere using a Four-Bed Molecular Sieve. The $\rm CO_2$ that is collected during the $\rm CO_2$ removal in the molecular sieve will then be reduced in the $\rm CO_2$ reduction unit. This will be accomplished using either a Bosch Carbon Reactor or a Sabatier Methanation Reactor Subsystem.

During the ${\rm CO}_2$ removal process in the Bosch, the water condensed will be put into the WRM condensate water line. The hydrogen required for the reaction will be acquired from the electrolysis unit.

As with the Bosch, the condensed water from the Sabatier process will be transferred into the condensate line of the WRM subsystem. The methane will be transferred to the Integrated Waste Fluid System for appropriate disposal.

9.3.4 Fire Detection and Suppression (FDS) Subsystem

The FDS subsystem will be fully charged when brought onboard and will not require resupply. Air from the cabin and the process air supply will be passed through the FDS subsystem for detection of possible fires before entering the cabin cooling package. The FDS subsystem will not alter the air in any way. The air will return to the cabin or process air return duct, or sent to the ${\rm CO}_2$ removal system as needed.

9.3.5 Water Recovery and Management (WRM) Subsystem

The WRM subsystem will interface with the THC, the ACS, and the AR subsystems. The WRM will be a closed loop system that does not require resupply. In fact, the WRM subsystem will supply excess water to the integrated waste system. The source of the water for the WRM will be in the form of moisture in the food. The moisture will enter the WRM subsystem through perspiration and urine. The perspiration will condense in the cabin cooling loop and enter the condensate loop to be processed for potable water. The urine will enter the urine processing loop.

For the urine processing, the TIMES, a distillation-based unit using membrane evaporation for unique phase separation will be used. Waste water will enter the unit and be preheated by a regenerative heat exchanger, filtered and heated by a Thermoelectric Device (TED) to operating temperature. The waste water will be passed through the Hollow Fiber Membrane (HFM) evaporator module where a portion of the consultant water will be evaporated into steam. The bulk of water not turned to steam will continuously recycled through the module until the solids concentration reaches a predetermined limiting level at which time this brine will be dumped to a collection tank. The brine collection tank will be part of the waste management subsystem. The tanks will be located near the TIMES and changed out when full. The full brine tanks will be stored in the Pressurized Logistics Module. The product steam will flow to the cold side of the TED where most of the steam will be condensed and the latent heat reclaimed and transferred back to the waste water heating side of the TED.

Additional condensation will occur in the regenerative heat exchanger and complete steam condensation will occur in the fan-cooled heat exchanger. The presence of noncondensible gases and condensate will result in a two-phase mixture requiring a gas-liquid separator. The separated noncondensible gases will be vented to a vacuum source and the pressurized condensate checked for conductivity. Acceptable condensate will be passed to the processed hygiene loop. Reject water will be returned to the recycle loop. A pulse valve/pressure sensor combination will ensure optimum operating steam pressure in the evaporator. A gas orifice will be provided to minimize pressure pulses.

The processed hygiene water will be used for wash purposes and water electrolysis. The hygiene water can be put back into the potable loop by latent loads from laundry, dishwash, and hygiene water in the form of condensate. Excess potable can also be transferred to the hygiene loop if needed.

9.3.6 Waste Management (WM) Subsystem

The WM subsystem will include the commode and urinal which interface with WRM subsystem. The WM subsystem will provide storage for the waste products of both the WRM and AR subsystems. The WM subsystem will store the urine brine, feces canisters, and carbon produced in the ${\rm CO}_2$ reduction unit in the pressurized logistics carrier.

9.4 ENVIRONMENTAL CONTROL AND LIFE SUPPORT SYSTEM REFERENCES

Space Station Definition and Preliminary Design, WP-01, Book 3 - U.S. Lab Module, SSP-MMC-00031 (Rev. B) NAS8-36525. Martin Marietta Denver Aerospace, October 1986.

Space Station Definition and Preliminary Design, WP-01, Book 10 Airlocks. SSP-MMC-00031 (Rev. A), NAS8-36525. Martin Marietta Denver Aerospace, June 1986.

Larkins, J. T., Wagner, R. C., and Gopikanth, M. L., A Space Station Utility - Static Feed Electrolyzer. Presented at ICES Conference, Life Systems, Inc., July 1986.

Data submitted by Jim Reuter, Marshall Space Flight Center, Huntsville, AL, April 30, 1987.

Fluids Technical Integration Panel Data. Presented at Marshall Space Flight Center, Huntsville, AL, October 1986.

10.0 THERMAL CONTROL SYSTEM

10.1 THERMAL CONTROL SYSTEM OVERALL REQUIREMENTS

The Thermal Control System shall be an integrated system which maintains structures, ancillary compartments, components, subsystems and user payloads within their specified thermal limits. The TCS will be a closed loop system that does not require scheduled fluid resupply and will be considered independent from the integrated fluid systems. Accommodations will be made in the system TCS for fluid leakage and system purging to remedy system contamination. Overall thermal control system requirements are provided in Table 10.1-1.

Table 10.1-1 Thermal Control System Overall Requirements

- 1) Structures/Environmental Protection
 - Maintain Space Station Program Element (SSPE) structures, systems and subsystems within required temperature ranges using passive thermal control techniques or by efficient integration with the acquisition and transport subsystems.
- 2) Waste Heat Acquisition/Transport
 - Provide waste heat acquisition and transport within each pressurized element.
 - Collect, transport, and where feasible, utilize waste heat generated from Station elements for use in airlocks, interconnects and intramodular elements.
- 3) Heat Rejection
 - United States modules shall provide a low temperature heat sink to support requirements for refrigerators and freezers.
 - Heat acquisition and transport systems shall provide continual service during all normal vehicle operating environments and orientations to U.S. pressurized elements.

10.2 THERMAL CONTROL SYSTEM FLUID SYSTEM REQUIREMENTS

The TCS design is required to provide modular growth capability and on-orbit reconfiguration capability to accommodate multiple heat loads of varying magnitudes, heat flux densities, temperature levels and locations. The U.S. Modules and attached elements shall provide heat collection, transport and rejection capabilities at the levels provided in Table 10.2-1.

Table 10.2-1 Thermal Control System Heat Rejection Capability

Element	Thermal Load (kW)	Temperature Range (°F)
Habitation		
Internal Loop	25	40 - 120
Resource Node	25	40 - 120
United States Lab		
Internal Loop	50	40 - 120
Resource Node	25	40 - 120
Logistics	10	40 - 120
Airlock	TBD	TBD
Hyperbaric Airlock	TBD	TBD
Resource Node	TBD	TBD

Interfaces

The thermal design shall easily interface with equipment, subsystems and payloads. The interface shall not, where practical, require making and/or breaking of fluid connections for maintenance and refurbishment or experiment installation.

Manned Pressurized Element

Thermal acquisition and transport systems shall be capable of transporting the elements waste heat to a central thermal bus interface. Internal loop designs shall be based upon a single phase water system. Heat rejection/transfer to the station central thermal bus will be through bus interface heat exchangers attached externally to the elements. This method will be used by both U.S. Manned Pressurized Elements and International Modules. The exception to this will be the Logistics Module/Airlock Internal Thermal Support Loop which will be connected to the central thermal bus through an internal interface with a core station internal loop and the resource nodes which will be connected TBD.

Attached Elements

For pressurized Logistics Modules, Airlocks and Hyperbaric Airlocks attached to the resource node, thermal acquisition and transport will be provided at the resource node/element interface by an internal water system connected to the thermal transport bus located in the resource node. A heat sink for the refrigeration and freezer, located in the Logistics Module, will be provided at the node/element interface. For pressurized payloads attached directly to the node, thermal acquisition will be through central thermal bus interface heat exchangers attached externally to the payload.

Leak Detection

A method for detecting, isolating, and repairing leaks within the system is required. Where practical, provisions will be made to remove and replace failed fluid loop components without draining and reservicing the fluid loops.

Coolant Fluids

The coolant fluid to be used within the pressurized manned environment shall be water or some other non-toxic fluid.

The coolant fluid to be used outside of the pressurized manned environment shall be TBD.

10.3 THERMAL CONTROL SYSTEM FLUID SYSTEM DESCRIPTION AND CONFIGURATION

Manned Pressurized Elements

The TCS of the U.S. Manned pressurized elements and international modules will be similar in configuration to the USL Thermal Control System shown in Figure 10.3-1. The system will contain three basic loops; a primary experiment loop, an attached payload loop and a refrigeration/freezer loop.

The primary experiment loop will be a pumped single-phase water coolant loop which will service all four rack banks and will be capable of rejecting 50 kW of waste heat. The 70°F loop will collect waste heat from the avionics heat exchanger as well as from subsystem/experiment cold plates and/or heat exchangers mounted in the racks. The 35°F loop will collect waste heat from the cabin condensing heat exchanger as well as from subsystem/experiment cold plates and/or heat exchangers. The 35°F coolant interface will only be provided down one side of the module due to its limited demand, primarily from the biological experiments. USL waste heat from this primary experiment loop will be transferred to the Space Station Heat Rejection and Transport System (HR&T) through 70°F and 35°F central bus heat exchangers mounted on the exterior of the USL endcone structure. Redundant pump packages will be provided for safety.

An attached payload loop, sized for 25 kW, will be provided to cool equipment in USL adjacent nodes and/or interconnects. This loop will also be pumped single-phase water.

Refrigerator/freezer services are required in the USL. Low temperature body mounted radiators will be provided to reject the heat necessary to meet the -30° C freezer requirement.

Airlocks

Fluid lines will be installed in the airlocks to supply chilled water to atmospheric heat exchangers. The chilled water will be supplied to the airlocks by the attached payload loop. The pump, controls, and heat exchangers for the attached payload loop are located in the core modules. Temperature sensors will be installed at the inlet and the outlet of the atmospheric control heat exchanger in the airlock.

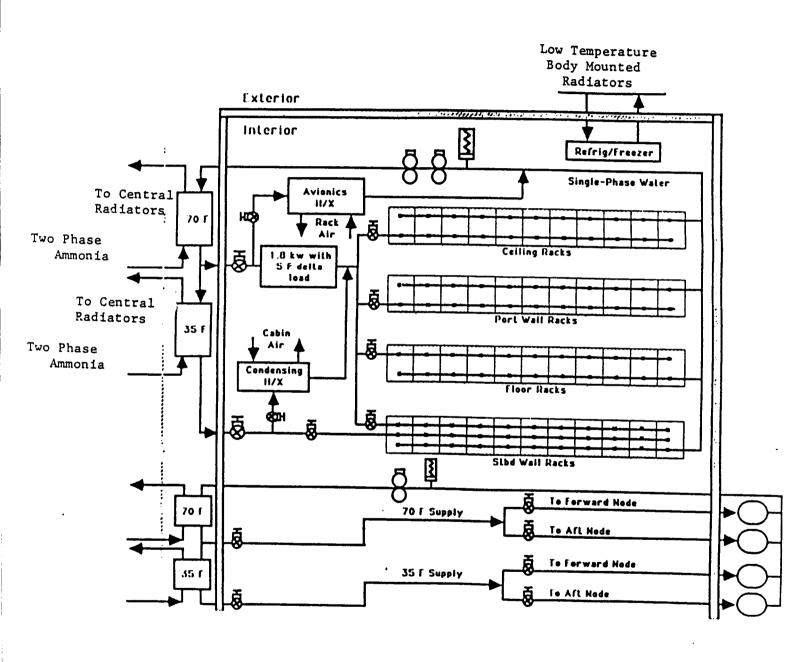


Figure 10.3-1 USL Thermal Control System

10.4 THERMAL CONTROL SYSTEM REFERENCES

- Space Station Definition and Preliminary Design, WP-01, Book 3, U.S. Lab Module, SSP-MMC-00031, Rev. B, NAS8-36525. Martin Marietta Denver Aerospace, Denver, CO., October 31, 1986.
- 2) Space Station Definition and Preliminary Design, WP-01, Book 2, Common Module. SSP-MMC-00031, Rev. B, NAS8-36525. Martin Marietta Denver Aerospace, Denver, CO., October 31, 1986.
- Space Station Definition and Preliminary Design, WP-01, Book 10, Airlocks. SSP-MMC-00031, Rev. B, NAS8-36525. Martin Marietta Denver Aerospace, Denver, CO., October 31, 1986.
- Space Station Program Definition and Requirements, Section 3 System Requirements, SS-SRD-0001. Space Station Projects Office, Marshall Space Flight Center, Huntsville, AL, January 12, 1987.

11.0 ATTACHED PAYLOADS

11.1 ATTACHED PAYLOADS OVERALL REQUIREMENTS

Overall requirements for the attached payloads are presented in Table 11.1-1.

Table 11.1-1 Attached Payloads Overall Requirements

- 1) Payloads will be mounted on stationary or rotating attachment provisions on the Resource Nodes.
- 2) Tethered Deployment shall be considered as an alternative to attachment for payloads with sensitive environmental requirements.
- 3) Interface Monitoring and Protection. Space Station and platforms shall provide monitoring, measurement and protection of all interfaces that provide data, power, cooling, or similar resources to payloads such that a payload failure or payload misuse of resources cannot result in adverse impact on other payload or other operations.
- 4) Servicing None
- 5) Contamination None
- 6) Standard Interfaces Interfaces shall be standarized appropriately so that any payload can be easily interchangeable between the manned element and attached payload.

The integration of fluids from attached payloads to other Space Station elements is presently an open issue. The baseline configuration for the attached payloads does not require fluids to be integrated. As of the October 1986 time frame, the attached payloads community preferred to be autonomous because of possible operational constraints imposed by interfacing with the station during operation.

The alternatives to interfacing with the station are to either vent waste gases to the external environment or store the waste quantities for return to earth. Venting constraints are becoming more restrictive with the new station configuration, and experiment operations may become very limited with the new contamination requirements. This would say that each attached payload would be required to include in its design a gas collection and storage system which would require additional plumbing, tanks, possibly compressors and most likely additional EVA time.

11.2 ATTACHED PAYLOADS FLUID SYSTEMS REQUIREMENTS

Attached payloads listed in Table 11.2-1 were identified in a NASA Lewis study as candidate systems that could benefit from fluid system integration.

Table 11.2-1 Annual Waste Gases from Attached Payloads (1bm/yr)

Mission/Fluids	1995	1996	1997	1998	1999	2000	2001	2002
SAAX 001 - Cosmi	.c Ray Nu	clei Ex	periment					
C02	243	485	243					
N2	155	309	155					
SAAX 021 - Superc	onductin	g Magne	t Facil:	ity				
Не	193	772	772	772	772	772	772	772
SAAX 207 - Solar	Terrestr	ial Obs	ervatory	7				
Ar	322	322	322	322	322	322	322	
N2	230	230	230	230	230	230	230	
TDMX 2311 - Long	Term Crv	ogenic	Storage					
H2			140	140	448	140		
TDMX 2421 - Activ	e Optic '	Technol	OgV					
Не			- 67	88	88			
Totals	1143	2118	1950	1552	1772	1464	1324	772
Derived from the Task Force (CETF)		Require	ments Da	atabase	and the	Critica	l Evalua	ation

11.3 ATTACHED PAYLOADS FLUID SYSTEMS DESCRIPTIONS AND CONFIGURATIONS

The NASA study recommended providing common utility ports at available payload attach points for waste gas disposal in the integrated waste fluid system. A further assessment of experiment venting constraints and commitments of attached payloads scheduled for flight will need to be performed before the benefits of fluid system integration versus nonintegration can be assessed.

11.4 ATTACHED PAYLOADS REFERENCES

- Peterson, T., Space Station Fluid Inventories of the Integrated

 Waste Fluid and Integrated Water Systems, PIR No. 159. NASA Lewis
 Research Center, Cleveland, OH, March 25, 1987.
- Space Station Program Definition and Requirements, Section 3:

 System Requirements, SS-SRD-0001, Rev. A. Space Station Projects
 Office, Marshall Space Flight Center, Huntsville, AL, January 12,
 1987.

12.0 FLUID SERVICER/VEHICLE ACCOMMODATIONS

The Space Station long range goals include the repair and servicing of various space based satellites and platforms. To accomplish this goal requires the use of transport vehicles such as the Orbital Maneuvering Vehicle (OMV), the Orbital Transfer Vehicle (OTV) or the Manned Maneuvering Unit (MMU) to transport satellites and platforms to and from the Space Station (SS) for repair or refueling. To refuel a spacecraft on-orbit will require the use of the mono-propellant version of Orbital Spacecraft consumables resupply system (OSCRS) for hydrazine users or the Superfluid Helium Tanker (SFHT) for resupply of Superfluid Helium (SFHe).

12.1 FLUID SERVICER/VEHICLE ACCOMMODATIONS OVERALL REQUIREMENTS

The top level requirements for fluid serviced vehicle accommodations are to provide for post IOC Space Station use of a National Space Transportation System (NSTS) shuttle based system which will be transported aboard the shuttle to and from Space Station and refueled and serviced on the ground. This will require protected storage with power, communications, data management and structural interfaces.

12.2 FLUID SERVICER/VEHICLE ACCOMMODATIONS FLUID SYSTEMS REQUIREMENTS

There are no fluid subsystem requirements for IOC SS with regard to fluid servicers or vehicles. The only fluid requirements at IOC are for scarring of the Integrated Nitrogen System for growth to support a low and high pressure port for a servicing facility and high pressure ports for the OMV, an Enhanced Maneuvering Unit (EMU) and an Extra vehicular Excursion Unit (EEV).

12.3 FLUID SERVICER/VEHICLE ACCOMMODATIONS FLUID SYSTEMS DESCRIPTIONS AND CONFIGURATIONS

12.3.1 Orbital Maneuvering Vehicle Description and Configuration

The OMV configuration and description are covered in detail in the Space Station Architecture Propellant System Databook, EP 1.1.

12.3.2 Orbital Transfer Vehicle (OTV) Description and Configuration

The OTV configuration and description are covered in detail in the Space Station Architecture Propellant System Databook, EP 1.1.

12.3.3 Manned Maneuvering Unit (MMU) Description and Configuration

The MMU configuration and description are covered in detail in the Space Station Architecture Propellant System Databook, EP 1.1.

12.3.4 Orbital Spacecraft Consumables Resupply System (OSCRS) Descriptions and Configurations

The OSCRS configuration and descriptions are covered in detail in the Space Station Architecture Propellant System Databook, EP 1.1

12.3.5 Superfluid Helium Tanker (SFHT) Description and Configuration

12.3.5.1 SFHT General Description

Initially resupply will be accomplished as a Shuttle based operation. A typical resupply operation would use the SFHT mounted to a pallet in the Shuttle Cargo Bay, once on orbit, the user satellite will be safed by Satellite RF Control, and appendages configured for retrieval with the orbiter Remote Manipulator System (RMS). The RMS will place the satellite on the SFHT berthing equipment, where it will be secured with latches. After the umbilicals are installed and verified to be functional, the Extra vehicular Activity (EVA) crew is no longer required for chilldown of Super Fluid Helium (SFHe) transfer. Fluid transfer is then controlled by a mission specialist from the Aft Flight Deck (AFD) Control Panels. Future growth would call for use of SFHT on an OMV. System requirements for the SFHT are shown in Table 12.3-1.

Table 12.3-1 Primary Superfluid Helium Tanker Requirements

- 1) Provide the versatility to satisfy NASA requirements for resupply of SFHe to a variety of users for initial design considerations SIRTF resupply shall be considered the design baseline.
- 2) Provide an adaptable and versatile SFHT design that can meet the requirements for orbital resupply of SFHe into the next century without major hardware modifications.
- 3) Meet hold times of four weeks on the ground and nine months on orbit.
- 4) Designed for low cost maintenance by using ground based check-out, maintenance, overhaul and adjustment.
- 5) Designed to be compatible with use on an OMV.
- 6) Operating Life; 50 Cycles
- 7) Useful Life; 20 Years
- 8) Shelf Life; 20 Years
- 9) Withstand surges from zero pressure to peak surge pressure and return to Maximum Expected Operating Pressure (MEOP) within 20 miliseconds.
- 10) Safety redundancy shall satisfy NHB 1700.7A (Two-fault tolerance to a hazard).
- 11) No credible single failure shall result in permanent inability of SFHT to complete mission. (One-fault tolerance to mission success)
- 12) Conform to Orbiter Payload bay envelope.

Table 12.3-1 Primary Superfluid Helium Tanker Requirements (Continued)

- 13) Conform to Space Station Satellite Servicing Facility envelope.
- 14) Center of Gravity compatible with the Orbiter, Space Station and OMV.
- 15) Maximum Total Loaded System Weight = 4
 Helium Weight
- 16) Tankage capacity of 388.4 cu. ft. SFHe (141.2 cu. ft. for SIRTF + 176.6 cu. ft. for system cooldown + 70.6 cu. ft. for Misc. losses and margin reserves)
- 12.3.5.2 SFHT Performance Requirements Table 12.3-2 lists the potential SFHT users and their fluid requirements. SIRTF is defined as the baseline for system design and sizing considerations for SFHT, although, the maximum required volume identified by a single user is 247.2 cu. ft. for LDR. The SIRTF requirement is to supply 141.2 cu. ft. of SFHe which requires 176.6 cu. ft. additional SFHe for cooldown purposes. These quantities, plus unavailable liquid and margin reserves, indicate a fluid system tank volume of 388.4 cu. ft. or more.

Table 12.3-2 Superfluid Helium User Database

	Helium	
	Volume	Helium
User	Cu. Ft.	<u>Phase</u>
-AXAF	7.1	SFHe
-IR Telescope in Space	15.9	TBS
-MMPS/CPPF	7.1	SFHe & LHe
-Gravity Probe B	53.0	SFHe
-SIRTF	141.2	SFHe
-Lambda Point Experiment	7.1	SFHe
-Astromag	211.9	TBD
-Far IR/Subm Space Telescope	211.9	SFHe
-LDR	247.2	SFHe
-Submm Telescope	8.8	TBS
-Superconducting Magnet Facility	17.7	SFHe or LHe
-Planetary IR Telescope	17.7	SFHe

12.3.5.3 SFHT Configuration and Subsystems - The SFHT fluid system design provides for storage and transfer of superfluid helium. Since the thermal requirements to maintain helium in the superfluid condition are so unique, the SFHT is quite different from a conventional cryogenic tanker. The SFHT takes advantage of SFHe's unique properties to accomplish venting and fluid transfer. Because helium is a safe media for cargo bay purging, venting on board the orbiter while in a hold presents no hazard. The basic design uses two tanks which are separated by three layers of insulation blankets and vapor cooled shields. The shields are thermally coupled to the supports, lines, and wires to intercept most of the heat leaking into the insulated space.

The vacuum jacket is a leak before rupture pressure vessel so that the failure becomes controllable and the rate of heat transferred to the inner tank is reduced. This in turn reduces the rate of pressure buildup and also reduces the size of the emergency vent line. Both the inner tank and the vacuum jacket are designed to withstand at least 15 psia external pressure. This is necessary for the inner tank for protection against vacuum jacket failure, as well as to facilitate the rigorous leak checks that will be required, using a leak detection procedure that requires evacuation of the tank.

The fluid system schematic is shown in Figure 12.3-1 with the corresponding component listing shown in Table 12.3-3. To meet the two fault tolerance for safety and one fault tolerance for mission success, a total of 14 valves are required inside the vacuum jacket, and 16 external valves are used. The fill line is not thermally coupled to the vapor cooled shields in order to minimize heat leak during its use. This allows its heat to bypass the shield. The cold valves are located close to the inner tank wall to minimize piping heat leak, including the prevention of serious heat leak by thermal-acoustic oscillations that occur when open lines connect to the cold vapor space between a tank and a warm valve. Porous plugs are used to provide the phase separation for thermodynamic venting through the vapor shields.

12.3.5.5 SFHT Accommodations

The current IOC phase of Space Station calls for the use of the SFHT to provide a superfluid helium resupply capability, as a NSTS Shuttle based operation with a future growth option of Space Station storage for use with an OMV, leaving the current interfaces as structural and power only. Since resupply is to be done on the ground, there are no fluid interfaces defined at this time.

12.4 FLUID SERVICE/VEHICLE ACCOMMODATIONS REFERENCES

- 1) Space Station Architecture Propellant Systems Databook, EP 1.1, MCR-87-516, NAS8-36438. April 2, 1987, Martin Marietta Denver Aerospace.
- 2) Study and Design of a Superfluid Helium Tanker, Technical Proposal, Volume One, P87-61055-1. Mission Suitability, May 1987.
- 3) Space Station Definition and Preliminary Design, WP-01, Book 7
 Vehicle Accommodations, SSP-MMC-00031 (Rev. A) NAS8-36525.

 Martin Marietta Denver Aerospace, June 1986.

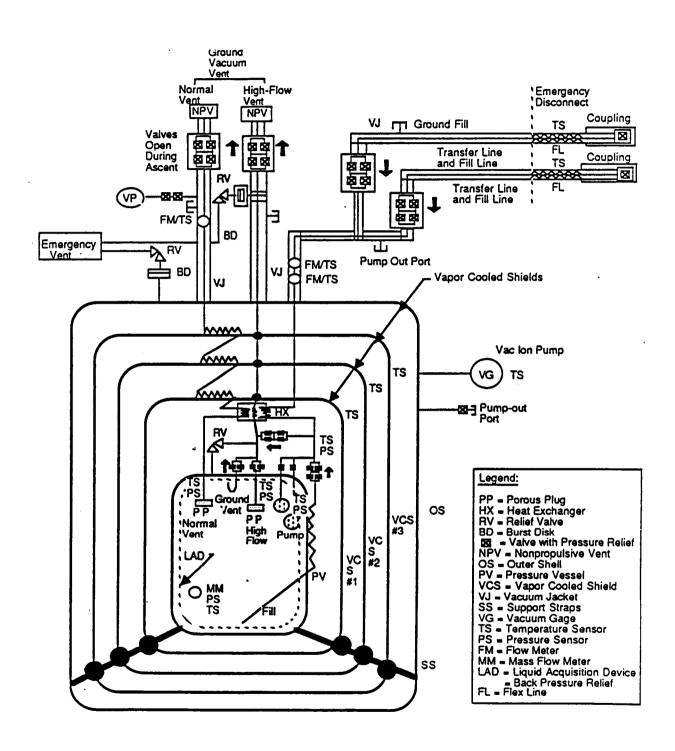


Figure 12.3-1 Superfluid Helium Tanker Fluid System Schematic

c-3

Table 12,3-4 Superfluid Helium Tanker Component List

NG.	}	Mandayo	8	SIZE	PRESSURE MEOP	USAGE	APPROX	VENDOR NAME	VENDOR PART
i	APPLICATON	TYPE	RECO	(1n)	(psia)	MEDIA	MASS (1b)		NUMBER
149	SFHT,	DI SCONNECT,	~~~	1.0	VACUUM	SFHE	2.0	TBO	30
150	SFHT,	DISCONNECT, EMERGENCY	~ ~ ~	1.0	VACUUM	SFHE	3.0	TBD	TBD
- 29	I SFHT,	MISC, BURST DISK	~	1.0	VACUUM	SFHE	6.0	TBD	OBT
151	SFHT,	MISC, FLEX HOSE	~~~	1.0	VACUUM	SFHE	0.0	TBD	TBD
169	SPHT,	MISC, HEAT EXCHANGER	 	MULTIPLE	VACUUM	SFHE	3.0	TBD	TBO
191	SPHT,	MISC, POROUS PLUG		.375	VACUUM	SFHE	0.3	TBD	TBO
3	SPHT,	MISC, POROUS PLUG		1.0	VACUUM	SFRE	1.2	TBD	TBD
2	SFHT,	MISC, PUMP, FEP	~~-	1.0	VACUUM	SFHE	8.0	TBD	OBT
165	SFHT,	MISC, PUMP, VACUUM		.375	VACUUM	SFHE	0.0	TBD	TBD
166	I SFHT,	MISC, PUMP, VACUUM GAGE ION		νį	VACUUM	SFHE	3.0	TBD	1780
161	SFHT,	MISC, VENT ASSY, NON-PROPULSIVE		1.0	VACUUM	SFHE	0.3	TBD	TBD
162	SFHT,	MISC, VENT ASSY, NON-PROPULSIVE		375.	VACUUM	SFHE	0.3	TBD	TBD
163	SFHT,	MISC, VENT ASSY, NON-PROPULSIVE		MULTIPLE	VACUUM	SFHE	0.5	TBD	TBD
147	SFHT,	PRESSURE VESSEL, ISOGRID		MULTIPLE	VACUUM	SFHE	750.0	130	138D
148	SFHT,	PRESSURE VESSEL, STIFFENED MONOCOQUE		MULTIPLE	VACUUM	SFHE	1500.0	TBO	TBD
7	SEHT,	SENSOR, FLOW METER, GAS		375.	VACUUM	SFHE	1.0	THO	TBD
173	SFHT,	SENSOR, FLOW METER, LIQUID	~	1.0	VACUUM	SFHE	1.0	TBD	TBD
172	SPHT,	SENSOR, MASS METER		CMT	VACCUM	SFHE	0.1	Off	TBD
170	SFHT,	SENSOR, PRESSURE	· · ·	OET	VACUUM	SFHE	9 ;	ORT	TBD
-2:	SFHT,	SENSOR, TEMPERATURE		OF .	VACTUM	SFHE	0.2	TBD	TBD
155	SFHT,	VALVE, MANUAL, SHUT-OFF		1.0	VACUUM	SPHE	1.0	138D	TBD
158	SFHT,	VALVE, RELIEF	7	1.0	VACUUM	SFHE	3.0	TBO	TBD
159	SFHT,	VAIVE, RELIEF		1.0	VACUUM	SFHE	2.0	TBD	TBD
156	SEHT,	VALVE, SEAL-OFF, VACUUM		1.0	VACUUM	SFHE	1.0	Cet	TBD
157	SFHT,	VALVE, SEAL-OFF, VACUUM		5.0	VACUUM	SFHE	0.5	TBD	TBD
154	SFHT,	VALVE, SOLENOID, LATCHING		1.0	VACUUM	SFHE	3.0	1790	TBD
152	SEHT,	VALVE, SOLENOID, LATCHING W/BPR	9	.375	VACUUM	SFRE	1.5	1780	TBD
153	SFHT,	VALVE, SOLENOID, LATCHING W/BPR	22	1.0	VACUUM	SFHE	.	1380	TBD
-									